

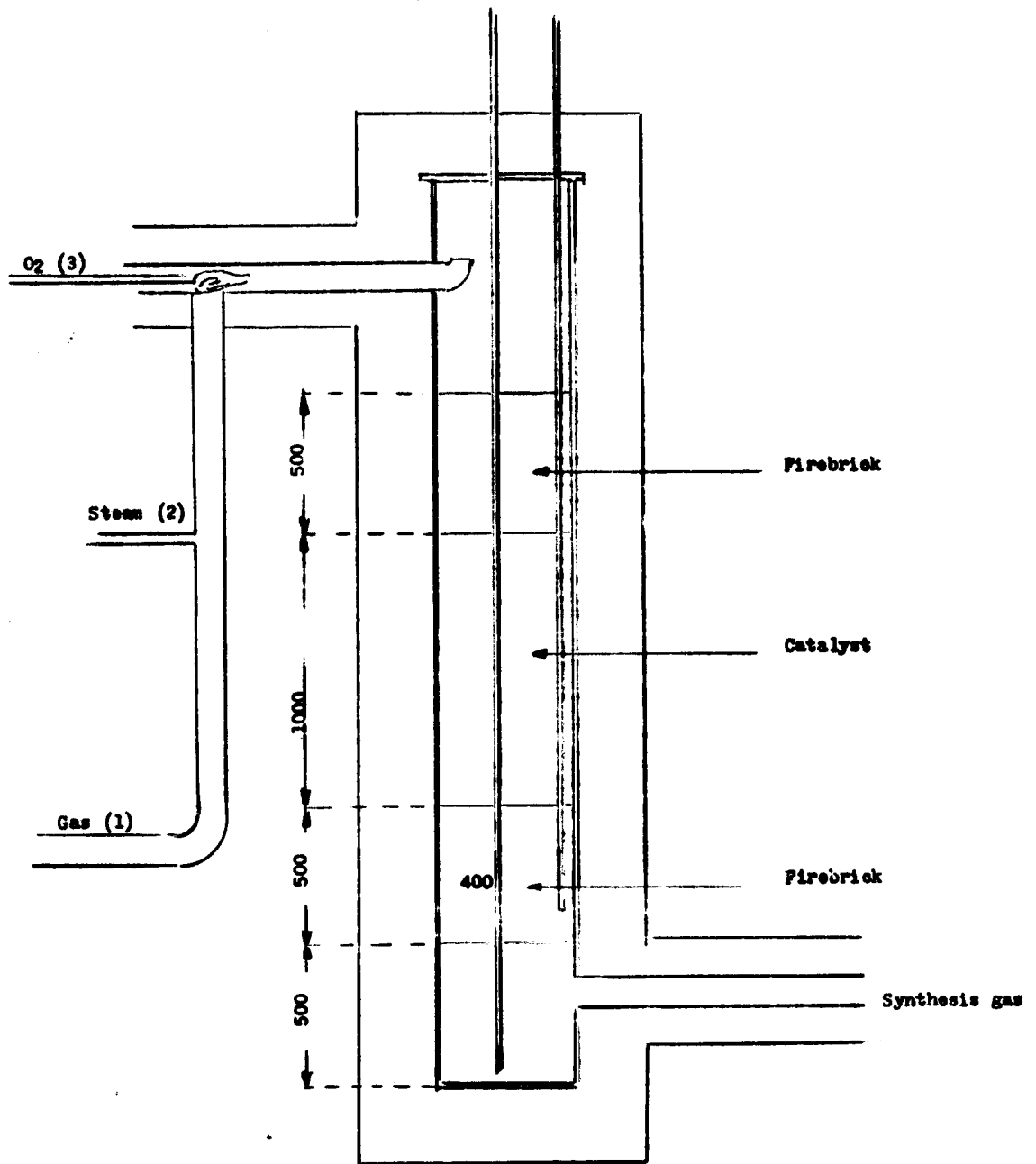


Figure 1

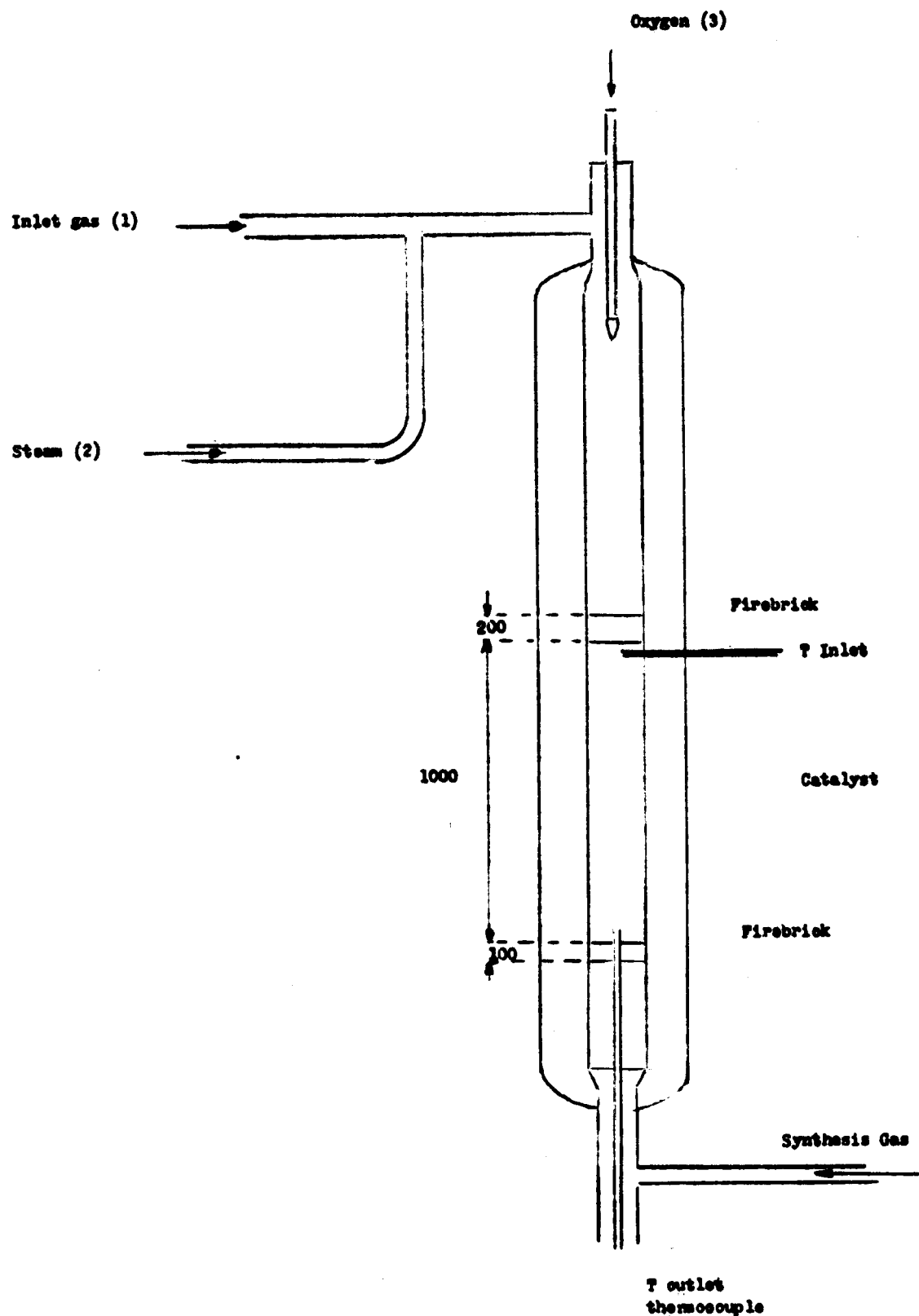
