Effect of Synthesis Gas Quality on Yields

From the Case 6 design breakdown of the reactor effluent previously submitted, it was found that the total C_3 + yield (incluing WSC) per MM SCFH of syn. gas feed predicted was 36.22 Bbls. This was for a synthesis gas that was quite different from that now being produced at Brownsville.

Shown in the following Table C are radomly selected analyses of the synthesis gas in various runs compared with that predicted in design.

On Nov. 29, 1951, the end of Run 13, the practice of adding about 15% steam to the natural gas feed to the generator in order to reduce soot formation was started. It will be noted that this made a perceptible difference in the syn. gas composition, H_2/CO ratio and H_2+CO purity as shown below.

		Average Runs $\frac{4}{11}$ 13 & $\frac{4}{11}$ 16 Incl.	Average Runs #6 & #12 Incl.*
	Design	with Steam	No Steam
Syn. Gas Rate MMSCFH	5.0	3.18	3.10
Mol % Dry: CO	33.23	31.73	33.27
H ₂	61.35	59.78	60.15
^{CO} 2	1.31	3.90	2.97
N ₂ +A CH ₁	3.01	2.12	1.94
CH ₄	1.10	2.47	1.80
H ₂ /co (H ₂ +co)%	1.845 94.2	1.88 91.5	1.81 93.42

^{*} Run %8 Excluded

TABLE C

COMPARISON OF FRESH FEED COMPOSITIONS

Run # Date Syn Gas Rate	Design	2/22/	#16 /52 2/29/52	$\frac{2}{2/3/2}$	1 <u>5</u> 52 2/10/52	1/11/5	#14 52 1/21/5	2 1/22/52	#1 12/23/5	.3 51 12/30/51	
H2 61 CO2 N2 CH4 H2O	3.1 33.2 1.1 61.3 1.3 1.3 3.0 3.0	559.70 1 4.63 1 1.34 0 2.76	3.30 .63 32.34 58.98 3.87 1.60 2.58	2.856 .69 32.20 59.65 3.71 1.31 2.44	6 2.663 .69 31.43 60.14 4.01 1.11 2.62	2.646 .73 31.74 59.58 3.90 1.45 2.60	3.354 .68 31.62 60.23 3.63 1.68 2.16	3.771 .65 31.69 60.08 3.77 1.38 2.43	2.999 .73 32.08 59.82 3.71 1.43 2.23	2.990 .70 31.56 59.87 3.84 1.61 2.42	
H ₂ /CO 1.8 (H ₂ +CO)%94.2	B45 2	1.93 90.62	1.81 91.32	1.85 91.85	1.91 91.57	1.88 91.32	1.90 91.85	1.90 91.77	1.86 91.90	1.90 91.43	
Run # Date Syn. Gas Rate A CO H2 CO2 N2 CH4	#1 11/30 3.03 .69 33.48 59.77 3.06 .93 2.07	2 12/5 2.81 .68 32.14 59.86 3.88 1.41 2.03	3.00 3 .65 32.88 34 60.89 59 2.87 2 1.04 1	.05 2 .71 .03 32 .97 60 .69 2	#10 /21 7/29 2.51 2.67 .66 .61 2.66 34.42 0.93 60.56 2.65 2.49 1.08 .88 2.02 1.04	#9 6/6 6 2.81 .67 33.313 60.936 2.74 1.07 1.28	7/8 4.77 3.93 3.93 3.93 3.07 2. 1.18 1.	07 3.46 74 .79 70 34.95 40 58.05 94 2.58	.74 33.30 32. 58.63 59. 3.12 3. 1.88 1.	06 73 51	
H2/CO H2+CO)%	1.79 93.25	1.86 92.00			1.87 1.76 3.59 49.80	1.83 94.249		68 1.66 10 93.00	1.76 1. 91.93 92.		

If it is assumed that steam will continue to be added to the generator to control soot formation the syn. gas will contain only 90.32 of $\rm H_2+CO$ having an $\rm H_2/CO$ ratio of 1.845, assuming the extra hydrogen is not beneficial, thus

% CO = 31.73 x 1.845 = 58.6 = % Effective
$$H_2$$
 31.73 + 58.6 = 90.3% H_2 +CO

It follows therefore that the anticipated yield of $C_3+/MMSCF$ of synthesis gas must be reduced to 90.3/94.2 = 95.9% of that originally anticipated due to inferior synthesis gas composition. This amounts to 34.73 Bbls/MMSCF of syn. gas.

Similarly if steam is not added the syn. gas will contain 92.1% of $\rm H_2+CO$ of 1.845 $\rm H_2/CO$ ratio and the anticipated yield must be reduced to $\frac{92.1}{94.2}$ = 97.82 of that predicted (35.42 Bbls/MMSCF FF). Roughly therefore some 3 or 4 percentage points of the discrepancy between anticipated and actual yields of $\rm C_3+/MMSCF$ of syn. gas at Brownsville can be accounted for by differences in the synthesis gas compositions.

Incidentally, it is noted that the Nitrogen plus Argon in the Brownsville gas is consistently less than that predicted. This is because it was assumed in design that the nat. gas would contain 5% N₂ whereas this has been running consistently at 0.3 to 0.5%.

On the above Fig. C we have also shown vertical lines representing the space velocity required per reactor for the present production of syn. gas (abt. 3,000,000 SCFH/Reactor) and that required ultimately for the design rate of 5,000,000 SCFH for each reactor. These values were developed as follows: