

Table II-1. SUMMARY OF KINETIC STUDIES OF THE FISCHER-TROPSCH SYNTHESIS ON COBALT-BASED CATALYSTS

REFERENCE	CATALYST	REACTOR TYPE	T (°C)	OPERATING CONDITIONS		INTRINSIC KINETIC EXPRESSION <sup>a</sup>	EQ
				P (MPa)	H <sub>2</sub> /CO <sub>2</sub> In (molar)		
Brötz <sup>1</sup>	Co/MgO/THO <sub>2</sub> / kies.	Fixed-bed	185-200	0.1	2	$-R_{H_2+CO} = \frac{aP^2 H_2}{P CO}$	(3)
Anderson <sup>2</sup>	Co/THO <sub>2</sub> /kies.	Fixed-bed	186-207	0.1	0.9-3.5	$-R_{H_2+CO} = \frac{aP^2 P CO}{(1 + bP H_2)^2 P CO}$	(4)
Yang et al. <sup>3</sup>	Co/CuO/Al <sub>2</sub> O <sub>3</sub>	Fixed-bed	235-270	0.17-5.5	1.0-3.0	$-R_{H_2+CO} = aP^2 H_2 CO^{-0.5}$	(5)
Parnell et al. <sup>4</sup>	Co/La <sub>2</sub> O <sub>3</sub> / Al <sub>2</sub> O <sub>3</sub>	Berty (low conversion)	215	0.49-0.8	2	$-R_{H_2+CO} = aP^{0.55} P CO^{-0.33}$	(6)
Rautavaara and van der Baan <sup>5</sup>	Co/Al <sub>2</sub> O <sub>3</sub>	Fixed-bed (low conversion)	250	0.1	0.2-4.0	$-R_{CO} = \frac{aP^2 H_2 CO}{(1 + bP^{1/3} H_2 CO)}$	(7)
Wang <sup>6</sup>	Co/B/Al <sub>2</sub> O <sub>3</sub>	Fixed-bed (low conversion)	181	0.1-0.2	0.25-4.0	$-R_{CO} = aP^2 H_2 CO^{-0.5}$	(8)
Sarup and Wojlechowski <sup>7</sup> and Wojlechowski <sup>8</sup>	Co/kies.	Berty	190	0.2-1.5 <sup>b</sup>	0.5-8.3 <sup>b</sup>	$-R_{CO} = \frac{aP^{1/2} H_2 CO}{(1 + bP^{1/2} H_2 CO + cP^{1/2} H_2 CO)^2}$	(9)
						$-R_{CO} = \frac{aP^2 H_2 CO}{(1 + bP^{1/2} H_2 CO + cP^{1/2} H_2 CO)^2}$	(10)

<sup>a</sup> a, b, c, and d in these equations are temperature-dependent constants.

<sup>b</sup> these ranges of operating conditions are estimated from their experimental data.

Table II-2.

ACTIVITY FOR REPEATED CONDITIONS OF 240°C, 0.79 MPa, H <sub>2</sub> /CO=2, AND SYNTHESIS GAS FEED RATE OF 0.067 NI/min/g of catalyst <sup>†</sup>				
Time-On-Stream [h]	Oxygen Closure [% molar]	-R <sub>H<sub>2</sub>+CO</sub> [mmol/min/gcat]	P <sub>H<sub>2</sub></sub> [MPa]	P <sub>CO</sub> [MPa]
257.5	97.06	0.678	0.48	0.25
617.0	101.23	0.680	0.48	0.24
1073.0 <sup>†</sup>	100.21	0.594	0.45	0.25
2176.5	99.89	0.694	0.47	0.24

<sup>†</sup> Flow is calculated at standard conditions; grams of catalyst are on an unreduced basis.

<sup>†</sup> H<sub>2</sub>/CO and feed rate were slightly lower for this material balance at 1.95 and 0.066 standard l/min/gcat, respectively.