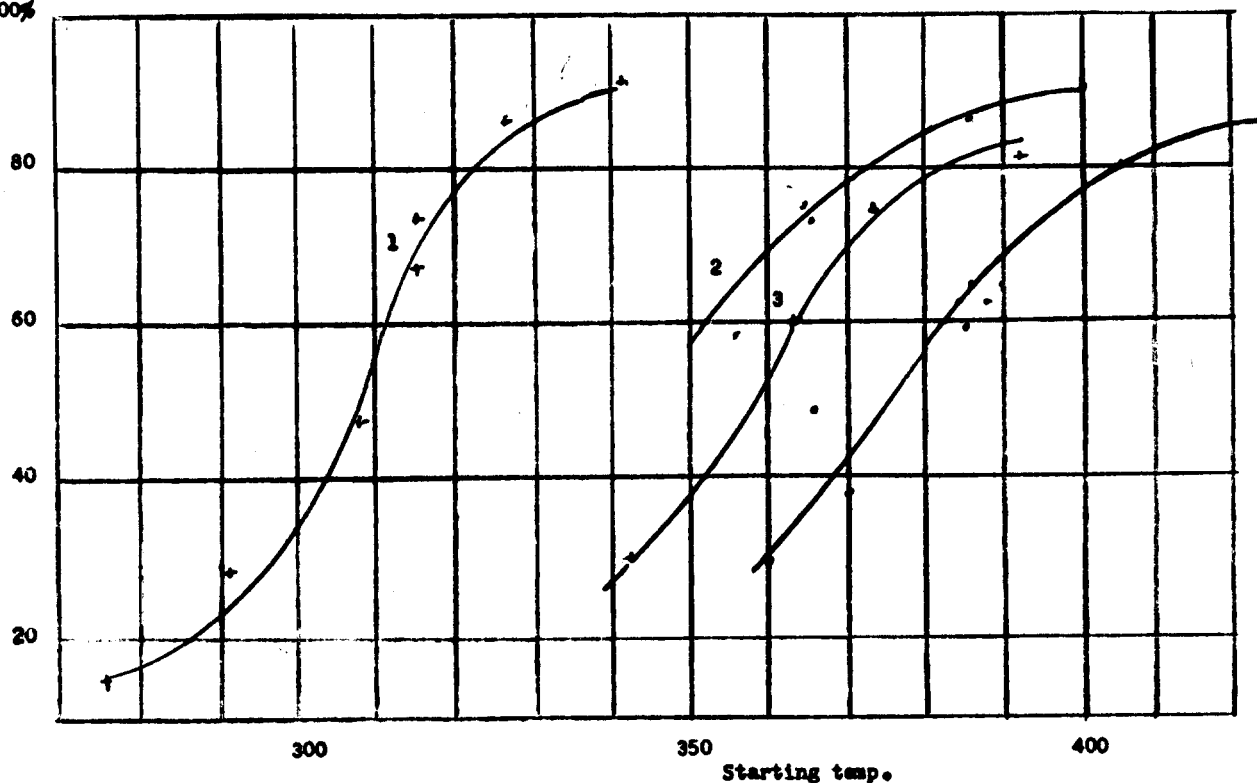


