

INSTITUTE OF GAS TECHNOLOGY  
IIT CENTER  
CHICAGO, ILLINOIS 60616

PREPARATION OF A  
COAL CONVERSION SYSTEMS  
TECHNICAL DATA BOOK

ERDA Contract No. E(49-18)-1730  
Report No. 6  
April 1975

Project 8964 Status Report

for

ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION



INSTITUTE OF GAS TECHNOLOGY - IIT CENTER - CHICAGO 60616

Project Status Report  
for

ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION

Report for

April 1975

Project Title: Preparation of a Coal Conversion Systems Technical  
Data Book

ERDA Contract No.: E(49-18)-1730

I. Project Objective

The objective of this work is to provide a single, comprehensive source of data on coal conversion systems. This compilation shall be entitled The Coal Conversion Systems Technical Data Book and shall provide up-to-date data and information for the research, development, design, engineering, and construction of coal conversion processes and/or plants. Other concurrent objectives are to identify those areas where data are required and to suggest research programs that will provide the required data.

II. Summary

Liquefaction

A number of people were contacted regarding the data book project during the Pittsburgh Symposium on "Catalytic Conversion of Coal." Some data, obtained from Conoco, are being studied.

Gasification

A method is presented for estimating the relative reactivity of coal. Some typical relative reactivities are presented for different ranks of coal.

An example is given, which demonstrates the use of the various steam-oxygen gasification charts presented in previous reports.

**BLANK PAGE**

### Fluidization

The proposed correlation for estimating the minimum fluidization velocity for coal and related materials is presented in graphical form. Two other correlations are also evaluated; they show no improvement over the proposed correlation.

Three other correlations for estimating bed expansion were evaluated by comparison with the available data.

### Combustion

#### Low-Temperature (Fluidized-bed)

A kinetic model is described for sulfur removal from the fluidized-bed combustors.

#### High-Temperature (MHD)

A meeting was arranged with Mr. Bomkamp of Argonne National Laboratory to coordinate its efforts on MHD data collection and evaluation with our plans.

### Coal, Char, and Oil Shale Properties

We have received analytical and other data on 50 large coal deposits from Penn State. It is being prepared for inclusion in the coal properties compilation table.

A list of large deposits in the United States, which are capable of supplying at least 150 million tons of coal over a 20-year period, has been compiled and is presented in this report.

Additional papers on the specific heat of coal and related materials were obtained and are reviewed herein.

### Notice to Readers of Open File

Any comments about the material presented in this report or suggestions about the format and the content of the data book as well as the priorities of the needed data are most welcome. Please direct any communications to Mr. Bipin Almaula of ERDA (202/634-6643) or to Dr. Al Talwalkar of the Institute of Gas Technology (312/225-9600, Ext. 869).

### III. Work Accomplished

#### A. LIQUEFACTION

While attending the "Catalytic Conversion of Coal" symposium in Pittsburgh, we took the opportunity of contacting Dr. E. Donath, consultant, Mr. Willard Bull of Gulf, and personnel from Conoco in Library, Pa. Mr. Walter Lobo, our consultant on the project, accompanied us on the visit to Conoco.

Dr. Donath is not available for evaluating and correlating the coal liquefaction data for the data book, but he may be available for its review and for any consultation. We also tried to enlist the services of Dr. R. Hiteshue in correlating the liquefaction data, but he also is not available at this time.

Mr. Bull indicated that the data from the S. R. C. pilot plant will become available in 1975-76. They are trying to collect information on corrosion, heat transfer, and physical properties. He suggested that correlations between coal liquids and petroleum fractions be included in the data book.

We received some information on properties of solvents, tars, coal, and char from Conoco's data book, which includes the following items:

- a. Estimated density of solvents versus temperature
- b. Estimated viscosities of various cuts versus temperature
- c. Extract-solvent viscosities versus temperature
- d. Heat content of coal and char
- e. Heat content of low-temperature tar fractions
- f. Heating value of coal tar and char
- g. A chart of mean specific heat versus temperature for coke
- h. Latent heats and molecular weights for coal-tar fractions
- i. Specific gravity of tar versus ultimate analysis.

We also received a copy of Design Criteria for Scale-Up of CSF Slurry Preheater developed by Dr. Rutledge of Conoco. This report, as well as other data received from Conoco, is being studied now.

## B. GASIFICATION

### 1. Relative Reactivity Factor for Low-Rate Gasification, $f_o$

The mathematical correlation describing the char gasification kinetics in the low-rate gasification stage, which has been presented in detail in previous monthly reports, is -

$$\frac{dx}{dt} = f_L k_T (1-X)^{2/3} \exp(-\alpha X^2) \quad (1)$$

The parameter,  $f_L$ , is further defined as -

$$f_L = f_o \exp(8467/T_o) \quad (2)$$

where -

$X$  = base carbon conversion fraction

$k_T$  = rate constant which is a function of the gasification temperature  $T$  and the gas composition

$T_o$  = maximum temperature to which char has been exposed prior to gasification, °R (if  $T_o < T$ , then a value of  $T_o = T$  is used)

$f_o$  = relative reactivity factor for low-rate gasification which is a property of the particular coal.

The value of  $f_o$  for different types of coals is based on the definition  $f_o = 1$  for a specific batch of air-pretreated Ireland mine coal. The exponential term in Equation 2 accounts for the effect of the temperature history of the coal being gasified on the gasification reactivity.

The reactivity of a particular coal is a function of the chemical properties of its organic and mineral constituents and of the physical structure of the coal particle. It has been observed in general that the coal reactivity for gasification increases with decreasing coal rank. Efforts are under way to predict the coal gasification reactivity based on the physical and chemical properties of the particular coal.

A standard experimental procedure has been set up to determine both the rapid-rate and low-rate gasification reactivities of coal. At this time, only the procedure for the determination of low-rate gasification reactivity will be outlined.

For constant temperature, pressure, and gas composition, the rate equation (Equation 1) can be integrated with time to yield -

$$M(X) = \int_{X_0}^{X_F} \frac{\exp(\alpha X^2)}{(1-X)^{2/3}} dX = f_L k_T t \quad (3)$$

where

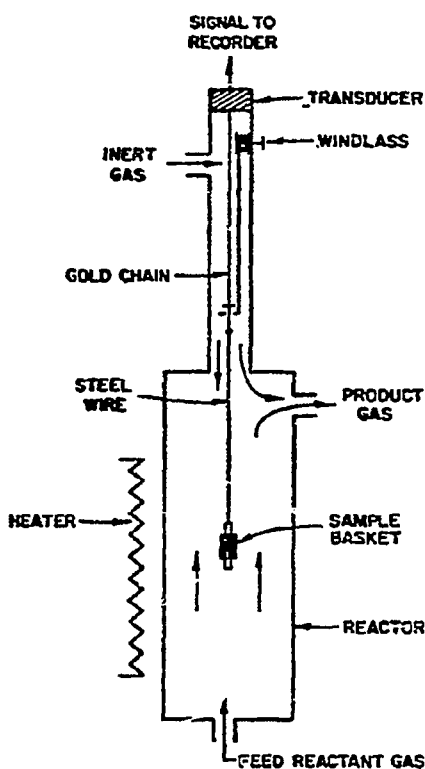
$X_F$  = base carbon conversion fraction at final time,  $t$

$X_0$  = base carbon conversion fraction at time  $t = 0$ , this value for devolatilized coal = 0

A plot of  $M(X)$  versus  $t$  yields a straight line with a slope of  $f_L k_T$ . To obtain the quantitative information needed to plot  $M(X)$  versus  $t$ , the test coal sample is gasified in an apparatus known as a thermobalance at the standard conditions - gasification with hydrogen at a temperature of 1700 °F and a pressure of 35 atm.

The thermobalance is an apparatus capable of continuously weighing a coal sample that is undergoing reaction in a gaseous environment of desired composition and at a constant pressure. The temperature can either be kept constant or varied; 10° F/min is the maximum rate for the apparatus used at IGT. A schematic of the thermobalance apparatus is shown in Figure 1. The coal sample is contained in the annular space of a wire-mesh basket bounded on the inside by a hollow, stainless-steel tube and on the outside by a wire-mesh screen. To facilitate mass and heat transfer between the bed and its environment, the thickness of the bed is only 2 to 3 particle diameters when using -20+40 U. S. sieve-size particles. Gas flow rates used with this system are sufficiently large relative to gasification rates so that gas conversion is limited to less than 1% for devolatilized coal char.

The following is a typical test procedure: The wire-mesh basket is initially in an upper, cooled portion of the reactor in which a downward, inert gas flow is maintained. During this time the desired temperature and pressure conditions are established in a lower heated portion of the reactor in the presence of a flowing gas. A test is initiated by lowering the basket into the heated reaction zone, a procedure which takes 5 to 6 seconds. Theoretical computation indicates that about 1 to 2 minutes are required for the sample to achieve reactor temperature, as measured by several thermocouples surrounding the basket in the reaction zone. This computation is reasonably



A-112-1009

Figure 1. DIAGRAM OF THERMOBALANCE REACTOR

corroborated by various kinetic indications and by the behavior of the thermocouples in reattaining their preset temperatures. The sample is kept in the heated portion of the reactor for the specified time while its weight is continuously recorded. The test is terminated by raising the basket back to the upper, cooled portion of the reactor.

During a test, the dry feed gas flow rates are measured by an orifice meter and the dry product gas flow rates by a wet-test meter. Periodic samples of product gas are taken to determine the dry gas' composition by mass spectrography.

For determining the low-rate gasification reactivity, the coal sample is initially exposed to a nitrogen atmosphere at a temperature of 1700°F prior to exposure to a hydrogen atmosphere. During this period, the volatile



matter in the coal sample is essentially removed and at the same time the tendency to undergo rapid-rate methane formation is destroyed. The resulting devolatilized coal is then exposed to hydrogen at 1700° F and 35 atm for a desired period of time during which the low-volatile carbon reacts with hydrogen.

The value of the slope of the plot of  $M(X)$  versus  $t$  for the standard Ireland mine pretreated coal can be calculated at the standard test conditions of 1700° F and a hydrogen gas pressure of 35 atm. ( $k_T$  is calculated from the rate constant equations given in the February 1975 Report,  $\exp 8467/T_0$  is equal to 50.4, and  $f_0 = 1$  by definition.) The thermobalance yields the weight loss information from which the  $M(X)$  versus  $t$  plot can be constructed and the slope of the straight line obtained. Dividing the experimental value of the slope for the test coal by the calculated value of the slope for the standard coal yields the value of  $f_0$  for the test coal.

Table 1 shows the approximate ranges of the relative low-rate gasification reactivity factors for different ranks of coal. These values are from previous work that has been performed at IGT and may be used in conjunction with the design charts presented in previous monthly reports. These results do not, however, generally apply to lignites, which show a wide variability in reactivity due to inherent catalytic effects of certain mineral components which predominate at this level of rank. With lignites, therefore, experimental determination of reactivity factors is usually necessary.

Table 1. RELATIVE LOW-RATE GASIFICATION REACTIVITY FACTORS

Carbon Content of Raw Coals (Dry, Ash-Free), wt%	Low-Rate Gasification Reactivity Factor, $f_0$
65-70	1.4-1.3
70-75	1.3-1.2
75-80	1.2-1.0
80-85	1.0-0.8
85-90	0.8-0.6
90-95	0.6-0.3

## 2. Example

This example shows the use of the design charts presented up to now for the fluidized-bed steam-oxygen gasification of char.

A fluidized-bed gasifier must be designed to produce synthesis gas from a char feed that has been devolatilized and partially gasified. The appropriate conditions of operation are taken to be 1850°F, 70 atm, and a steam-to-carbon feed ratio of 1.2. Ninety percent of the feed carbon has to be gasified, with the heat for gasification being supplied by burning part of the coal with oxygen. Assume that the coal is in plug flow and the gases are backmixed.

The following information on the coal feed is available:

- a. Ultimate and proximate analysis of fresh coal before partial gasification is —

	<u>wt %, dry</u>		<u>wt %</u>
C	67.5	Volatile Matter	36.9
H <sub>2</sub>	4.6	Fixed Carbon	52.1
O	18.5	Ash	7.5
N <sub>2</sub>	0.9	Moisture	<u>3.5</u>
S	0.7		100.0
Ash	<u>7.8</u>		
	100.0		

- b. The ultimate analysis of the partially gasified char to the steam-oxygen gasifier is —

	<u>wt %</u>
C	78.0
H <sub>2</sub>	1.2
O	--
N <sub>2</sub>	1.1
S	0.6
Ash	<u>19.1</u>
	100.0

- c. The rate of char feed to the gasifier is 500 lb/hr.

#### Solution

Because the feed to the gasifier is a partially gasified char, the initial base carbon conversion fraction,  $X_0$ , is not equal to zero but has some value, which is calculated as follows:

$$\begin{aligned}
 C_{b^0} \text{ (base carbon), the carbon} \\
 \text{in the fixed carbon fraction} &= 0.96 \times \text{fixed carbon fraction of feed coal} \\
 &= 0.96 \times \frac{0.521}{1.000 - 0.035} \\
 &= 0.518 \text{ lb carbon/lb raw coal (dry)}
 \end{aligned}$$

This approximation is used when an estimate of the organic coal components present in the fixed carbon fraction is not available.

The fraction of base carbon,  $C_b$ , in the partially gasified char, may be obtained by an ash balance.

$$\begin{aligned}
 C_b &= \frac{0.078}{0.78} \frac{\text{lb ash}}{\text{lb raw coal}} \times \frac{1}{0.191} \frac{\text{lb partially gasified char}}{\text{lb ash}} \\
 &\quad \times 0.78 \frac{\text{lb carbon}}{\text{lb partially gasified char}} \\
 &= 0.318 \text{ lb carbon/lb raw coal}
 \end{aligned}$$

Thus, the initial base carbon conversion fraction is -

$$\begin{aligned}
 X_o &= \frac{C_b^o - C_b}{C_b^o} \\
 &= \frac{0.518 - 0.318}{0.518} = 0.39
 \end{aligned}$$

Note: These calculations are shown with a block diagram in Figure 2 for convenience. Charts presented in previous monthly reports are reproduced here as Figures 3 to 6; an open circle on each of them indicates the values read for this example.

Using the graph in Figure 3 for 1850°F, 90% feed carbon conversion, and a steam-carbon ratio of 1.2, the following are read:

$\theta_b$ , the base case char residence time = 80 min.

Oxygen feed requirements = 0.23 lb-mole/lb-mole feed carbon.

Three corrections must be applied to the base case residence time:

1. Reactivity Correction: The relative low-rate gasification reactivity for the feed coal is read from Table 1 to be 1.2. The char residence time is inversely proportional to  $f_o$  and, therefore -

$$M_{f_o}, \text{ correction factor for reactivity} = 1/f_o = 1/1.2 = 0.833$$

2. Partially gasified char feed correction: To use the chart in Figure 4, a corrected carbon conversion fraction, Y, must be calculated:

$$Y = \left( \frac{\text{total carbon gasified}}{\text{carbon in feed}} - \frac{\text{oxygen}}{\text{carbon in feed}} \right), \text{ in mole/mole} = 0.9 - 0.23 = 0.67$$

From Figure 4,  $M_{X_o} = 1.22$ .

3. Solids plug-flow model correction: Using Figure 5, for initial carbon conversion fraction  $X_o = 0.39$ , and the "corrected" final carbon conversion fraction  $Y = 0.67$ ,  $R = 0.63$ .

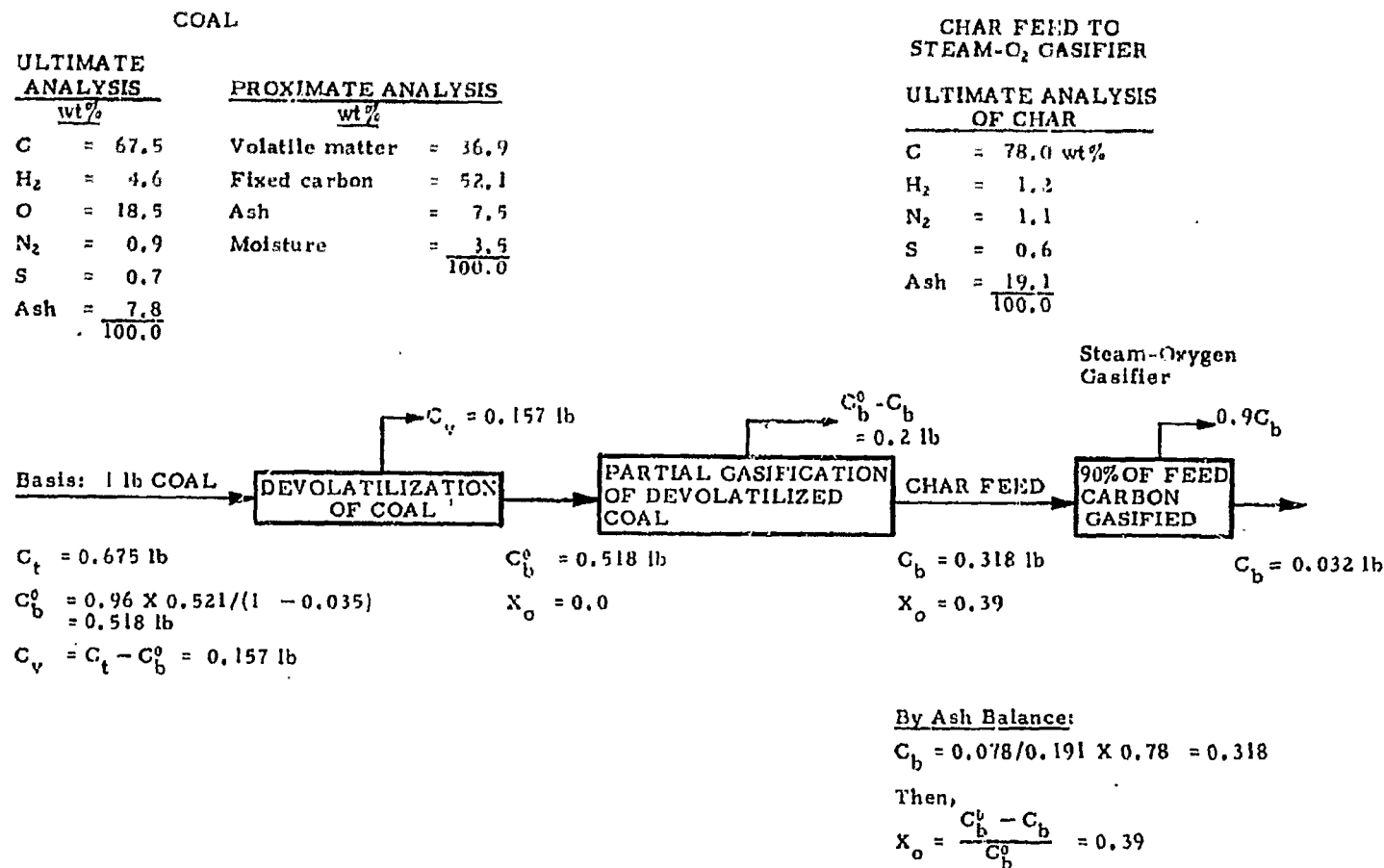


Figure 2. BLOCK DIAGRAM OF HISTORY OF THE CHAR FEED USED IN THE STEAM-OXYGEN GASIFIER

A7505/124



ERDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____

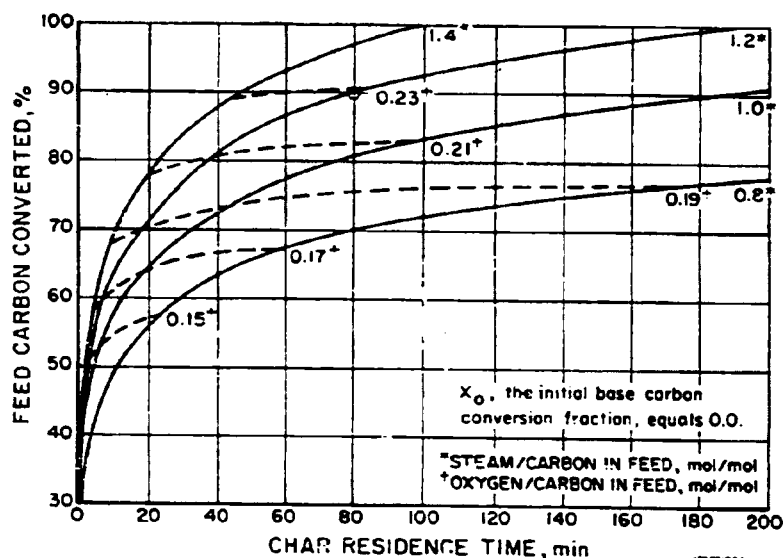


Figure 3. STEAM-OXYGEN GASIFICATION OF DEVOLATILIZED IRELAND MINE BITUMINOUS CHAR AT 1850° F AND 70-atm PRESSURE

The corrected char residence time,

$$\begin{aligned}\theta &= \theta_b \times M_f \times M_{X_0} \times R \\ &= 80 \times 0.833 \times 1.22 \times 0.63 \\ &= 51 \text{ min}\end{aligned}$$

The total product gas moles and the product gas composition is obtained from Figure 6.

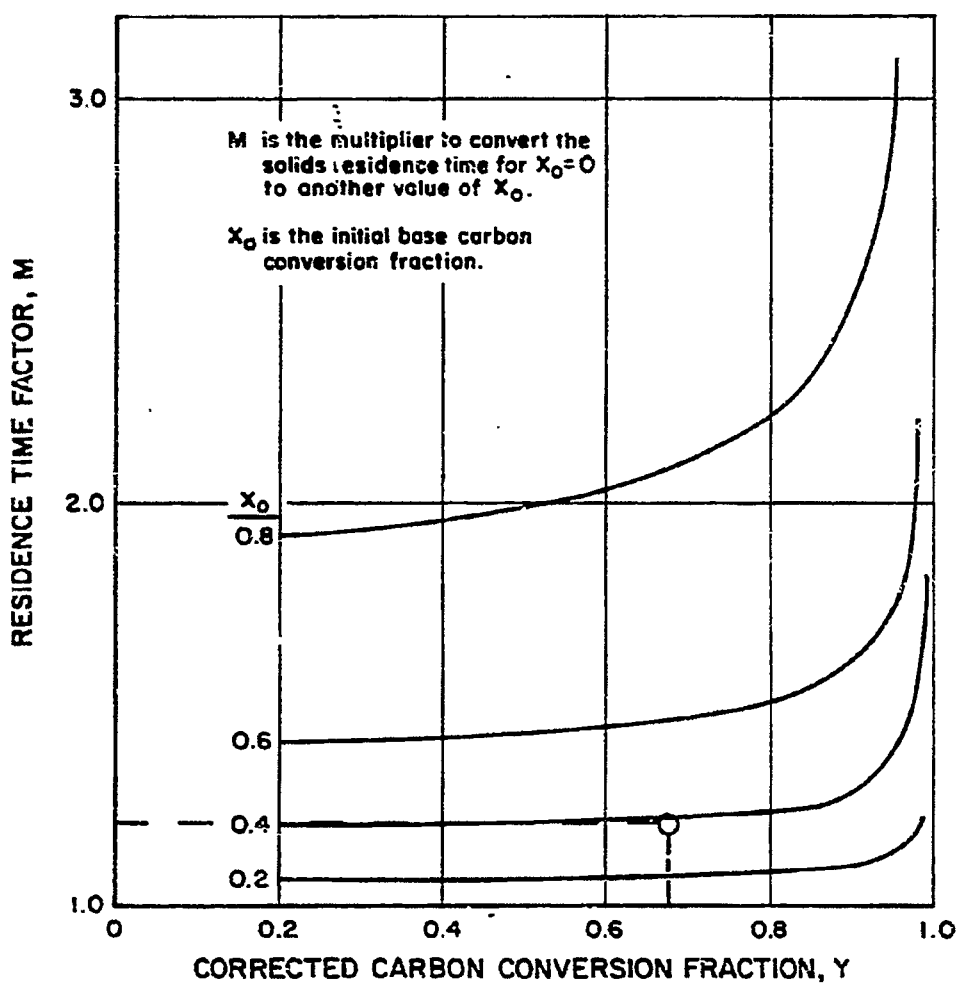
$$\begin{aligned}\text{Total moles of product gas} &= 1.88 \frac{\text{moles gas}}{\text{moles C feed}} \times \frac{500(0.78)}{12.01} \frac{\text{moles C feed}}{\text{hr}} \\ &= 61.05 \text{ lb-moles/hr}\end{aligned}$$

Product gas composition —

	mol %
CH <sub>4</sub>	4.5
CO	26.0
CO <sub>2</sub>	15.0
H <sub>2</sub>	26.5
H <sub>2</sub> O	28.0
	100.0



ERDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____



A75051084

Figure 4. CONVERSION FACTOR FOR PARTIALLY GASIFIED CHAR FEED



ERDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____

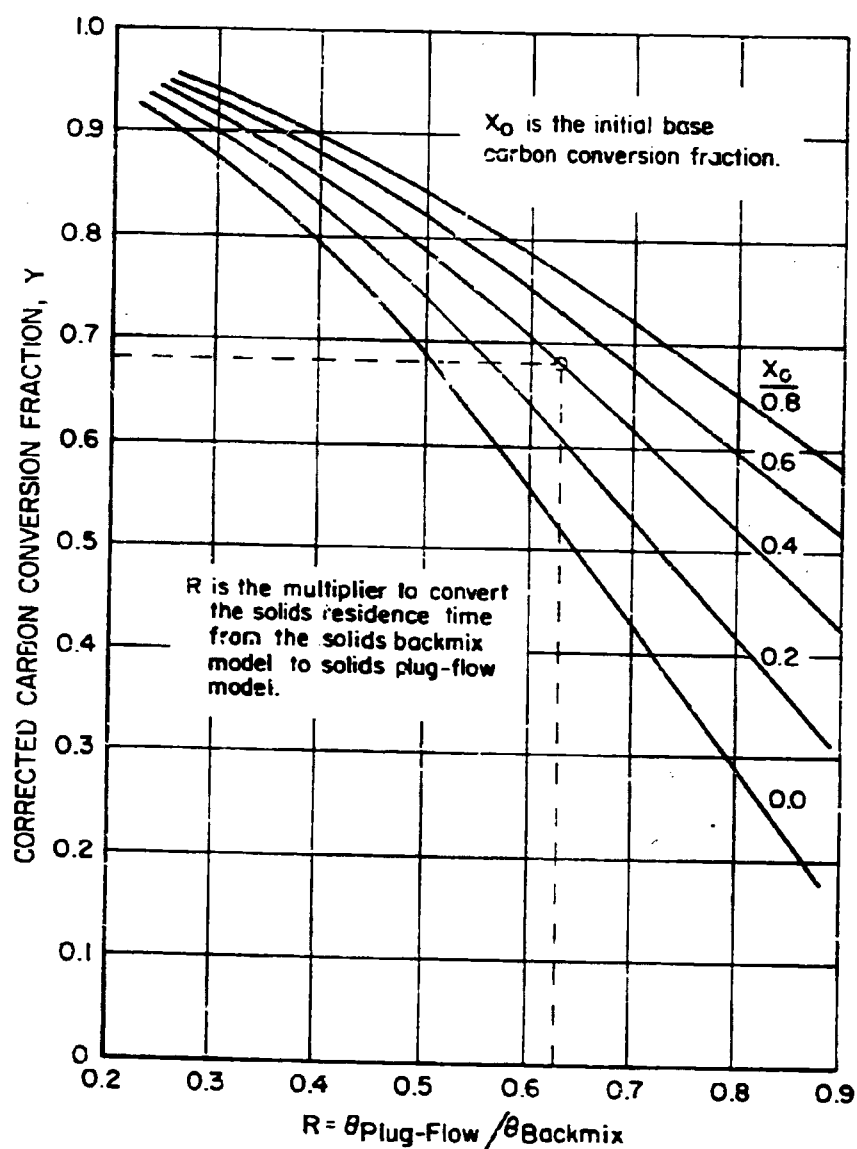


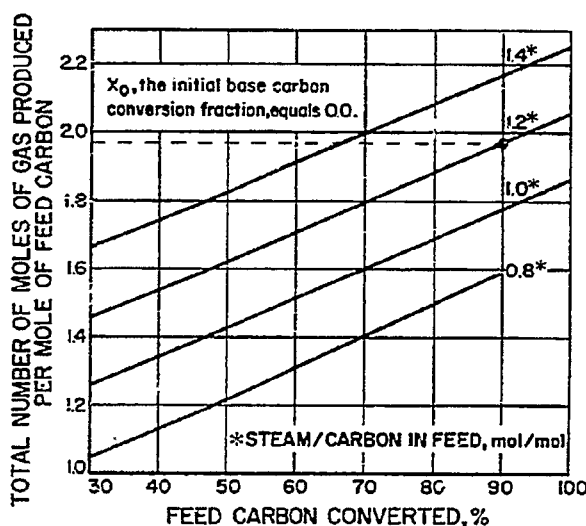
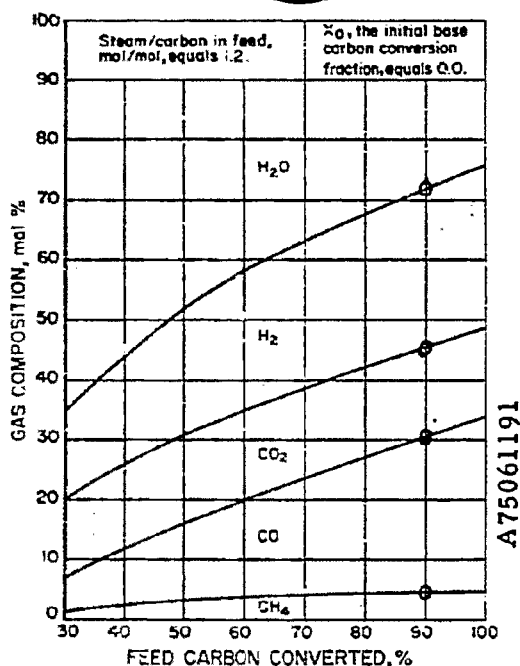
Figure 5. CONVERSION FACTOR FOR PLUG-FLOW MODEL

4/75



8964

ERDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____



A. Gas Composition

B. Total Moles of Gas Produced

Figure 6. STEAM-OXYGEN GASIFICATION - PRODUCT GAS COMPOSITIONS AT 1850°F AND 70-atm PRESSURE

$$\text{Total oxygen required} = 0.23 \frac{\text{mole O}_2}{\text{mole C feed}} \times \frac{500(0.78)}{12.01} \frac{\text{moles C feed}}{\text{hr}}$$

$$= 7.47 \text{ moles/hr}$$

$$\text{Total steam required} = 1.2 \frac{\text{moles steam}}{\text{mole C feed}} \times \frac{500(0.78)}{12.01} \frac{\text{mole C feed}}{\text{hr}}$$

$$= 38.97 \text{ moles/hr}$$

$$\text{Total carbon gasified} = \frac{500(0.78)}{12.01} \times 0.9$$

$$= 29.23 \text{ moles/hr}$$

$$\text{Residue from the gasifier} = \text{lb char feed} - \text{lb carbon gasified}$$

$$= 500 - 500(0.78) \times 0.9$$

$$= 149 \text{ lb/hr}$$



Knowing the required char residence time in the gasifier, the fluidized-bed height may be obtained as follows:

$$\text{Fluidized-bed height} = \frac{W_{\text{avg}} \times \theta}{\rho_b \times A}$$

where —

$\theta$  = char residence time, hr

$\rho_b$  = density of the fluidized bed, lb/ft<sup>3</sup> (may be obtained from known correlations)

$A$  = fluidized-bed cross-sectional area, ft<sup>2</sup> (fixed by the design gas velocity in the fluidized bed)

$W_{\text{avg}}$  = the average-weight flow rate of char, lb/hr

This last component,  $W_{\text{avg}}$ , may be approximated, for moderate conversions, for the plug-flow model as —

$$W_{\text{avg}} = \frac{\text{char feed rate} + \text{corrected residue rate}}{2}$$

where the corrected residue rate is the residue entering the combustion zone of the fluidized bed, that is —

$$\begin{aligned} \text{Corrected residue rate} &= \text{residue out of gasifier} + \text{C combusted by O}_2 \text{ feed} \\ &= 149 + 7.47 \times 12.01 \\ &= 239 \text{ lb/hr} \end{aligned}$$

Therefore,

$$W_{\text{avg}} = \frac{500 + 239}{2} = 369.5 \text{ lb/hr}$$

If it had been assumed that the solids were in backmixed flow, the solids plug-flow model correction would not have been required and the residence time would have been

$$\begin{aligned} \theta &= \theta_b \times M_{f_o} \times M_{X_o} \\ &= 80 \times 0.833 \times 1.22 \\ &= 81.3 \text{ min} \end{aligned}$$

$$\begin{aligned} \text{and fluidized-bed height} &= \frac{W_{\text{out}} \times \theta}{\rho_b \times A} \\ &= \frac{239 \times 81.3}{\rho_b A} \end{aligned}$$

### C. FLUIDIZATION

#### 1. Evaluation of Minimum Fluidization Correlations

##### a. Broadhurst-Becker Correlation

The following empirical correlation developed by Broadhurst and Becker<sup>2</sup> was evaluated in a manner similar to the procedure reported in the previous monthly reports.

$$U_{mf}^2 = \frac{D_p g (\rho_s - \rho_g)}{\rho_g} \cdot \frac{1}{2.42 \times 10^5 \left[ \frac{\mu^2}{D_p^3 g (\rho_s - \rho_g) \rho_g} \right]^{0.85} + \left( \frac{\rho_s}{\rho_g} \right)^{0.13} + 37.7} \quad (1)$$

for

$$0.01 < Re_{mf} < 1000$$

$$500 < \frac{\rho_s}{\rho_g} < 50,000$$

and

$$1 < D_p^3 \rho_g \cdot \frac{g(\rho_s - \rho_g)}{\mu^2} < 10^7$$

A graphical comparison of the calculated minimum fluidization velocity values from Equation 1 with published experimental data on coal and related materials is shown in Figure 7. It is seen from this figure that the calculated values are generally lower than the measured minimum fluidization velocity values.

##### b. Zenz Correlation

A similar comparison was also made by solving for the minimum fluidization velocity from the following empirical equation,<sup>16</sup> fitted to the graphical correlation developed by Zenz.<sup>17</sup>

$$\epsilon_{mf} = 1.4673081 + 0.0147726 (\beta) - 0.26864208 (\ln \alpha) + 0.18601248 (\ln \beta) + 0.00814086 (\ln \beta)^2 \quad (2)$$

where

$$\alpha = \frac{D_p}{\left[ \frac{3}{4} \cdot \frac{\mu^2}{\rho_g (\rho_s - \rho_g) g} \right]^{1/3}} \quad (3)$$

$$\beta = \frac{U_{mf}}{\left[ \frac{4}{3} \cdot \frac{\mu (\rho_s - \rho_g) g}{\rho_g^2} \right]^{1/3}} \quad (4)$$

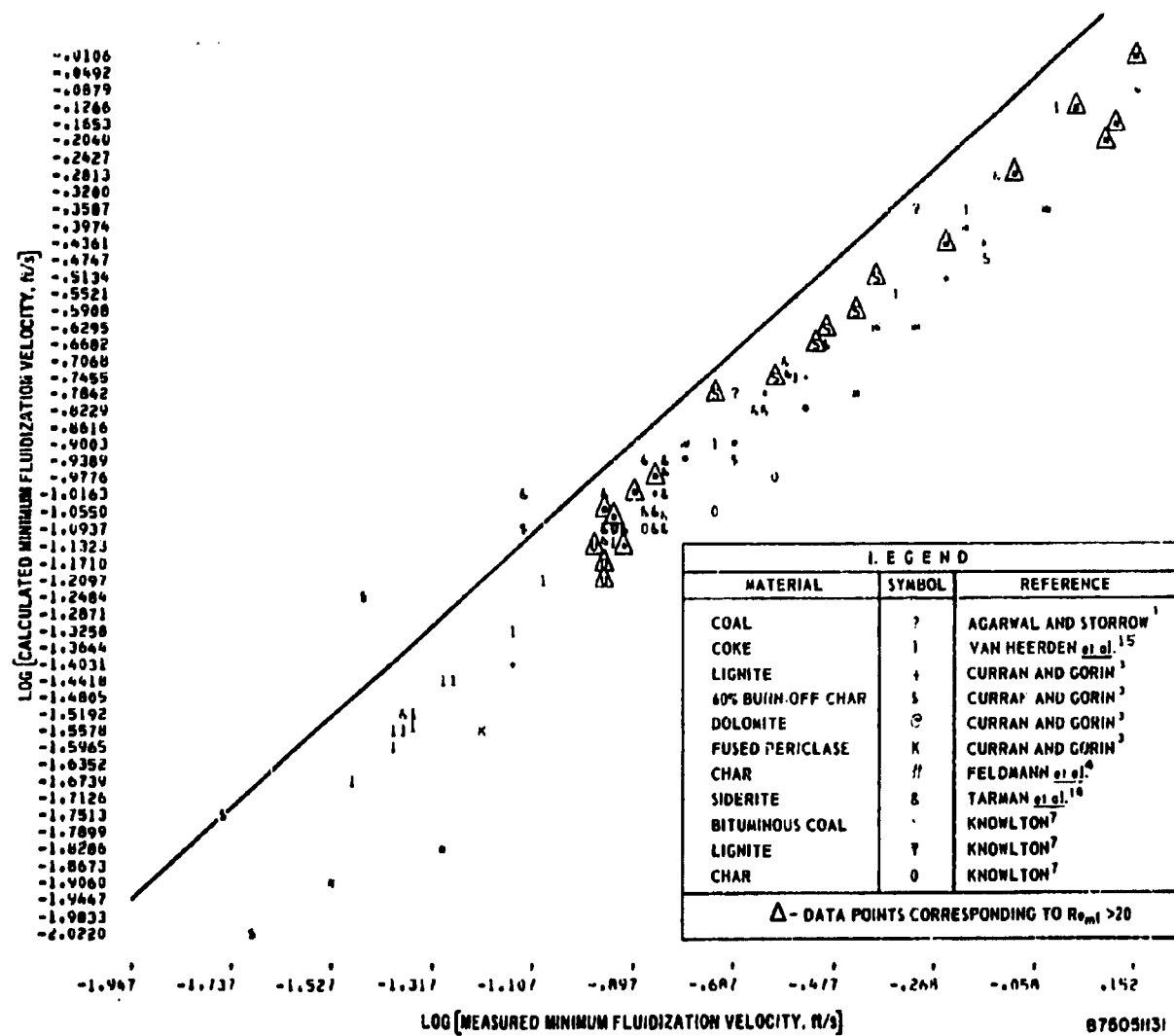
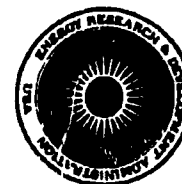


Figure 7. COMPARISON OF BROADHURST-BECKER'S CORRELATION WITH MEASURED MINIMUM FLUIDIZATION DATA



4/75

ERDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____

8964

The comparison of the calculated values using Equation 2 with the published data used in this investigation is shown in Figure 8.

The calculated standard relative deviations for the correlations given by Equations 1 and 2 are -

a. Broadhurst-Becker, <sup>2</sup>	36.04
b. Zenz, <sup>16</sup>	113.29 %

It must be recognized that even though Broadhurst and Becker<sup>2</sup> used the data of particles ranging in density from 81 to about 463 lb/cu ft, the particles were usually spherical; conceivably, therefore, the empirical constants in Equation 1 may not be fully descriptive of the physical characteristics of coal and the related types of material used in this investigation.

It is apparent that by employing the empirical equation (Equation 2), the percent standard relative deviation is lower than when the values are calculated by the graphical readout procedure reported earlier.<sup>6</sup> The magnitude of the standard relative deviation is still a reminder that Zenz's graphical correlation<sup>17</sup> is sensitive to the bed voidage at minimum fluidization velocity and was developed primarily for the particulate fluidization of particles that are generally spherical in shape.

Studies similar to this will be made and reported whenever new correlations become available.

#### c. Proposed Correlation

The proposed correlation given in last month's report is plotted in Figure 9, where  $Re_{mf}$  is given as a function of Galileo's number. It should be recalled that this correlation was developed by determining the parameters  $1/\phi \cdot \epsilon_{mf}^3$  and  $(1 - \epsilon_{mf})/\phi^2 \cdot \epsilon_{mf}^3$  from the available data by nonlinear regression analysis.

However, if the shape factor,  $\phi$ , and the minimum fluidization voidage,  $\epsilon_{mf}$ , can be precisely determined for the system under study, a better estimation of the minimum fluidization velocity can presumably be obtained by substituting these values in the original Kunii-Levenspiel equation:<sup>8</sup>

$$\frac{1.75}{\phi \cdot \epsilon_{mf}^3} (Re_{mf})^2 + \frac{150(1 - \epsilon_{mf})}{\phi^2 \cdot \epsilon_{mf}^3} \cdot Re_{mf} - Ga = 0 \quad (5)$$

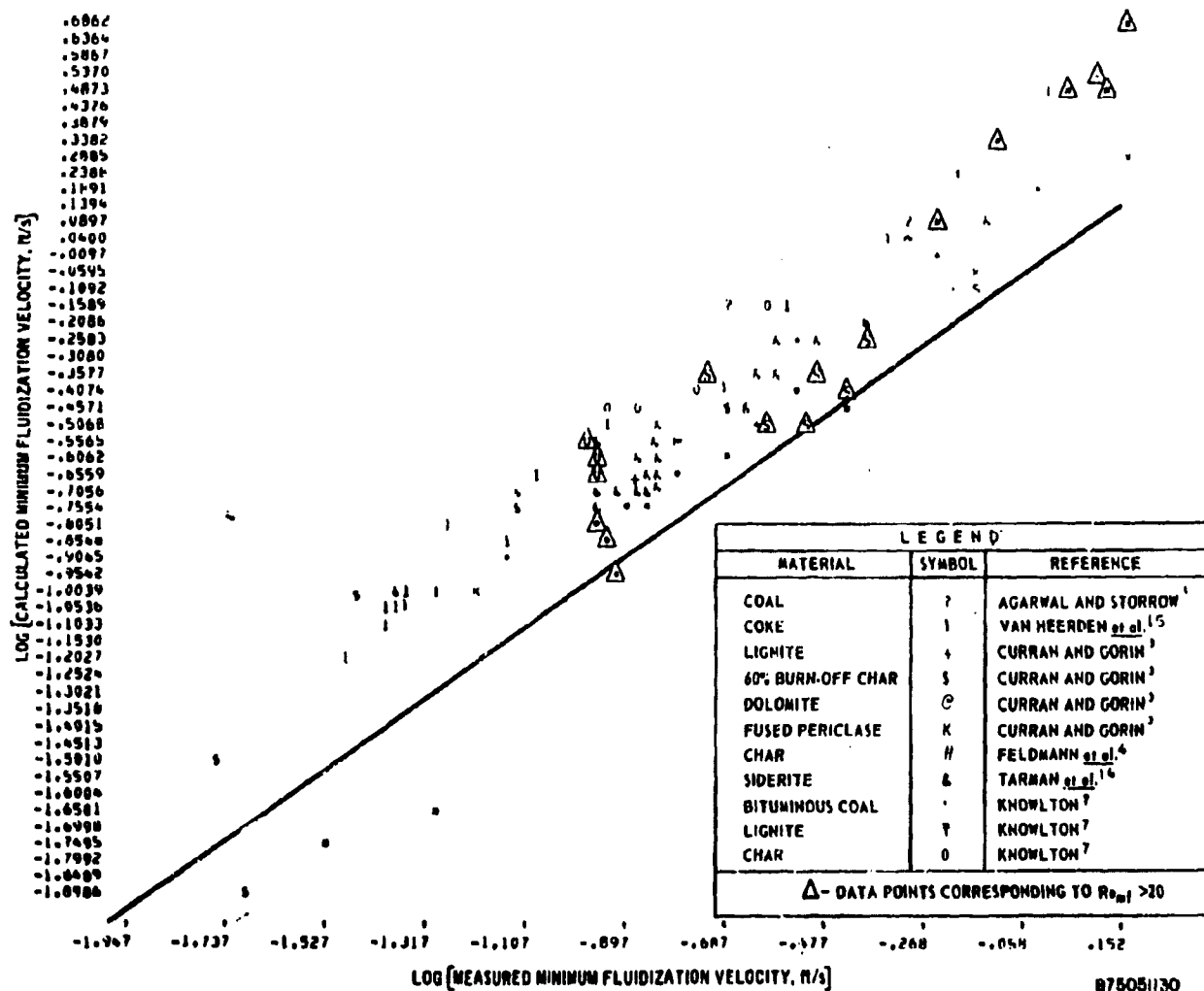
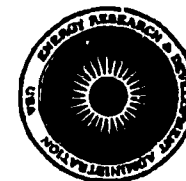


Figure 8. COMPARISON OF ZENZ'S CORRELATION WITH MEASURED MINIMUM FLUIDIZATION DATA



ERDA
PAGE
REVISION No.
DATE



ERDA \_\_\_\_\_  
 PAGE \_\_\_\_\_  
 REVISION No. \_\_\_\_\_  
 DATE \_\_\_\_\_

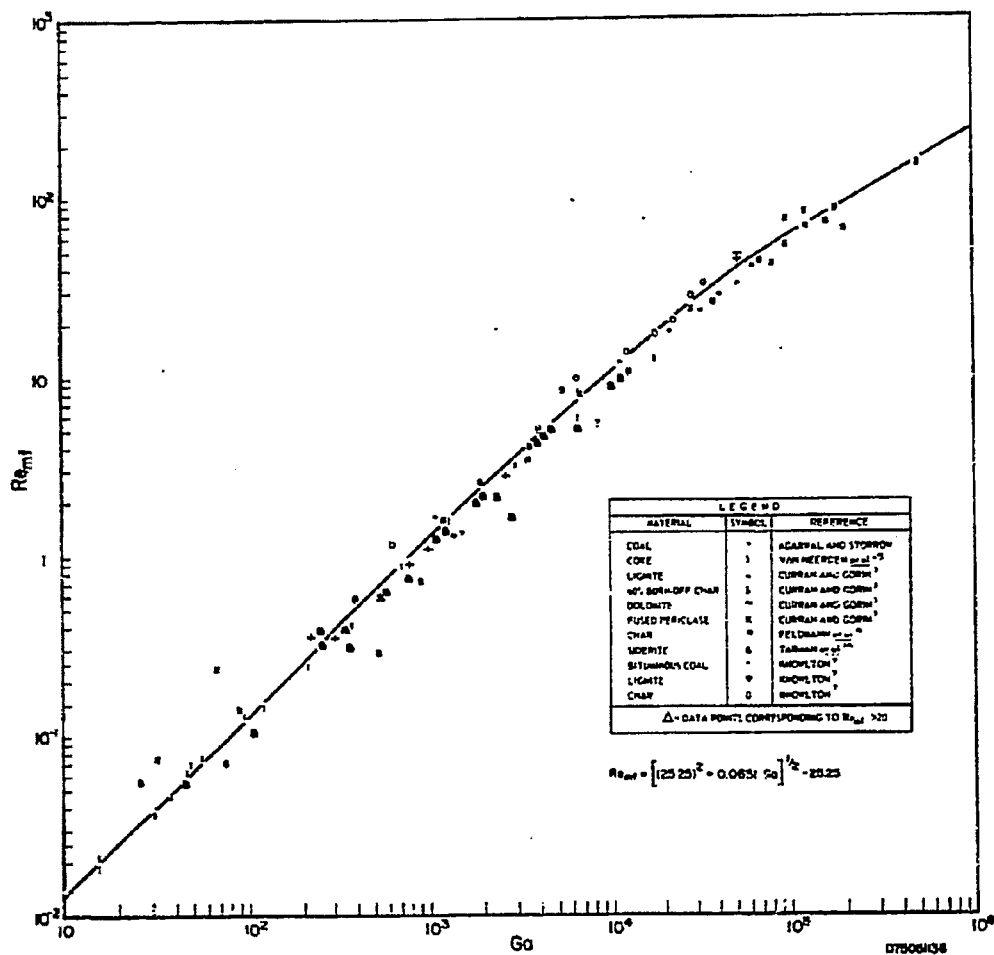


Figure 9. PROPOSED CORRELATION FOR THE PREDICTION OF MINIMUM FLUIDIZATION VELOCITY

But the values of  $\phi$  and  $\epsilon_{mf}$  are generally not available with any acceptable degree of precision, and hence it is recommended that the proposed correlation be used to estimate the minimum fluidization velocity for coal and related materials.

## 2. Bed Expansion on Fluidization

The two-phase theory<sup>8</sup> postulates that the gas in excess of the minimum fluidization velocity will traverse the bed height in the form of gas bubbles. The literature published on fluidization during the last decade can be broadly divided into two groups: those in support of the two-phase theory and those against the generalization of the two-phase theory principles. However, from a theoretical point of view, it is conceivable that the bed expansion ratio is related to the gas flow in excess of the minimum fluidization velocity.

### a. Lewis et al. Correlation

The correlation developed by Lewis et al.<sup>12</sup> was one of the first to relate the bed expansion ratio ( $L_f/L_{mf}$ ) to the difference in superficial gas velocity at the fluidizing and minimum fluidizing conditions. The empirical relationship developed by these investigators is given by —

$$\frac{L_{mf}}{L_f} = 1 - \frac{0.188}{D_p^{0.5}} (U - U_{mf}) \quad (6)$$

A graphical comparison of the calculated fluidized-bed expansion ratio from Equation 6 with the measured bed expansion data is shown in Figure 10. It is seen that about 90% of the published data are within  $\pm 20\%$  of the values calculated from Equation 6.

The data by Tarman et al.<sup>14</sup> show a uniquely different trend compared with the rest of the data in Figure 10. Their measured bed expansion ratios are lower than those calculated from Equation 6, indicating the generally accepted effect of the column diameter. Clearly, the Lewis et al. correlation predicts a lower bed expansion for most of the cases except for the Tarman et al. system. The reasons for this discrepancy are not clear because no definite and physically pertinent trends could be rationalized by grouping the data in Figure 10 into different density groups, particle sizes, or operating pressures or into fluidizing columns of the same diameters.

CALCULATED EXPANSION RATIO,  $L_f/L_i$



4175



ERDA \_\_\_\_\_  
PAGE \_\_\_\_\_  
REVISION No. \_\_\_\_\_  
DATE \_\_\_\_\_

8964



### b. Shen-Johnstone Correlation

A modification of the Lewis et al. correlation for the bed expansion ratio was published by Shen and Johnstone<sup>13</sup> in the following form:

$$\frac{L_f}{L_{mf}} = 1 + \frac{0.0188}{D_p^{0.5}} (U - U_{mf}) \quad (7)$$

This modification was developed to describe their experiments with a cracking catalyst in a fluidized bed, 3.75 inches in diameter.

A comparison of the calculated bed expansion characteristics with the measured values as a function of the gas velocity, taken from the literature, is shown in Figure 11. About 90% of the measured data is within  $\pm 20\%$  of the calculated values from the Shen-Johnstone correlation. As seen in Figure 10, the data reported by Tarman et al.<sup>14</sup> show a trend different from the majority of the data in Figure 11. Also, the values calculated by the Shen-Johnstone correlation for the lighter materials (such as lignite and some chars) are less than 80% of the measured values.

### c. Leva et al. Correlation

Using the empirical correlation for minimum fluidization and assuming uniform particles and therefore uniform voidage in the fluidized bed, Leva et al.<sup>9,11</sup> related the mass velocity of the fluidizing medium to the fractional volume of voids by the following equation:

$$G \propto \left( \frac{1 - \delta}{\delta^3} \right)^m \quad (8)$$

Frantz<sup>5</sup> later summarized the following procedure to predict the fluidized-bed expansion characteristics using Leva's derivations:

- Step 1. Predict  $G_{mf}$  from the Leva et al. correlation<sup>10</sup>
- Step 2. Estimate  $\epsilon_{mf}$  from Figure 12.
- Step 3. Obtain slope  $m$  from Figure 13.
- Step 4. Plot  $G_{mf}$  and  $(1 - \epsilon_{mf})/\epsilon_{mf}^3$  on logarithmic coordinates.
- Step 5. Draw line of slope  $m$  through  $G_{mf}$ ,  $(1 - \epsilon_{mf})/\epsilon_{mf}^3$ , as shown in Figure 14. (Note:  $\epsilon_{mf} = \delta$  at incipient fluidization conditions.)
- Step 6. Estimate the fluidized-bed expansion characteristics from Figure 14.

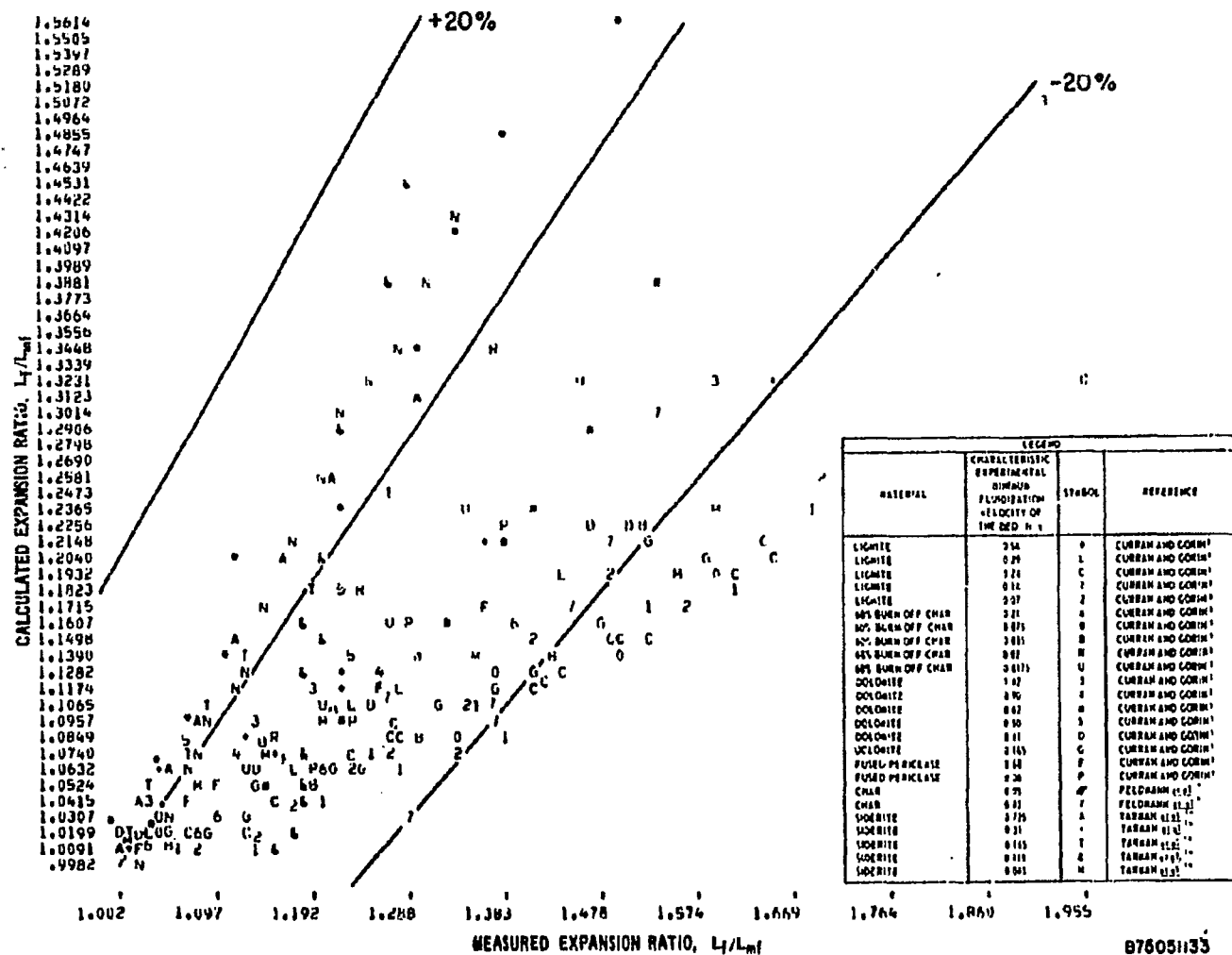
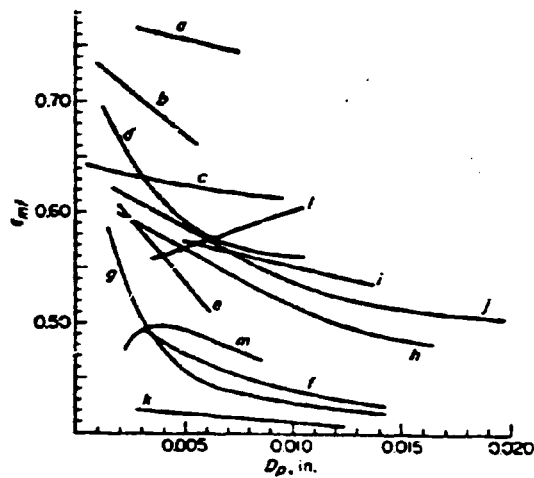


Figure 11. COMPARISON OF SHEN-JOHNSTONE CORRELATION WITH MEASURED BED EXPANSION DATA



ERDA  
PAGE  
REVISION No.  
DATE



LEGEND			
MATERIAL	SYMBOL	REFERENCE	
SOFT BRICK	A	AGARWAL AND STORROW :	
ABSORPTION CARBON	B	AGARWAL AND STORROW :	
BROKEN RASCHIG RINGS	C	AGARWAL AND STORROW :	
COAL AND GLASS POWDER	D	AGARWAL AND STORROW :	
CARBONHOLDS	E	AGARWAL AND STORROW :	
SAND	F	AGARWAL AND STORROW :	
ROUND SAND	• 0.86	C	LELA et al. :
SHARP SAND	• 0.67	H	LELA et al. :
FISCHER-TROPSCH CATALYST	• 0.58	I	LELA et al. :
ANTHRACITE COAL	• 0.65	J	LELA et al. :
MIXED ROUND SAND	• 1.86	K	LELA et al. :
COKE	L	VAN HEERDEN et al. :	
CARBONHOLDS	M	VAN HEERDEN et al. :	

A75051125

Figure 12. RELATION OF INCIPIENTLY FLUIDIZED-BED VOIDAGE TO THE AVERAGE PARTICLE DIAMETER

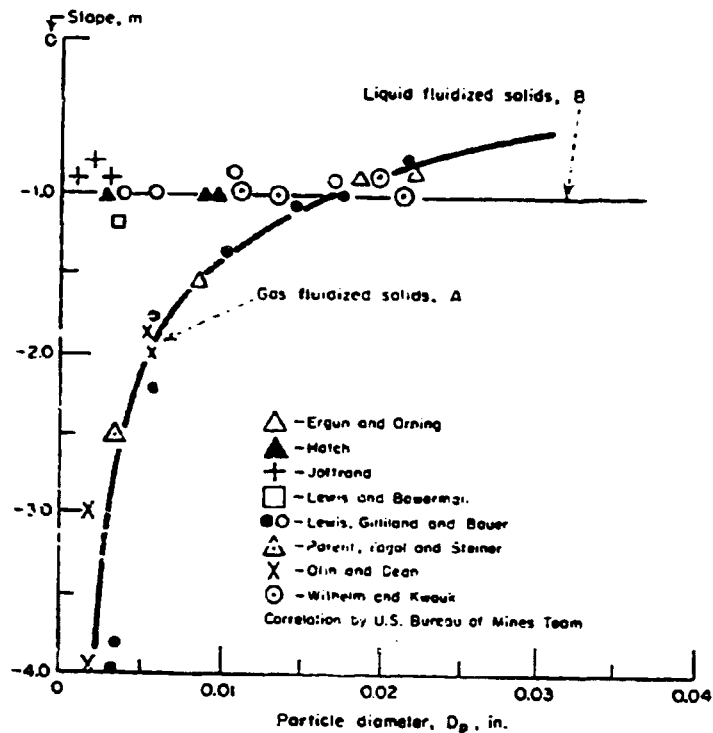


Figure 13. VALUES OF  $m$  IN RELATION TO  $D_p$



EFDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____

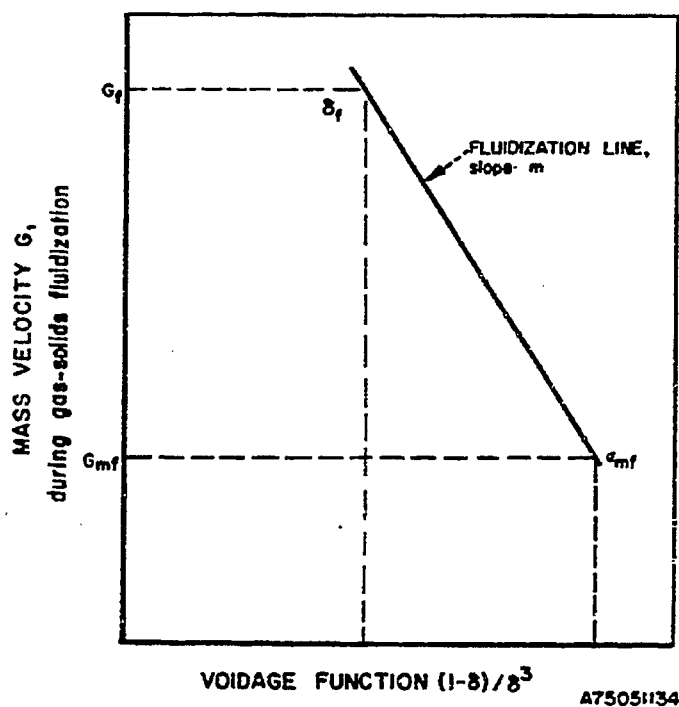


Figure 14. BEHAVIOR OF EXPANDED BED<sup>9</sup>

Frantz<sup>5</sup> also notes that the Leva et al. correlation can predict the expansion characteristics as long as the voids are uniformly distributed in fluidized beds. He estimates that beyond a fractional volume of voids equal to 0.65, the fluidized bed becomes heterogeneous, and therefore the Leva et al. correlation may not result in adequately reliable values.

A comparison of the calculated fluidized-bed expansion characteristics using Leva's procedure with the published data used in this investigation is shown in Figure 15. Leva's procedure of calculating bed expansion ratio produces values that compare with 90% of the data within  $\pm 20\%$  deviation. No definite trend descriptive of density, particle size, or the diameter of the fluidizing column is noticed in Figure 15.

It can be visualized that the fluidized-bed expansion characteristics are not only related to the physical properties of the solids and gases but also to the fluidized-bed diameter in some complex manner. The evaluation of these correlations gives no insight into the phenomena of fluidized-bed expansion. We anticipate that the analysis of correlations incorporating bubble properties and bubble inventory will produce a better description of the published data. However, such an analysis will not be attempted until we complete work on the section on bubble properties in gas-solid fluidized beds.

Specific recommendations regarding the use of published correlations to estimate the fluidized-bed expansion characteristics in coal conversion will be proposed in the future monthly reports.

### 3. Nomenclature

$D_f$  = particle diameter of a sieved fraction, ft

$D_p$  = average particle diameter, ft =  $\frac{1}{\sum(X/D_p)}$

$g$  = gravitational constant, ft/s<sup>2</sup>

$G$  = superficial mass velocity, lb/ft<sup>2</sup>·s

$Ga$  = Galileo number =  $g \frac{D_p^3(\rho_s - \rho_g) \rho_g}{\mu^2}$

$L_f$  = height of fluidized bed, ft

$L_{mf}$  = height of minimum fluidized bed, ft

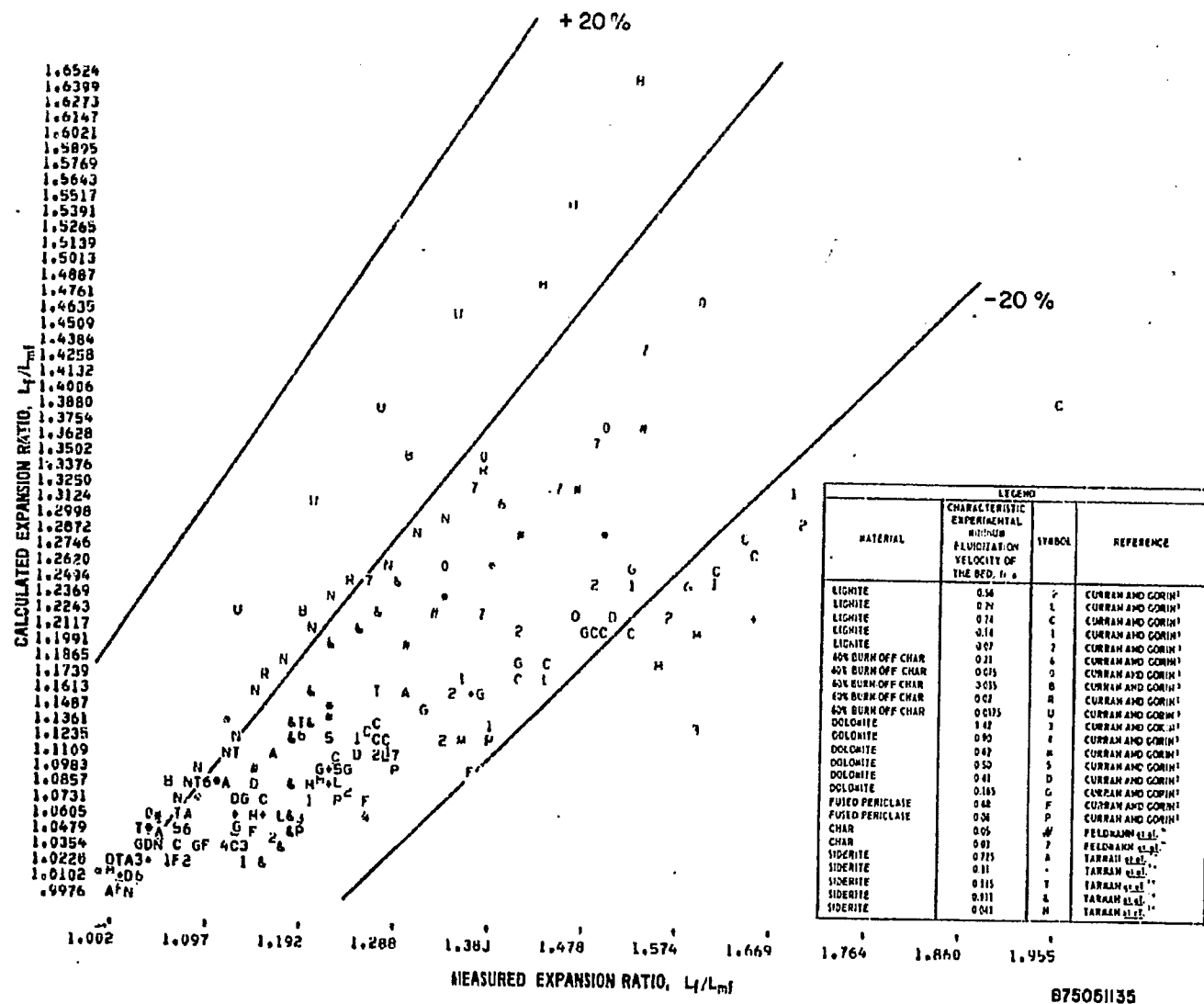


Figure 15. COMPARISON OF THE LEVA et al, CORRELATION WITH MEASURED BED EXPANSION DATA



4/75

ERDA	
PAGE	
REVISION No.	
DATE	

8964

$m$  = constant

$Re_{mf}$  = particle Reynold's number =  $(D_p \cdot U_{mf} \cdot \rho_g / \mu)$

$U_{mf}$  = minimum fluidization velocity, ft/s

$V$  = superficial velocity, ft/s

$X$  = weight fraction of sieved particles

$\delta$  = fractional volume occupied by bubbles and voids in a fluidized bed

$\epsilon_{mf}$  = voidage of minimum fluidized bed

$\phi$  = shape factor

$\rho_g$  = density of fluidizing gas, lb/CF

$\rho_s$  = particle density of fluidizing solids, lb/cu ft

$\mu$  = viscosity of fluidizing gas, lb/ft-s

#### 4. References Cited

1. Agarwal, O. P. and Storrow, J. A., "Pressure Drop in Fluidized Beds - Part I," Chem. Ind. (London), 278-86 (1951) April 14.
2. Broadhurst, T. E. and Becker, H. A., "Onset of Fluidization and Slugging in Beds of Uniform Particles." A.I.Ch.E. J. 21, No. 2, 238 (1975).
3. Curran, G. P. and Gorin, E., "Studies on Mechanics of Fluo-Solids Systems," prepared for Office of Coal Research, Contract No. 14-01-0001-415, Interim Report No. 8, Book 1. Washington, D. C., 1970.
4. Feldmann, H. F., Kiang, K. and Yavorsky, P., "Fluidization Properties of Coal Char," Symposium on Gasification of Coal, 162nd National Meeting, ACS Division of Fuel Chemistry Preprints 15, 62-76 (1971) September.
5. Frantz, J. F., "Design for Fluidization," Chem. Eng. 69, 161-178 (1962) September 17.
6. Institute of Gas Technology, "Preparation of a Coal Conversion Systems Technical Data Book," ERDA Contract No. 14-32-0001-1730, Rep. No. 4. Chicago, February 1975.
7. Knowlton, T. M., "High-Pressure Fluidization Characteristics of Several Particulate Solids: Primarily Coal and Coal-Derived Materials." Paper No. 9b, presented at the 6th Annual Meeting of the A. I. Ch. E., Washington D. C., December 1-5, 1974.
8. Kunii, D. and Levenspiel, O., Fluidization Engineering, New York: John Wiley, 1969.

9. Leva, M., "Flow Through Packings and Beds - Correlations in Fluidized Systems," Chem. Eng. 64, 266-70 (1957) November.
10. Leva, M., Fluidization. New York: McGraw-Hill, 1959.
11. Leva, M., Weintraum, M., Grummer, M., Pollchik, M. and Storch, H. H., "Fluid Flow Through Packed and Fluidized Systems," U.S. Bur. Mines Bull. 504. Pittsburgh, 1951.
12. Lewis, W.K., Gilliland, E. R. and Bauer, W. C., "Characteristics of Fluidized Particles." Ind. Eng. Chem., 41, 1104 (1949).
13. Shen, C. Y. and Johnstone, H. F., "Gas-Solid Contact in Fluidized Beds," A.I.Ch.E. J. 1, 349 (1955).
14. Tarman, P., Punwani, D., Bush, M. and Talwalkar, A., "Development of the Steam-Iron System for Production of Hydrogen for the HYGAS Process," prepared for Office of Coal Research, Contract No. 14-32-0001-1518, R&D Report No. 95, Interim Report No. 1. Washington, D.C., 1974.
15. van Heerden, C., Nobel, A. P. P. and van Krevelen, D. W., "Studies on Fluidization I - The Critical Mass Velocity," Chem. Eng. Sci. 1, No. 1, 37-49 (1951).
16. Zenz, F. A., Private Communication, April 1975.
17. Zenz, F. A., "Calculate Fluidization Rates," Pet. Refiner 36, No. 8, 147-55 (1957).

##### 5. Errata

In the Project 8964 February 1975 Status Report, the following correction is to be noted. In Table 3 (page 36), the bed diameter for Feldmann et al.'s data is 2 and 3.69 inches instead of 3.69 inches.

In the Project 8964 March 1975 Status Report, the following corrections are to be noted.

In Table 3 (page 26), the bed diameter for Feldmann et al.'s data is 2 inches instead of 3.69 inches.

In Section 4, References Cited, Reference 14 of Leva et al. should be numbered as 13 and Reference 14 should be -

14. Lewis, W. K., Gilliland, E. R. and Bauer, W. C., "Characteristics of Fluidized Particles," Ind. Eng. Chem. 41, 1104 (1949).



#### D. COMBUSTION

##### Low-Temperature Combustion (Fluidized-Bed Combustion)

A major factor in the design of fluidized-bed combustors is the recovery of sulfur through reaction of  $\text{SO}_2$  with  $\text{CaO}$  according to the following reaction:



The source of  $\text{CaO}$  can be natural limestone or dolomite, or a regenerated  $\text{CaO}$  or  $\text{CaCO}_3$ .

As discussed by Archer *et al.*,<sup>1</sup> the results of the kinetics studies of the above reaction based on flue products or  $\text{SO}_2$ -air mixtures cannot be directly used in fluidized-bed coal combustion systems. An obvious difference is in the temperature effect. In several studies of the combustion of a wide range of coal in the presence of a wide range of additives, a maximum rate of sulfur recovery was observed between 1500° and 1600° F. There is no counterpart of this phenomenon in the  $\text{SO}_2$ - $\text{CaO}$  kinetics. It also may be peculiar to low-pressure operation<sup>3</sup> because it was not observed in a system operating at 8 atm. Until the detailed structure of the fluidized-bed combustion (FBC) process is known, we cannot apply the kinetics of other contacting systems. We presumably must derive them from FBC systems studies.

As must be expected in gas-solid reactions, the reaction rates depend strongly on the source of the  $\text{CaO}$ . To a lesser but still significant extent, the apparent rate depends on the coal characteristics.

To calculate the sulfur retention in a combustor, therefore, we need reactivity factors for the additive (the source of  $\text{CaO}$ ), and for the coal. To establish these factors from FBC data, we must assume a mixing model and a kinetic model and assign reference materials. In the present state-of-the-art, the gas phase can be considered completely mixed or in plug flow and the solid phase uniformly distributed. The kinetics with respect to  $\text{SO}_2$  and  $\text{CaO}$  also can be expected to be some simple, approximately first, order.

To describe the sulfur recovery system, we define the following symbols:

$S_{\text{feed}}$  = feed rate of coal sulfur (moles/time)

$F$  = product (flue) gas rate (moles/time)

$X_{\text{SO}_2}$  =  $\text{SO}_2$  mole fraction in product gas

$r$  = mole ratio of CaO or equivalent in additive feed to coal sulfur

$R_S$  = fraction of feed coal sulfur recovered as  $\text{CaSO}_4$

$W_{\text{bed}}$  = bed mass (mass)

$\text{Ca}_{\text{bed}}$  = calcium mass fraction in bed

$X_{\text{Ca}}$  = fraction of feed CaO or equivalent converted to  $\text{CaSO}_4$

Some relationships among these are—

$$X_{\text{SO}_2} = (1 - R_S) S_{\text{feed}} / F \quad (1)$$

$$X_{\text{Ca}} = R_S / r \quad (2)$$

If the elutriation is or assumed to be nonselective with respect to the different calcium compounds, the conversion,  $X_{\text{Ca}}$ , would apply to the fluidized bed. If the elutriation is nonselective with respect to the coal and additive residues, then we have the following relation:

$$\text{Ca}_{\text{bed}} = 1.25r / \left[ \left( \frac{\text{ash}}{S} \right)_{\text{coal}} + 2.5R_S + 1.25r \left( \frac{\text{ash}}{\text{Ca}} \right)_{\text{additive}} \right] \quad (3)$$

where the numerator is the amount of calcium in the bed and the terms in the denominator give the contributions to the bed weight by the residue from coal, retained  $\text{SO}_2$ , and the additive residue, respectively.

For a simple completely mixed reactor model, if we assume the bed weight is proportional to the bed volume, the rate of reaction should be calculated from

$$\text{rate (moles of S/time/mass of bed)} = R_S \cdot S_{\text{feed}} / W_{\text{bed}} \quad (4)$$

If we assume a rate law that is first order in the  $\text{SO}_2$  in the bed, and is some function of the unreacted CaO,

$$\text{rate} = k X_{\text{SO}_2} \quad (5)$$

where  $k$  is some function of temperature, pressure, and unreacted CaO. In this simple representation,  $k$  is, for now, determined from FBC data and therefore, as long as it works, is a means of summarizing or coordinating the data and is not implied to be a correct physical model.