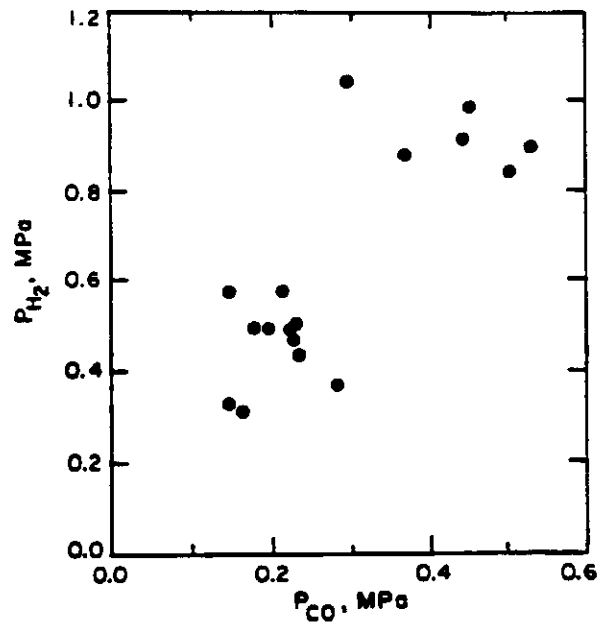


Fig. II-1 Plot showing lack of covariance between  $P_{H_2}$  and  $P_{CO}$  at 220°C.

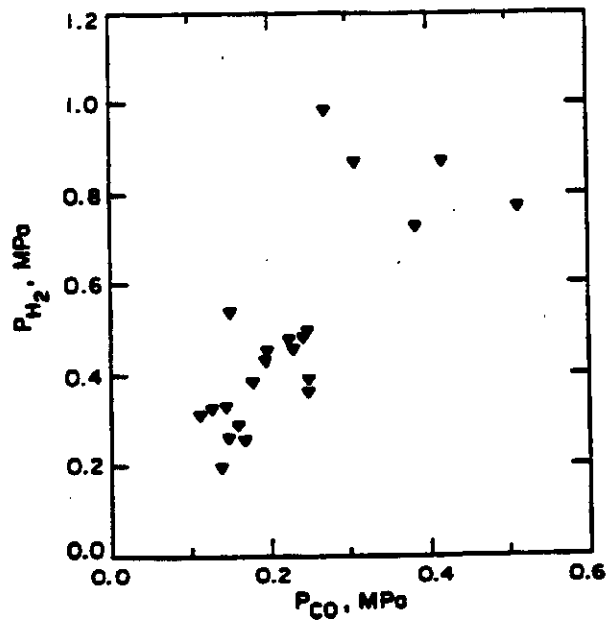


Fig. II-2 Plot showing lack of covariance between  $P_{H_2}$  and  $P_{CO}$  at 240°C.

**Table II-3.  $R^2$  for Linearized Expressions**

eq	$T, ^\circ\text{C}$	$R^2$	eq	$T, ^\circ\text{C}$	$R^2$
17	220	0.954	20	220	0.970
	240	0.909		240	0.886
18	220	0.938	21	220	0.968
	240	0.945		240	0.984
19	220	0.927			
	240	0.590			

**Table II-4. Nonlinear Regression Statistical Analyses**

eq	residuals [sum of squared errors]	$F$ ratio	$R^2$
4	0.340	42.06	0.663
7	0.072	303.27	0.929
14	0.245	85.82	0.758
15	0.214	101.61	0.788
16	0.062	361.22	0.938

**Table II-5. Results of Nonlinear Fit of Data from This Study at 220 and 240  $^\circ\text{C}$  to Eq 16**

reactor temp, $^\circ\text{C}$	$a^a$	std error of $a^a$	$t$ value <sup>b</sup> of $a$	$b^c$	std error of $b^b$	$t$ value <sup>b</sup> of $b$
240	75.76	9.20	8.23	11.61	0.97	12.02
220	53.11	1.38	38.63	22.26	3.63	6.62

<sup>a</sup>In mmol/(min·g of catalyst·MPa<sup>2</sup>). <sup>b</sup>There were 23 data points collected at 240  $^\circ\text{C}$  and 17 at 220  $^\circ\text{C}$ . Critical  $t$  values for 99% confidence that the parameters are statistically significant are  $t_{0.995,21} = 2.831$  for 240  $^\circ\text{C}$ ;  $t_{0.995,15} = 2.947$  for 220  $^\circ\text{C}$ .  $t$  values above these critical values indicate that one can be 99% confident that the parameters are significant. <sup>c</sup>In 1/MPa.

