UNITED STATES DEPARTMENT OF THE INTERIOR BUREAU OF MINES OFFICE OF SYNTHETIC LIQUID FUEL LOUISIANA, MISSOURI

From Dr. Pier's File

T - 431

High Pressure Experiments Ludwigshafen, 558

W. M. Sternberg Jan. 7, 1946

PRINCIPAL DATA ON THE FOAMING PROCESS FOR THE HYDRO-CARBON SYNTHESIS

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Process:

The gas is forced into a sump filled with paraffin produced in the reaction and containing colloidal iron (a filter plate is used with a pore width of 0.15 mm.)

Heat removal:

The sump is cooled by making the contents circulate through a relatively small outside cooler (heat transfer from liquid to liquid). Permissible heat rise 10°C. One sump circuit in about minutes.

Reactor Construction: An empty vertical cylinder 8 mm high which contains in the bottom part a number of foaming plates (of granular quartz, held together by glass). A small vessel, in which the sump is degased, adjoins the reactor.

Catalysts:

Iron from iron carbonyl (or else obtained by precipitation) ground in oil to a particle size of 2 (...).
2 percent alkali (borax) added.
300 - 350 kg Fe/cbm of sump.

Synthesis gas:

CO : H2 = 5 : 4

20 atm. Pressure: 250°C Temperature: 0.30 - 0.35; if the gas is Production: recirculated, with a CO2 scrubber 0.40 - 0.45. - 10 percent Gasol Products: 45 Gasoline, - 200°C Mirdle oil, 200 - 350°C 30 Paraffin, 350°C abt. Gasification, 62 Refined gasoline, O.N. Properties of Refined gasoline, with 0.09 products: 76 percent Pb, O.N. Middle oil (Diesel oil) C.N. 70 75 percent Olefines: gasol 70 gasoline middle oil 175 g liquid and solid products per cbm utilized gas, 160 g liquid and Yields: solld products per nobm ges (90% convers.). 65 percent of the gasoline can be Applications: converted to alcohols by the oxo process (lacquer section). 40 - 50 percent of the middle oil gives sulfonates with HoSO (detergents). 1.5 cbm reactors with seven months Experiments to operation. Longest continuous operdate: ations - three months. No more difficulties are being experienced.

Industrial units; Reactors 8 m high, 2 m diam., 30 cbm capacity, or else reactors 8 m high, 2.5 m diameter, cap. 45 cbm.

New experimental 8 m high reactor: cbm, for

8 m high, diam. 1.50 m, cap. 13.5 cbm. for 5 te/cay.