Keppel in the ANL report of 1971<sup>2</sup> presented a model based on plug flow of the gas and different possible patterns of  $\text{SO}_2$  generation. The ability to describe the experimental results apparently was not sensitive to these patterns. If one were

to use the Koppel model with uniform generation of  $\text{SO}_2$ , then instead of Equation 5 one would need the implicit equation

$$\ln \left[ 1 - \frac{k X_{\text{SO}_2}}{(R_s \cdot S_{\text{feed}}/W_{\text{bed}})} \right] = - \frac{R_s}{1 - R_s} \left[ \frac{k X_{\text{SO}_2}}{(R_s \cdot S_{\text{feed}}/W_{\text{bed}})} \right] \quad (6)$$

For sulfur recoveries greater than 40%, Equation 6 can be replaced by the approximation -

$$\text{rate} = R_s \cdot S_{\text{feed}}/W_{\text{bed}} = \frac{k X_{\text{SO}_2}}{1 + 1.2 (1 - R_s)} \quad (7)$$

Because the models are different, the rate constants derived from the data will be different and they must be used only in their respective models.

Koppel also introduced a dependence on the  $\text{CaO}$  in the bed assuming first-order dependence on an effective fraction of the  $\text{CaO}$ . He concluded, for the materials and conditions of that study,<sup>2</sup> that the additive (a limestone) had only 50% effective  $\text{CaO}$ . This cannot be considered the general case and probably implies the need of at least two parameters to describe the reactivity of the additive.

For choice of reference materials, the work of Argonne National Laboratories<sup>3</sup> using Tymochtee Dolomite as an additive and a highly volatile bituminous Pittsburgh seam coal from the Consolidation Coal Company Arkwright Mine is one of the more extensive studies and permits examination of the effects of some major variables. The variables considered are velocity, temperature, and  $\text{CaO}$ -to-sulfur ratio. The data are constrained to relatively constant air-fuel ratio, feed particle size, bed weight, and system pressure. The air-fuel ratio must be expected to be a significant factor, but in practice, may not have a wide range. The effect of bed volume or weight can be anticipated from simple kinetics considerations. Feed particle size, if necessary, will show up in the proposed simple formulation, in the reactivity factors. The pressure effects are apparently very temperature sensitive and must ultimately appear in the chemical kinetic expression. However, here too, probable practice may limit the pressures of interest to a few distinct ranges. This study<sup>3</sup> also reports the bed compositions and conversions, thereby avoiding the dependence on Equations 2 and 3 and their unproved assumptions.

In Table 2, the characteristics of the coal and additive are shown. In Table 3, the operating conditions are summarized.

Table 2. CHARACTERISTICS OF REFERENCE MATERIALS<sup>3</sup>

Analysis, wt %	Arkwright Coal	Tymochtee Dolomite
Moisture	2.89	Ca 20.0
Ash	7.68	CO <sub>2</sub> 38.5
Sulfur	2.32	Ash 59.7
Carbon	74.91	
Hydrogen	5.08	
Oxygen	4.83	
Sieve Range, U.S. sieve No.	-14+170	-14+170
Mean Particle size, $\mu\text{m}$	323	750

Table 3. OPERATING RANGES OF REFERENCE SYSTEM<sup>3</sup>

Temperature	1445° - 1665° F
Pressure	8 atm
Dry Flue Gas/Coal	153 SCF/lb
Bed Diameter	0.5 ft
Bed Weight	22-36 lb
Ca/S Mole Ratio	1.0-3.3
Ca Conversion	0.32-0.83
Ca Bed Wt Fraction	0.17-0.24
Sulfur Recovery Fraction	0.62-0.95

The validity of Equations 2 and 3 for bed compositions was examined. As an estimate of the calcium weight fraction, Equation 3 gives values, on the average, 0.01 less than the measured value with a standard deviation of about 0.01. This accuracy, if generally true, makes Equation 3 a useful equation. Equation 2 for the conversion,  $X_{Ca}$ , gives values that are 20% low with a standard error of 12%. At higher conversions, the calculated value of  $(1 - X_{Ca})$  which appears in the rate expression, could have a high uncertainty, and prevent reasonable interpretation of data. However, if generally true, the use of the factor of 1.2 to correct the calculated conversion would serve adequately for the range of probable operation in which conversions of less than 0.5 will be necessary to maintain low  $SO_2$  levels.

In the following calculations, the reported rather than calculated values are used.

Following Koppel's line, we assume that the rate constant  $k$  is proportional to the effective  $CaO$ , that is -

$$k = k_o (X_{Ca,m} - X_{Ca}) Ca_{bed} \quad (8)$$

where  $X_{Ca,m}$  is the maximum possible conversion. The ANL data were used to calculate the values of  $k$  based on the completely mixed reactor model (Equations 4 and 5), and they were plotted to test Equation 8 in Figure 16. The completely mixed model and the plug flow (uniform generation) model seem to reasonably represent the data of this system with the assumption that maximum possible conversion is complete conversion. Also (again, for this system) there is no major temperature effect. (Since mole fraction of  $SO_2$  rather than concentration was used, one may assume the rate is proportional to the absolute temperature, but such a low dependence is lost in the random deviations.) The line drawn in Figure 16 is based on the completely mixed model and is such that  $k_o = 0.61$  lb-moles of sulfur/lb of calcium/minute. We have no rationalization of the point with apparently unusually high rate of reaction.

With the system discussed above for reference, other sets of data on the performance of FBC systems are being evaluated.



ERDA	_____
PAGE	_____
REVISION No.	_____
DATE	_____

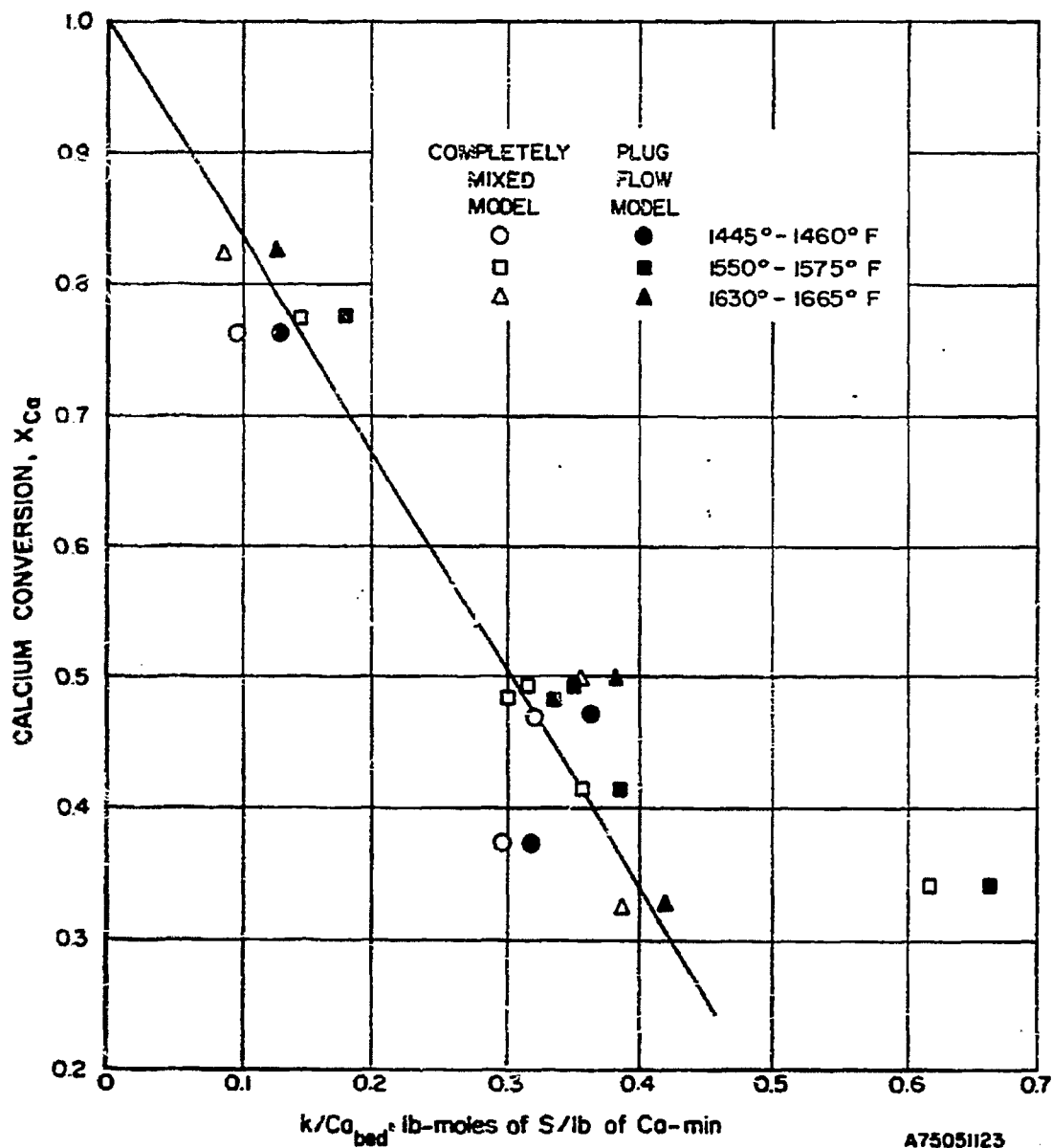


Figure 16. DEPENDENCE OF FBC SULFUR RECOVERY RATE CONSTANT ON CONVERSION [ANL Data<sup>3</sup> for Arkwright Mine Coal with Tymochtee Dolomite at 8 atm. ]

## 2. High-Temperature Combustion (MHD)

A meeting was held with Mr. Daryl Bomkamp of Argonne National Laboratory to determine the type of data being collected by ANL on MHD and the best means of coordinating ANL's work on MHD data collection with the Data Book project. He indicated that the data on electrical properties of the gases at high temperature will be available before the end of the year.

It was decided to prepare an outline of the MHD data section so that information can be collected in an orderly manner.

## 3. References Cited

1. Archer, D. H. et al., Evaluation of the Fluidized-Bed Combustion Process Vol. II, 16. Springfield, Va.: National Technical Information Service, 1970 (PB 212960).
2. Jonke, A. A. et al., Reduction of Atmospheric Pollution by the Application of Fluidized-Bed Combustion, Annual Report July 1970-June 1971, ANL ES-CEN-1004. Argonne National Laboratory, U. S. Environmental Protection Agency.
3. Vogel, G. J. et al., Reduction of Atmospheric Pollution by the Application of Fluidized-Bed Combustion, Annual Report, July 1973-June 1974. Argonne National Laboratory.

## E. COAL, CHAR, AND OIL SHALE PROPERTIES

### 1. Coal Data Compilation

The Bureau of Mines has recently published a compilation of coal reserve data for underground mining in states east of the Mississippi River,<sup>18</sup> and another for strippable coal in the whole of the United States.<sup>17</sup> With data from these and other publications we have prepared a table with region-by-seam entries of deposits seemingly large enough to support coal conversion plants (Table 4). The purpose of the table is to provide a basis for choosing the coal samples that will be included in our final compilation of data.

Terms used in the estimation of the amount of coal in the deposits are defined in the cited publications as follows:<sup>17, 18</sup>

"Coal resource and coal reserve classification is presently based upon three criteria - (1) thickness of the coalbed, (2) depth of the coalbed, and (3) the reliability of the data upon which the estimate was based. The criteria for each category are described in the following paragraphs.

"Identified Resources - Include beds of bituminous coal and anthracite 14 inches or more thick and beds of subbituminous coal and lignite 30 inches or more thick that occur at depths to 3,000 feet, the existence and quantity of which have been delineated within specified degrees of geologic assurance as measured, indicated, or inferred. Include also thinner and/or deeper beds that presently are being mined or for which there is evidence that they could be mined commercially.

"Undiscovered Resources - Include beds of bituminous coal and anthracite 14 inches or more thick and beds of subbituminous coal and lignite 30 inches or more thick that are presumed to occur in unmapped and unexplored areas reasonably near the surface (to depths of 3,000 feet) or in deeper structural basins of depths between 3,000 feet and 6,000 feet. All undiscovered coal resources in the United States are considered to be in the hypothetical category.

"Total Resources - Include in this category the sum of the identified and undiscovered resources.

"Reserve Base - Include in-place beds of bituminous coal and anthracite 28 inches or more thick and beds of subbituminous coal 60 inches or more thick that occur at depths to 1,000 feet. Include also thinner and/or deeper beds that presently are being mined or for which there is evidence that they could be mined commercially at this time. Include beds of lignite 60 inches or more thick that can be surface mined - generally those that occur at depths no greater than 120 feet. Also, it includes only coal from measured and indicated categories of reliability.

"Reserve or Recoverable Reserve - Include that portion of the reserve base that can be mined legally and economically at the time of classification.

"Subeconomic Resources - Include all identified resources that do not fall into the reserve category. Include in this category beds of bituminous coal and anthracite 14 inches to 28 inches thick and beds of subbituminous coal 30 inches to 60 inches thick that occur at depths to 1,000 feet. Include also beds of bituminous coal and anthracite 14 inches or more thick and beds of subbituminous coal 30 inches or more thick that occur at depths between 1,000 and 3,000 feet. Include lignite beds 30 inches or more thick that cannot be surface mined, generally those that occur at depths greater than 120 feet, and lignite beds 30 inches to 60 inches thick that can be surface mined. Include the nonrecoverable portion of the reserve base.

"The following criteria for measured, indicated, and inferred are applicable to both the reserve and subeconomic resource components:

"Measured - Tonnage is computed from dimensions revealed in outcrops, trenches, mine workings, and drill holes. The points of observation and measurement are so closely spaced and the thickness and extent of coals are so well defined that the tonnage is judged to be accurate within 20 percent of true tonnage. Although the spacing of the points of observation necessary



to demonstrate continuity of the coal differs from region to region according to the character of the coalbeds, the points of observation are, in general, no greater than one-half mile apart. Generally, measured reserves are synonymous with proved reserves of other reports.

"Indicated - Tonnage is computed partly from specified measurements and partly from projections of visible data for a reasonable distance on the basis of geologic evidence. In general, the points of observation are about 1 mile apart, but they may be as much as 1-1/2 miles apart for beds of known continuity. Generally, indicated reserves are equivalent to probable reserves of other reports.

"Inferred - Quantitative estimates are based largely on broad knowledge of the geological character of the bed or region, and few measurements of bed thickness are available. The estimates are based primarily on an assumed continuation for which there is geologic evidence. In general, inferred coal lies more than 1-1/2 miles from the outcrop or from points for which mining or drilling information is available, but usually does not exceed 4 miles, modified in practice by geological considerations.

"Demonstrated Reserves - Include in this category the sum of the measured and indicated reserves."

Terms applicable to strip mining are -

"Recoverable strippable resource - The remaining strippable resource multiplied by a mining recovery factor.

"Recovery factor - The proportion of the resource that is technically capable of being produced, usually expressed as a percent.

"Reserves - The measured portion of the resource that is recoverable (minable coal) with the technology and equipment presently available or that may be made available in the foreseeable future.

"Remaining strippable resource - The total original coal resource under a specified maximum depth of overburden and reduced by depletion computed from past strip and auger mining production.

"Resource - The estimated total quantity of all coal in place, having a specified minimum coalbed thickness and under a specified maximum depth of overburden.

"Strippable reserves - The recoverable strippable resource adjusted to conform to the stripping ratio, which varies by area. Coal that cannot be mined because of the proximity of natural or manmade features is also excluded. These reserves are the actual raw tons of coal that can be removed from the ground. They are also assumed to be all 'available' tonnages and are not divided into 'measured', indicated', and 'inferred' reserves."