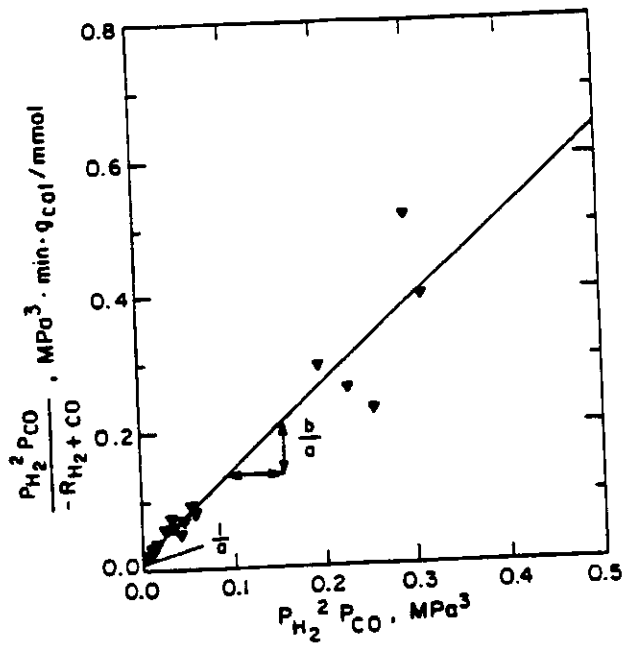


Fig. II-3 Test of eq 17 with experimental results at 240°C. Solid line is best fit linear regression line.

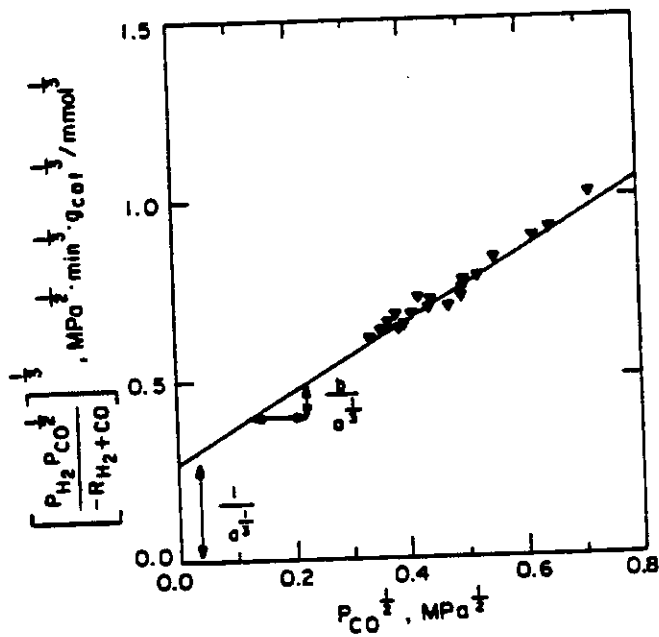


Fig. II-4 Test of eq 18 with experimental results at 240°C. Solid line is best fit linear regression line.

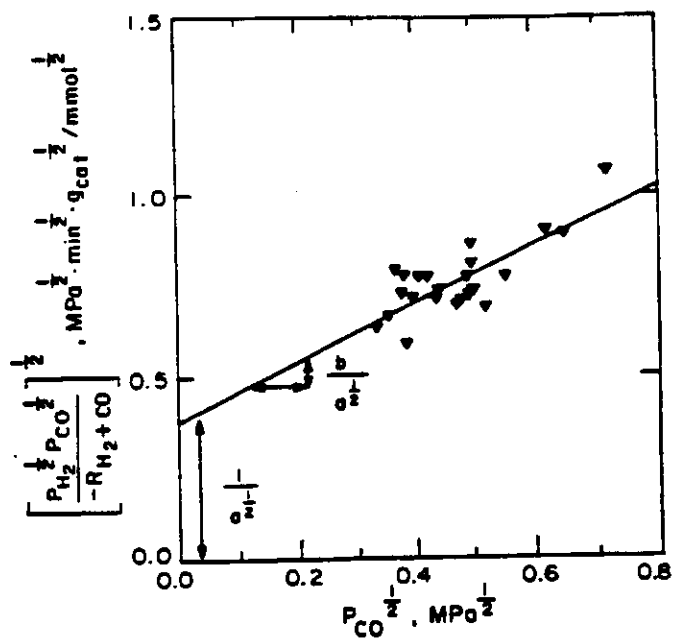


Fig. II-5

Test of eq 19 with experimental results at 240°C. Solid line is best fit linear regression line.