Figure 2

Conversion
100%



1. 1 atm. abs. 580 m³ gas/m³ cat.,hr.; H₂O:CO = 3.3:1
2. 7 atm. abs. 400 m³ gas/m³ cat.,hr.; H₂O:CO = 2.4:1
3. 11 atm. abs. 540 m³ gas/m³ cat.,hr.; H₂O:CO = 1.8:1
4. 16 atm. abs. 540 m³ gas/m³ cat.,hr.; H₂O:CO = 1.9:1

Figure 3. - Catalyst activity, variation with pressure percent of the theoretically possible CO conversion in relation to inlet temperature.

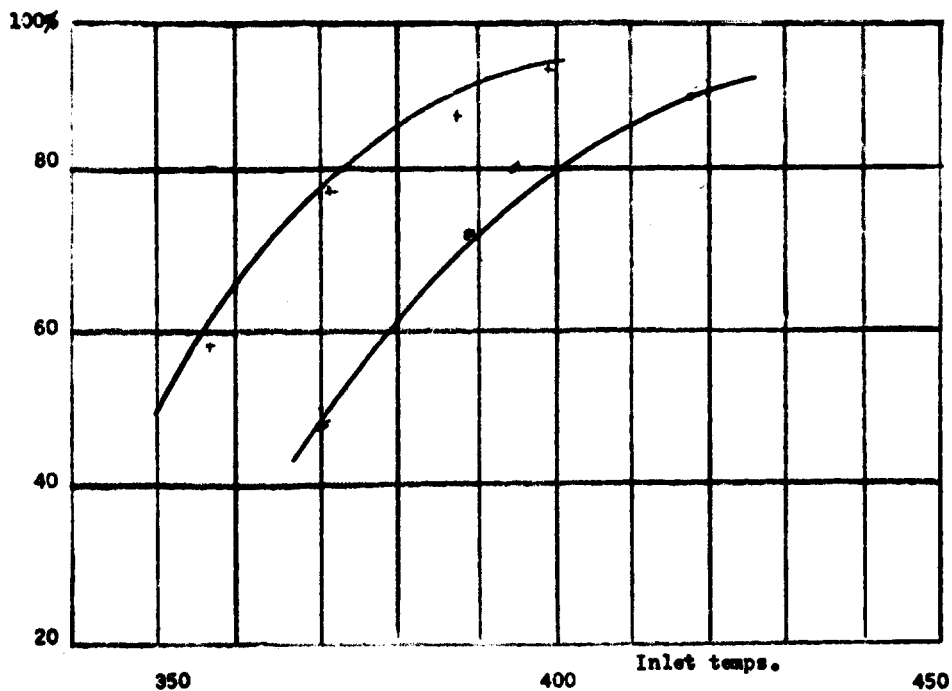


Figure 4. - CO-conversion with different inlet temperatures and residence time - 7 atm.

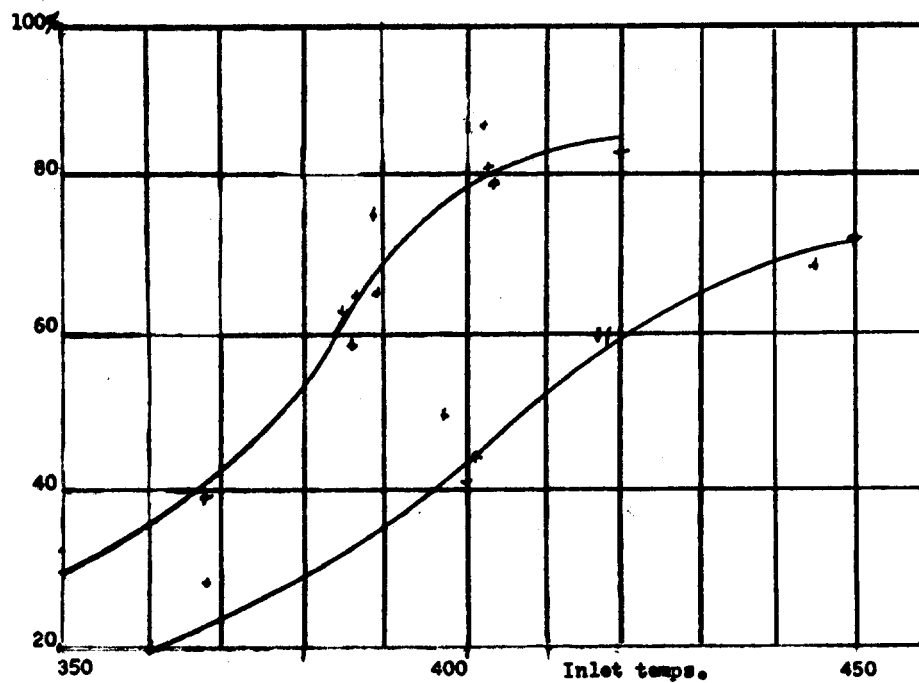
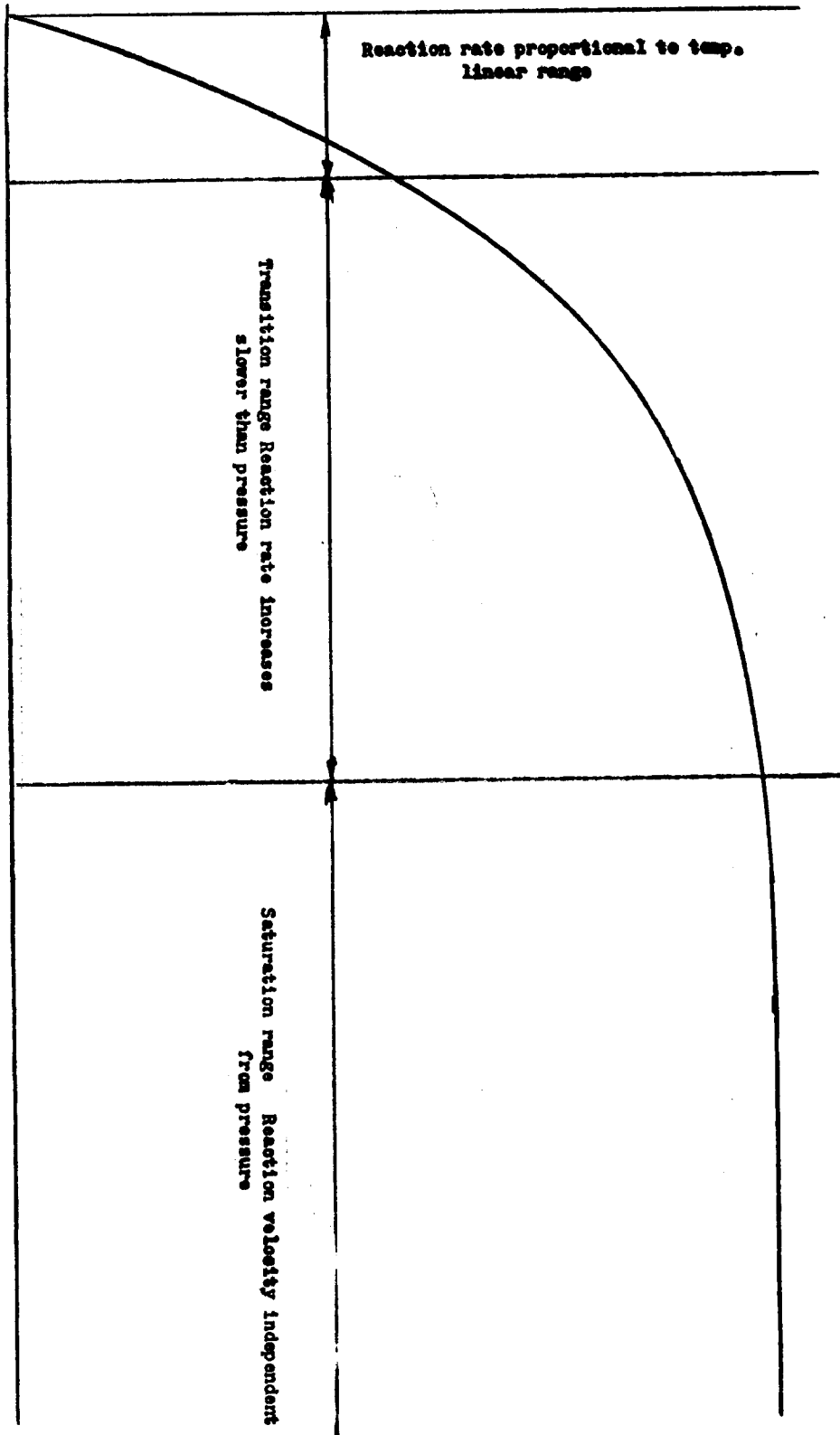