For underground mining, the reserve base, including measured and indicated deposits, is reported in the cited publications by county and seam.

In the Eastern United States, counties rarely extend more than about 30 miles. A reserve base of 300 million tons of coal in a county, from which 150 million tons is usually estimated to be producible, was taken as sufficient to support a conversion plant for 20 years. This criterion was applied for the inclusion of a county in our list. Seams contributing 10% or more to the county total were then listed under each county. Run-of-mine samples may occasionally consist of coal from more than one seam being simultaneously mined, but channel samples are always taken from a single seam. This necessitates the listing of seams in our table.

In the Western States, counties often extend 60 miles or more, and we consider listing by deposit or field to be necessary.

In the Bureau of Mines publication on coal resources for strip-mining,<sup>17</sup> amounts of measured and indicated strippable reserve (estimated producible amounts) are given for counties and for seams, but usually not by seam in each county or field. Breakdown of each county or field by seams (when available) was obtained from state geological survey publications; these amounts may include inferred deposits, as indicated in the table. A criterion of 150 million tons of strippable reserve (SR) for counties in Eastern States and counties or fields (where applicable) in Western States was adopted for the table. When data were available (Illinois and Montana), inferred deposits were included for application of the criterion. In other states, the criterion was applied to the strippable reserve values of the Bureau of Mines publication.<sup>17</sup>

No Bureau of Mines or similar publication is available for underground mining in the Western States. However, such a compilation is not needed at present because additional mining for lignite and subbituminous coal in the west is likely to be limited to stripping. However, underground mining may have to be considered for liquefaction, for which bituminous coal is preferable.

## 2. Penn State Data

We have received analytical and other data on 50 coal deposits from Penn State. The data are being tabulated in a suitable form for presentation in the Data Book. We will check the deposits analyzed by Penn State against the list of deposits presented in Table 4. The coal properties data will be presented in next month's report.

Table 4. Part 1. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
ARIZONA				
Navajo County <sup>b</sup>	SR	MI	387	17
Black Mesa Field	RSR	MI	400	17
Wepo Group (8 Seams)	SR	MI	387	17
COLORADO				
Routt County	SR	MI	330	17
Yampa Field, 20-mile deposit	RSR	MI	330	17
E				2
D				2
C, Webber, Butcher Knife, Rice Mine				2
No. 3, B, Bear River, Sun Mine				2
No. 2, A, Pinnacle				2
No. 1, Brooks, Curtis				2
ILLINOIS				
Adams County	SR	MII	619.275	10
	SR	MI	54.5	17
Colchester (No. 2)	SR	MII	619.275	10

Note: Bases of the amounts of coal reported in the table are indicated by the following symbols:

URB - underground reserve base

SR - strippable reserve

RSR - recoverable strippable resource

MI - value includes coal of measured and indicated reliability of estimate

MII - value includes coal of measured, indicated, and inferred reliability of estimate.

<sup>a</sup> All undesignated coal is bituminous.

<sup>b</sup> Subbituminous.

A75051187a

Table 4, Part 2. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Bond County	URB	MI	1831.5	18
Herrin (No. 5)	URB	MI	1752.1	18
Brown County	SR	MII	386.496	10
	SR	MI	37.1	17
Colchester (No. 2)	SR	MII	386.496	10
Bureau County	URB	MI	1029.44	18
	SR	MI	73.90	17
	SR	MII	452.4	16
Danville (No. 7)	URB	MI	186.30	18
	SR	MII	183.223	16
Herrin (No. 6)	URB	MI	250.18	18
	SR	MII	262.115	16
Colchester (No. 2)	URB	MI	592.96	18
Christian County	URB	MI	3347.44	18
Herrin (No. 6)	URB	MI	2651.30	18
Harrisburg-Springfield (No. 5)	URB	MI	617.21	18
Clinton County	URB	MI	1322.46	18
Herrin (No. 6)	URB	MI	1320.34	18
Crawford County	URB	MI	442.62	18
Danville (No. 7)	URB	MI	70.58	18
Harrisburg-Springfield (No. 5)	URB	MI	105.29	18
James Town	URB	MI	80.66	18
Seelyville	URB	MI	151.24	18
Douglas County	URB	MI	411.68	18
Herrin (No. 6)	URB	MI	390.61	18
Edgar County	URB	MI	1749.89	18
Danville (No. 7)	URB	MI	511.39	18
Herrin (No. 6)	URB	MI	333.50	18
Harrisburg-Springfield (No. 5)	URB	MI	332.01	18
Seelyville	URB	MI	572.99	18

<sup>a</sup> All undesignated coal is bituminous.

A7505 1187b

Table 4, Part 3. LARGE-SIZE U.S. STRIPPABLE AND EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Fayette County	URB	MI	1173.72	18
Danville (No. 7)	URB	MI	296.02	18
Herrin (No. 6)	URB	MI	877.70	18
Franklin County	URB	MI	3038.43	18
Herrin (No. 6)	URB	MI	1875.68	16
Harrisburg-Springfield (No. 5)	URB	MI	831.79	18
Fulton County	SR	MII	2120.797	16
Herrin (No. 6)	SR	MI	330.2	17
Harrisburg-Springfield (No. 5)	SR	MII	249.286	17
Colchester (No. 2)	SR	MII	702.386	17
			1104.785	17
Gallatin County	URB	MI	1761.08	18
	SR	MI	48.300	17
	SR	MII	237.754	12
Herrin (No. 6)	URB	MI	557.13	18
	SR	MII	121.905	12
Harrisburg-Springfield (No. 5)	URB	MI	582.38	18
	SR	MII	115.849	12
DeKoven	URB	MI	266.05	18
Davis	URB	MI	348.63	18
Greene County	SR	MII	597.922	14
	SR	MI	74.1	17
Herrin (No. 6)	SR	MII	97.274	14
Colchester (No. 2)	SR	MII	500.648	14
Grundy County	SR	MII	356.077	15
	SR	MI	46.3	17
Sumnum (No. 4)	SR	MII	43.558	15
Colchester (No. 2)	SR	MII	312.519	15
Hamilton County	URB	MI	2440.16	18
Herrin (No. 6)	URB	MI	1489.80	18
Harrisburg-Springfield (No. 5)	URB	MI	950.36	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187c

Table 4, Part 4. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Henry County	SR	MII	577.265	16
	SR	MI	112.1	17
Danville (No. 7)	SR	MII	58.878	16
Herrin (No. 6)	SR	MII	255.435	16
Colchester (No. 2)	SR	MII	242.952	16
Jackson County	SR	MII	391.321	13
	SR	MI	96.400	17
Herrin (No. 6)	SR	MII	149.318	13
Harrisburg-Springfield (No. 5)	SR	MII	99.843	13
Murphysboro	SR	MII	130.278	13
Jefferson County	URB	MI	1800.56	18
Herrin (No. 6)	URB	MI	1305.60	18
Harrisburg-Springfield (No. 5)	URB	MI	494.96	18
Jersey County	SR	MII	220.461	14
	SR	MI	28.10	17
Herrin (No. 6)	SR	MII	57.336	14
Colchester (No. 2)	SR	MII	163.125	14
Knox County	SR	MII	1583.379	16
	SR	MI	188.4	17
Herrin (No. 6)	SR	MII	257.066	16
Harrisburg-Springfield (No. 5)	SR	MII	626.509	16
Colchester (No. 2)	SR	MII	697.281	16
LaSalle County	URB	MI	1082.96	18
	SR	MI	39.300	17
	SR	MII	280.420	15
Danville (No. 7)	URB	MI	370.77	18
Herrin (No. 6)	SR	MII	70.204	15
Colchester (No. 2)	URB	MI	620.16	18
	SR	MII	209.712	15
Lawrence County	URB	MI	893.64	18
Danville (No. 7)	URB	MI	143.44	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187d

Table 4, Part 5. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Harrisburg-Springfield (No. 5)	URB	MI	272.52	18
James Town	URB	MI	152.85	18
Livingston County	URB	MI	586.49	18
Danville (No. 7)	URB	MI	272.05	18
Colchester (No. 2)	URB	MI	265.50	18
Logan County	URB	MI	813.68	18
Harrisburg-Springfield (No. 5)	URB	MI	813.68	18
McLean County	URB	MI	420.95	18
Danville (No. 7)	URB	MI	231.68	18
Harrisburg-Springfield (No. 5)	URB	MI	107.12	18
Colchester (No. 2)	URB	MI	82.15	18
Macon County	URB	MI	439.31	18
Harrisburg-Springfield (No. 5)	URB	MI	420.39	18
Macoupin County	URB	MI	3421.12	18
	SR	MI	46.10	17
	SR	MII	275.605	14
Herrin (No. 6)	URB	MI	3006.52	18
	SR	MII	250.810	14
Colchester (No. 2)	URB	MI	259.26	18
	SR	MII	24.795	14
Madison County	SR	MI	134	17
	SR	MII	615.35	14
Herrin (No. 6)	SR	MII	449.283	14
Colchester (No. 2)	SR	MII	166.067	14
Marion County	URB	MI	421	18
Herrin (No. 6)	URB	MI	319.35	18
Harrisburg-Springfield (No. 5)	URB	MI	101.65	18
McDonough County	SR	MI	58.400	18
	SR	MII	584.320	10
Colchester (No. 2)	SR	MII	584.320	10

<sup>a</sup> All undesignated coal is bituminous.

A75051187e

Table 4, Part 6. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal. 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Marshall County	URB	MI	357.98	18
Danville (No. 7)	URB	MI	77.62	18
Colchester (No. 2)	URB	MI	270.61	18
Montgomery County	URB	MI	3966.5	18
Herrin (No. 6)	URB	MI	3272.28	18
Rock Island (No. 1)	URB	MI	208.20	18
Menard County	URB	MI	1460.0	18
Harrisburg-Springfield (No. 5)	URB	MI	1460.0	18
Morgan County	SR	MI	111	17
	SR	MII	827.615	14
Herrin (No. 6)	SR	MII	485.880	14
Colchester (No. 2)	SR	MII	341.735	14
Peoria County	SR	MI	355.1	17
	SR	MII	2174.236	16
Danville (No. 7)	SR	MII	282.537	16
Herrin (No. 6)	SR	MII	1058.371	16
Harrisburg-Springfield (No. 5)	SR	MII	725.549	16
Colchester (No. 2)	SR	MII	107.779	16
Perry County	URB	MI	1201.02	18
	SR	MI	291.7	17
	SR	MII	1106.041	13
Herrin (No. 6)	URB	MI	1025.37	18
	SR	MII	896.767	13
Harrisburg-Springfield (No. 5)	URB	MI	175.65	18
Harrisburg-Springfield (No. 5)	SR	MII	209.274	13
Putnam County	URB	MI	588.89	18
Danville (No. 7)	URB	MI	181.01	18
Herrin (No. 6)	URB	MI	78.88	18
Colchester (No. 2)	URB	MI	329.0	18
St. Clair County	URB	MI	951.35	18
	SR	MI	395	17

<sup>a</sup> All undesignated coal is bituminous.

A75051187f



Table 4, Part 7. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Herrin (No. 6)	SR	MII	1249.123	13
	URB	MI	932.07	18
	SR	MII	1249.123	13
Randolph County	SR	MI	108.50	17
Herrin (No. 6) Harrisburg-Springfield (No. 5)	SR	MII	455.029	13
	SR	MII	279.139	13
	SR	MI	175.890	13
Saline County	URB	MI	2553.37	18
	SR	MI	78	17
	SR	MII	545.410	12
Herrin (No. 6)	URB	MI	1076.77	18
Herrin (No. 5)	SR	MII	284.572	12
Harrisburg-Springfield (No. 5)	URB	MI	814.92	18
	SR	MII	93.442	12
	URB	MI	215.82	18
DeKoven	URB	MI	428.02	18
Davis	URB	MI	428.02	18
Cutler	SR	MII	78.44	12
Sangamon County	URB	MI	3540.03	18
Herrin (No. 6)	URB	MI	1559.11	18
Harrisburg-Springfield (No. 5)	URB	MI	1955.33	18
Schuyler County	SR	MI	91.6	17
	SR	MII	719.544	10
Harrisburg-Springfield (No. 5)	SR	MII	113.394	10
Colchester (No. 2)	SR	MII	606.150	10
Shelby County	URB	MI	712.47	18
Danville (No. 7)	URB	MI	125.27	18
Herrin (No. 6)	URB	MI	534.09	18
Stark County	SR	MI	94.0	17
	SR	MII	525.951	16
	SR	MII	57.703	16
Danville (No. 7)	SR	MII	442.467	16
Herrin (No. 6)	SR	MII	442.467	16

<sup>a</sup> All undesignated coal is bituminous.

A75051187g

Table 4, Part 8. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Tazewell County	SR	MI	24.3	17
	SR	MII	150.005	16
Herrin (No. 6)	SR	MII	69.680	16
Harrisburg-Springfield (No. 5)	SR	MII	37.05	16
Colchester (No. 2)	SR	MII	39.092	16
Vermilion County	URB	MI	1544.28	18
Danville (No. 7)	URB	MI	963.12	18
Herrin (No. 6)	URB	MI	536.64	18
Warren County	SR	MI	39.30	17
	SR	MII	159.758	16
Colchester (No. 2)	SR	MII	158.951	16
Washington County	URB	MI	1555.21	18
Herrin (No. 6)	URB	MI	1543.1	18
White County	URB	MI	992.47	18
Herrin (No. 6)	URB	MI	360.64	18
Harrisburg-Springfield (No. 5)	URB	MI	626	18
Williamson County	URB	MI	1573.10	18
	SR	MI	161.1	17
	SR	MII	651.820	12
Herrin (No. 6)	URB	MI	398.30	18
Herrin (No. 6)	SR	MII	290.718	12
Harrisburg-Springfield (No. 5)	URB	MI	690.5	18
Harrisburg-Springfield (No. 5)	SR	MII	200.268	12
DeKoven	URB	MI	316.71	18
Davis	URB	MI	109.37	18
INDIANA				
Gibson County	URB	MI	1301.54	18
Danville (VII)	URB	MI	165.47	18
Hymers (VI)	URB	MI	252.68	18
Springfield (V)	URB	MI	883.39	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187h

Table 4, Part 9. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Knox County	URB	MI	1453.48	18
Danville (VII)	URB	MI	145.55	18
Hymera (VI)	URB	MI	473.80	18
Springfield (V)	URB	MI	652.49	18
Survant (IV)	URB	MI	156.60	18
Posey County	URB	MI	720.90	18
Danville (VII)	URB	MI	95.89	18
Hymera (VI)	URB	MI	213.50	18
Springfield (V)	URB	MI	292.30	18
Seelyville (III)	URB	MI	119.21	18
Sullivan County	URB	MI	1922.31	18
	SR		154.622	17
Danville (VII)	URB	MI	259.36	17
Danville (VII)	SR			
Hymera (VI)	URB	MI	539.43	17
	SR			
Springfield (V)	URB	MI	532.58	17
	SR			
Survant (IV)	SR	MI	264.53	17
Seelyville (III)	SR	MI	326.41	17
Vanderburgh County	URB	MI	451.36	18
Springfield (V)	URB	MI	233.80	18
Seelyville (III)	URB	MI	202.51	18
Vermillion County	URB	MI	497.63	18
Springfield (V)	URB	MI	99.53	18
Survant (IV)	URB	MI	106.90	18
Seelyville (III)	URB	MI	269.35	18
Vigo County	URB	MI	1212.14	18
Danville (VII)	URB	MI	320.43	16
Springfield (V)	URB	MI	452.04	18
Survant (IV)	URB	MI	110.02	18
Seelyville (III)	URB	MI	269.02	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187i