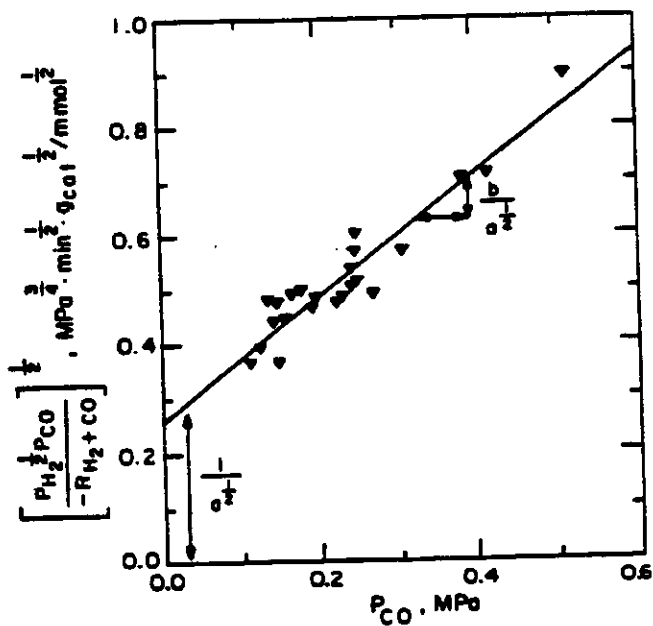


Fig. II-6

Test of eq 20 with experimental results at 240°C. Solid line is best fit linear regression line.

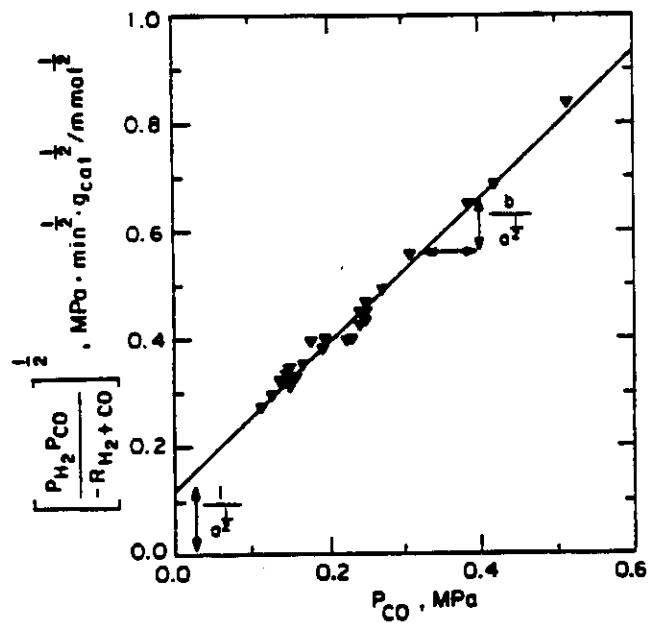


Fig. II-7 Test of eq 21 with experimental results at 240°C. Solid line is best fit linear regression line.

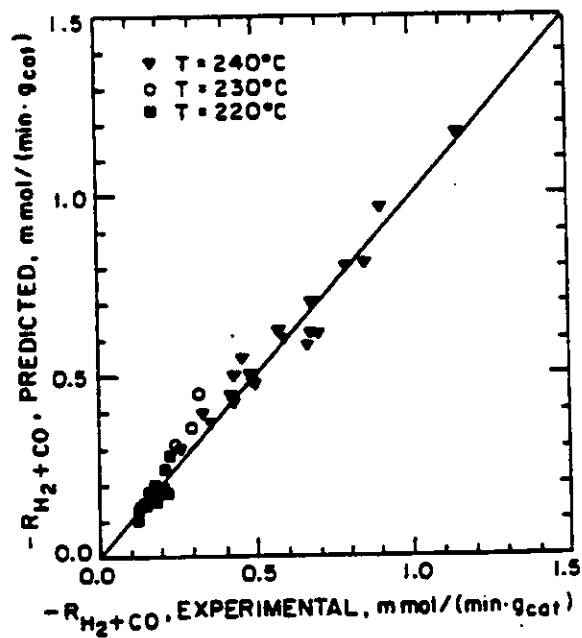


Fig. II-8 Parity plot comparison of data with prediction from eq. 16. Solid line gives predicted values.