Figure 5. - CO-conversion with different inlet temperatures and residence time - 16 atm.



Adsorption Isotherm
 Relation between amount adsorbed upon the catalyst and the partial pressure in the gas space
 Figure 6

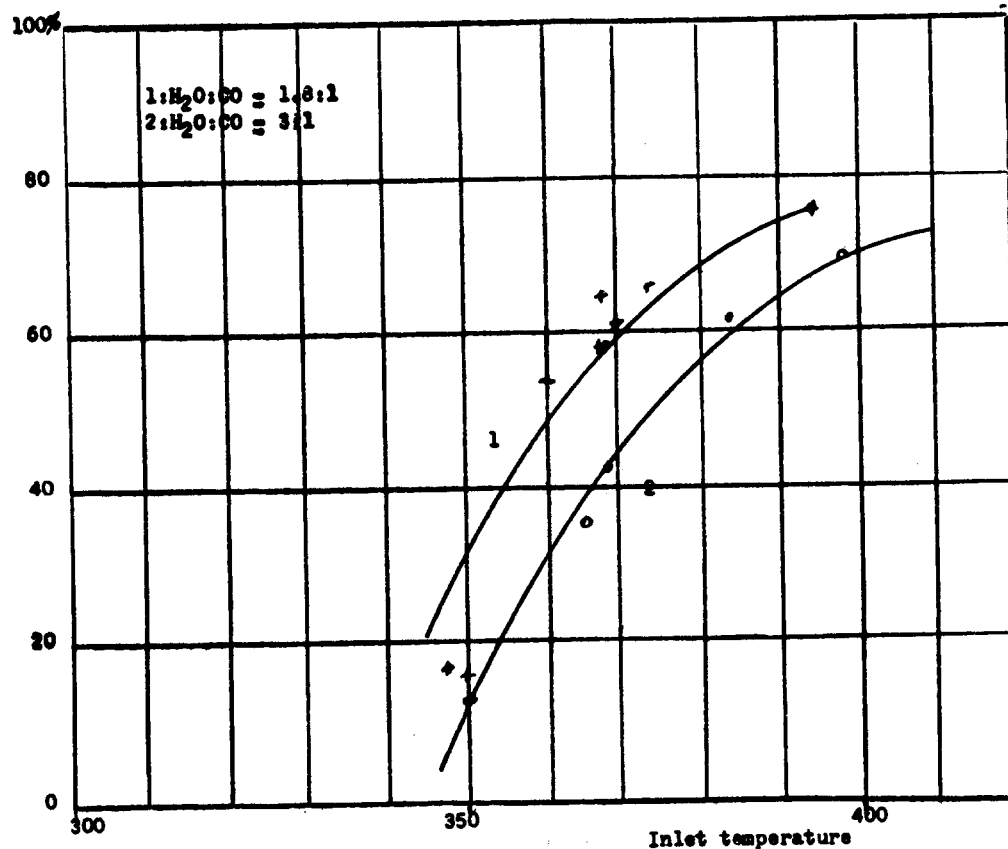


Figure 7. - CO conversion at different inlet temps. and excess steam

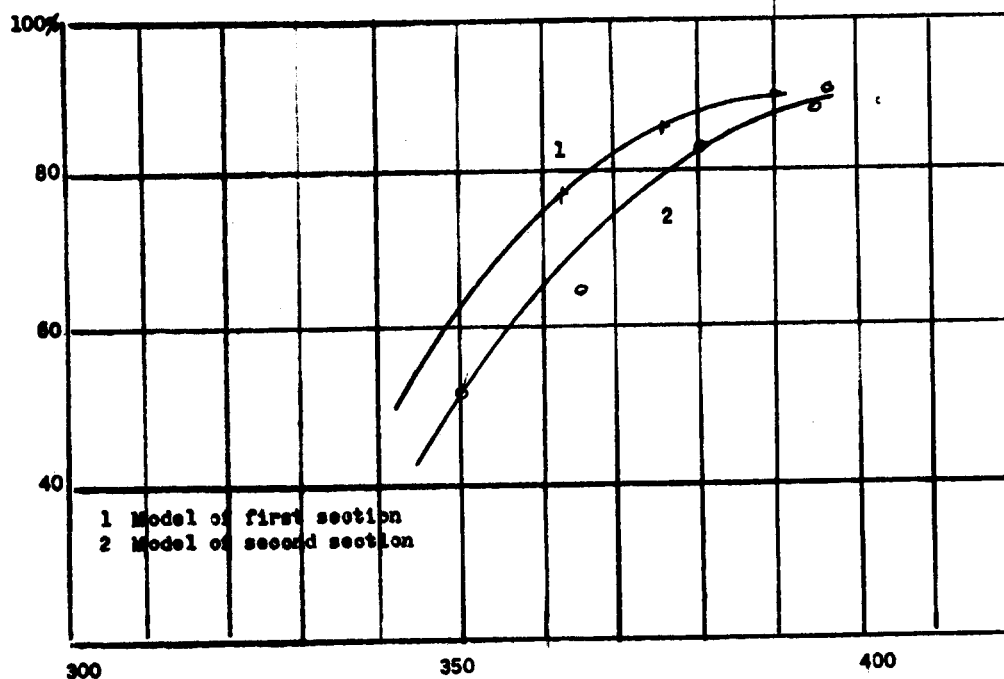


Figure 8. - Comparison of catalyst activity in the first and second sections variations of CO conversion with the inlet temperatures