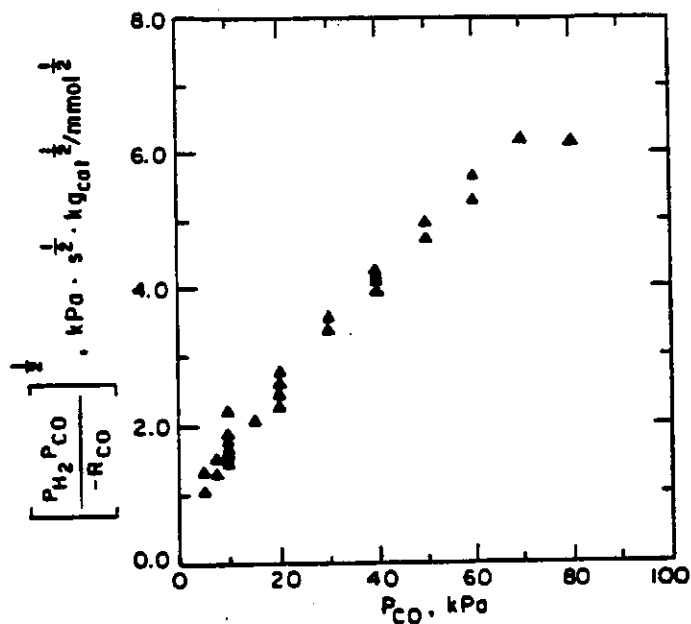


Fig. II-9 Test of eq 21 with data from Rautavuoma and van der Baan.<sup>5</sup>

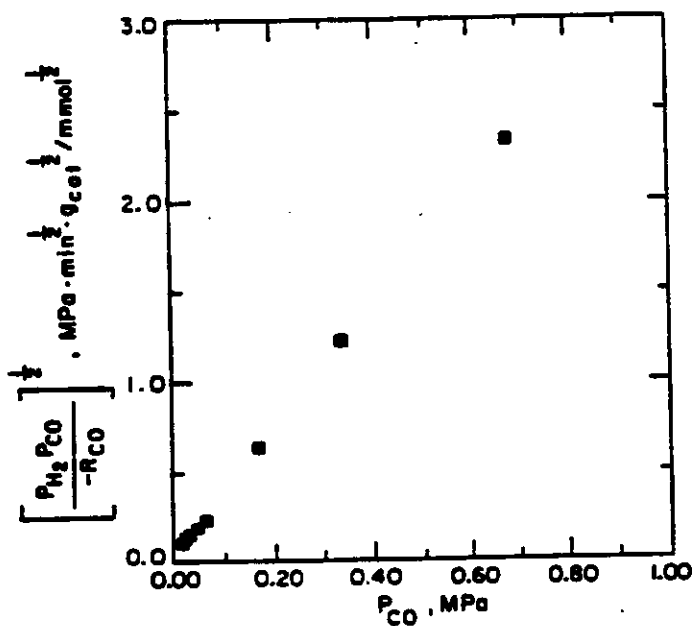


Fig. II-10 Test of eq 21 with data from Wang<sup>6</sup> (pp 100-101).



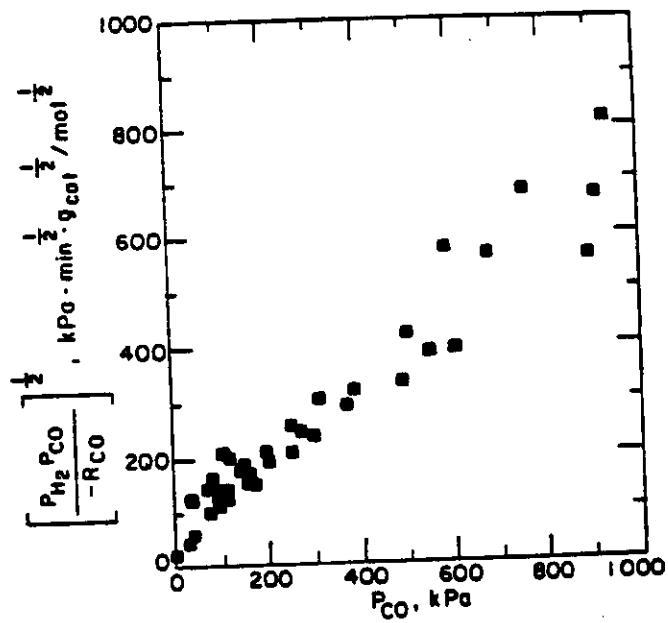


Fig. II-11 Test of eq 21 with data from Sarup and Wojciechowski.<sup>7</sup>