Table 4, Part 10. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Warrick County	URB	MI	532.57	18
	SR	MI	152.554	17
Danville (VII)	URB	MI	90.49	18
Hymera (VI)	URB	MI	81.15	18
	SR			
Springfield (V)	URB	MI	332.97	18
	SR			
IOWA				
Unnamed County	SR	MI	180	17
Unnamed Seam	SR	MI	180	17
KENTUCKY (EAST)				
Floyd County	URB	MI	952.57	18
Upper Elkhorn (No. 3)	URB	MI	334.80	18
Upper Elkhorn (No. 2)	URB	MI	226.93	18
Upper Elkhorn (No. 1)	URB	MI	296.22	18
Harlan County	URB	MI	1408.51	18
Hazard (No. 5A)	URB	MI	154.05	18
Upper Elkhorn (No. 3)	URB	MI	206.77	18
Upper Elkhorn (No. 2)	URB	MI	239.13	18
Upper Elkhorn (No. 1)	URB	MI	362.74	18
Lower Elkhorn	URB	MI	132.73	18
Knott County	URB	MI	1248.37	18
Hazard (No. 7)	URB	MI	264.67	18
No. 7	URB	MI	258.94	18
Upper Elkhorn (No. 3)	URB	MI	424.58	18
Upper Elkhorn (No. 2)	URB	MI	88.49	18
Leslie County	URB	MI	619.50	18
Hazard (No. 5A)	URB	MI	187.82	18
Fire Clay	URB	MI	125.37	18
No. 7	URB	MI	197.92	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187j

Table 4, Part II. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Letcher County	URB	MI	730.36	18
No. 7	URB	MI	180.73	18
Mason (Mingo)	URB	MI	75.36	18
Upper Elkhorn (No. 3)	URB	MI	244.04	18
Lower Elkhorn	URB	MI	82.84	18
Perry County	URB	MI	560.22	18
Hazard (No. 7)	URB	MI	148.42	18
No. 7	URB	MI	263.01	18
Mason (Mingo)	URB	MI	62.35	18
Pike County	URB	MI	2170.01	18
Upper Elkhorn (No. 3)	URB	MI	194.01	18
Upper Elkhorn (No. 2)	URB	MI	438.59	18
Upper Elkhorn (No. 1)	URB	MI	194.94	18
Lower Elkhorn	URB	MI	668.00	18
KENTUCKY (WEST)				
Henderson County	URB	MI	1503.64	18
	SR	MI	165	17
No. 9	URB	MI	1411.14	18
Hopkins County	URB	MI	1805.67	18
	SR	MI	165	17
No. 14	SR			
No. 12	URB	MI	170.53	18
No. 12	SR			
No. 11	URB	MI	154.88	18
No. 11	SR			
No. 9	URB	MI	1145.34	18
No. 9	SR			
McLean County	URB	MI	723.65	18
No. 9	URB	MI	627.25	18
No. 6	URB	MI	84.34	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187k

Table 4, Part 12. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Muhlenberg County	URB	MI	898.37	18
	SR	MI	258	17
No. 12	URB	MI	158.24	18
No. 12	SR			
No. 11	URB	MI	176.08	18
No. 11	SR			
No. 9	URB	MI	535.81	17
Ohio County	SR	MI	161	17
No. 14	SR			
No. 11	SR			
Union County	URB	MI	1926.29	18
No. 11	URB	MI	338.74	18
No. 9	URB	MI	1286.43	18
No. 6	URB	MI	182.64	18
Webster County	URB	MI	1436.44	18
No. 9	URB	MI	1194.42	18
MARYLAND				
Allegany County	URB	MI	378.58	18
Freeport	URB	MI	135.41	18
Lower Bakers Town	URB	MI	82.27	18
Upper Freeport	URB	MI	102.63	18
Garrett County	URB	MI	523.33	18
Lower Bakerstown	URB	MI	132.79	18
Upper Freeport	URB	MI	312.99	18
Upper Kittanning	URB	MI	55.98	18
MONTANA				
Bighorn County <sup>b</sup>	SR	MI	1009	17
Deckerfield	RSR	MI	816	17
Dietz	SR	MI	540	17
Rolandfield	RSR	MI	251	17
Roland	SR	MI	126	17
Hangingwoman Creek				
Field	RSR	MI	265	17
Dietz 1	ST	MI	132	17

<sup>a</sup> All undesignated coal is bituminous.

<sup>b</sup> Subbituminous.

A75051187-1

Table 4, Part 13. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Sarpy Creek Field	RSR	MI	1500	5
Wolf Mountains (Indian Reservation)	RSR	MII	1922	5
Powder River County <sup>b</sup>	SR	MI	1405	17
Moorhead Field	RSR	MI	1200	17
Canyonbed	SR	MI	100	17
Dietz	SR	MI	100	17
Anderson	SR	MI	400	17
Otter Creek Field	RSR	MI	915	17
Knoblock	SR	MI	608	17
Ashland (Knoblock)	RSR	MI	2595	5
Powder River County <sup>c</sup>	SR	MI	1245	17
Broadus Field	RSR	MI	373	17
Broadus	SR	MI	240	17
Sonnette Field	RSR	MI	165	17
Pawnee	SR	MI	95	17
Pumpkin Creek Field	RSR	MI	1520	17
Sawyer	SR	MI	910	17
Rosebud County <sup>b</sup>	SR	MI	922	17
Birney Coal Field	RSR	MI	160	17
Brewster-Arnold	SR	MI	28	17
Poker Jim O'Dell Field	RSR	MI	200	17
Knoblock	SR	MI	100	17
Rosebud Creek Field <sup>c</sup>	RSR	MI	168	17
Terret	SR	MI	80	17
Colstrip Field <sup>b</sup>	RSR	MI	1057	17
Rosebud	SR	MI	718	17
McCone County <sup>c</sup>	SR	MI	410	17
Weldon-Timber Creek	RSR	MI	579	17
S-Bed	SR	MI	290	17
Redwater Field	RSR	MI	240	17
S-Bed	SR	MI	120	17
Powder River County <sup>b</sup>				
Foster Creek Field	RSR	MI	472	17
Knoblock	SR	MI	224	17

<sup>a</sup> All undesignated coal is bituminous.<sup>b</sup> Subbituminous.<sup>c</sup> Lignite.

A75051187m

Table 4, Part 14. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Dawson County <sup>c</sup>	SR	MI	180	17
Thirteen Mile Creek				
Field	RSR	MI	180	17
Pust	SR	MI	180	17
Richland County <sup>c</sup>	SR	MI	109	17
Breezy Flat Field	RSR	MI	160	17
Pust	SR	MI	80	17
O'Brian-Alkalie Creek	RSR	MII	150	5
Fox Lake Field	RSR	MI	46	5
Pust	SR	MI	29	5
Roosevelt County <sup>c</sup>	SR	MI	204	17
Fort Kipp Field	RSR	MI	265	17
Fort Peck	SR	MI	73	17
Fort Kipp	SR	MI	131	17
Sheridan County <sup>c</sup>	SR	MI	460	17
Reserve Field	RSR	MI	197	17
Reserve	SR	MI	100	17
Coalridge Field	RSR	MI	480	17
Coalridge	SR	MI	360	17
Wibaux County <sup>c</sup>	SR	MI	462	17
Wibaux Field	RSR	MI	603	17
C	SR	MI	426	17
Four Buttes Field	RSR	MI	730	17
C	SR	MI	636	17
NEW MEXICO				
San Juan County <sup>b</sup>	SR	MI	2370	17
Navajo Field	RSR	MI	2400	8
Fruitland Field	RSR	MI	158	8
Bisti and Star Lake Areas	RSR	MI	635	8

<sup>a</sup> All undesignated coal is bituminous.<sup>b</sup> Subbituminous.<sup>c</sup> Lignite.

A75051187n



Table 4, Part 15. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal. 10<sup>6</sup> tons</u>	<u>Reference No.</u>
NORTH DAKOTA				
Bowman County <sup>c</sup>	SR	MI	2130	17
Bowman Field	RSR	MI	182	17
Harmon	SR	MI	101	17
Gascogne Field	RSR	MI	218	17
Harmon	SR	MI	112	17
Golden Valley County <sup>c</sup>	SR	MI	224	17
Beach Field	RSR	MI	368	17
C	SR	MI	224	17
Mercer County <sup>c</sup>	SR	MI	312	17
Renner's Cove Deposit	RSR	MI	77.7	9
Zap	RSR	MI	77.7	9
Hazen Deposit (9)	RSR	MI		
Hazen	RSR	MI	71.1	9
Knife River Deposit	RSR	MI	624	17
Beulah-Zap	SR	MI	295	17
Slope County <sup>c</sup>	SR	MI	594	17
Harmon Deposit	RSR	MI	777	17
Harmon	SR	MI	263	17
Slope I Deposit	RSR	MI	136	17
Harmon	SR	MI	102	17
Slope II Deposit	RSR	MI	112	17
Harmon	SR	MI	56	17
Slope III Deposit	RSR	MI	120	17
T-Cross	SR	MI	40	17
Slope IV Deposit	RSR	MI	160	17
Hansen	SP	MI	133	17
Stark County <sup>c</sup>	SR	MI	286	17
Dickenson Deposit	RSR	MI	640	17
D	SR	MI	210	17
E	SR	MI	160	17

<sup>a</sup> All undesignated coal is bituminous.<sup>b</sup> Subbituminous.<sup>c</sup> Lignite.

A750511870

Table 4, Part 16. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
OHIO				
Athens County	URB	MI	1326.97	18
Pittsburgh (No. 8)	URB	MI	135.52	18
No. 7	URB	MI	216.00	18
Middle Kittanning (No. 6)	URB	MI	962.58	18
Belmont County	URB	MI	3927.08	18
No. 9	URB	MI	1081.96	18
Pittsburgh (No. 8)	URB	MI	2431.25	18
Carroll County	URB	MI	757.73	18
Middle Kittanning (No. 6)	URB	MI	353.14	18
Lower Kittanning (No. 5)	URB	MI	157.77	18
Columbiana County	URB	MI	747.93	18
No. 7	URB	MI	561.80	18
Lower Kittanning (No. 5)	URB	MI	115.72	18
Gallia County	URB	MI	339.63	18
Pittsburgh (No. 8)	URB	MI	122.88	18
No. 7	URB	MI	36.47	18
Middle Kittanning (No. 6)	URB	MI	87.37	18
Lower Kittanning (No. 5)	URB	MI	48.77	18
Guernsey County	URB	MI	1184.43	18
No. 7	URB	MI	597.40	18
Middle Kittanning (No. 6)	URB	MI	422.85	18
Harrison County	URB	MI	1523.27	18
Pittsburgh (No. 8)	URB	MI	258.90	18
No. 7	URB	MI	267.74	18
No. 6A	URB	MI	391.05	18
Middle Kittanning (No. 6)	URB	MI	507.92	18

<sup>a</sup> All undesignated coal is bituminous.

Table 4, Part 17. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Jefferson County	URB	MI	1356.24	18
Pittsburgh (No. 8)	URB	MI	327.72	18
No. 7	URB	MI	168.79	18
No. 6A	URB	MI	729.13	18
Lawrence County	URB	MI	477.03	18
No. 7	URB	M	99.41	18
Middle Kittanning (No. 6)	URB	M	166.95	18
Lower Kittanning (No. 5)	URB	MI	164.98	18
Mahoning County	URB	MI	308.15	18
Lower Kittanning (No. 6)	URB	MI	285.48	18
Meigs County	URB	MI	396.32	18
No. 8A	URB	MI	376.94	18
Monroe County	URB	MI	468.36	18
Pittsburgh (No. 8)	URB	MI	413.33	18
Morgan County	URB	MI	435.12	18
No. 9	URB	MI	173.50	18
Middle Kittanning (No. 6)	URB	MI	208.21	18
Muskingum County	URB	MI	720.78	18
No. 7	URB	MI	83.68	18
Middle Kittanning (No. 6)	URB	MI	536.99	18
Noble County	URB	MI	570.02	18
No. 9	URB	MI	387.22	18
No. 7	URB	MI	168.17	18
Perry County	URB	MI	644.97	18
Middle Kittanning (No. 6)	URB	MI	515.41	18
Lower Kittanning (No. 5)	URB	MI	101.26	18
Stark County	URB	MI	376.61	18
Middle Kittanning (No. 6)	URB	MI	162.15	18
Lower Kittanning (No. 5)	URB	MI	109.71	18
No. 4	URB	MI	99.27	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187q

Table 4, Part 18. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

Location and Seam	Basis	Estimate Class	Amount of Coal, 10 <sup>6</sup> tons	Reference No.
Tuscarawas County	URB	MI	841.20	18
No. 7	UR B	MI	101.89	18
Middle Kittanning (No. 6)	URB	MI	523.18	18
Lower Kittanning (No. 5)	URB	MI	187.85	18
Vinton County	URB	MI	301.20	18
Middle Kittanning (No. 6)	URB	MI	85.35	18
Lower Kittanning (No. 5)	URB	MI	55.06	18
No. 4A	URB	MI	107.80	18
PENNSYLVANIA				
Allegheny County	URB	MI	881.41	18
Upper Freeport (E)	URB	MI	356.61	18
Lower Freeport (D)	URB	MI	425.46	18
Armstrong County	URB	MI	1092.87	18
Upper Freeport (E)	URB	MI	359.10	18
Lower Freeport (D)	URB	MI	172.58	18
Lower Kittanning (B)	URB	MI	463.69	18
Beaver County	URB	MI	435.29	18
Upper Freeport (E)	URB	MI	255.62	18
Lower Kittanning (B)	URB	MI	76.09	18
Butler County	URB	MI	863.85	18
Upper Freeport (E)	URB	MI	292.86	18
Lower Freeport (D)	URB	MI	117.07	18
Middle Kittanning (C)	URB	MI	290.23	18
Clarion (A)	URB	MI	125.91	18
Cambria County	URB	MI	1454.17	18
Upper Freeport (E)	URB	MI	263.14	18
Lower Freeport (D)	URB	MI	426.43	18
Upper Kittanning (C)	URB	MI	359.01	18
Lower Kittanning (B)	URB	MI	352.04	18

<sup>a</sup> All undesignted coal is bituminous.

Table 4, Part 19. LARGE-SIZE U. S. STRIPPABLE AND EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Clarion County	URB	MI	640.12	18
Lower Kittanning (C)	URB	MI	209.73	18
Clarion (A)	URB	MI	336.34	18
Clearfield County	URB	MI	1102.48	18
Lower Freeport (D)	URB	MI	170.21	18
Upper Kittanning (C)	URB	MI	118.45	18
Lower Kittanning (B)	URB	MI	372.74	18
Clarion (A)	URB	MI	116.51	18
Brookville (A)	URB	MI	195.35	18
Fayette County	URB	MI	1023.70	18
Waynesburg	URB	MI	172.43	18
Pittsburgh	URB	MI	217.83	18
Upper Freeport (E)	URB	MI	229.12	18
Lower Freeport (D)	URB	MI	125.14	18
Lower Kittanning (B)	URB	MI	120.80	18
Greene County	URB	MI	6515.66	18
Waynesburg	URB	MI	1178.31	18
Sewickley	URB	MI	785.45	18
Pittsburgh	URB	MI	3540.07	18
Upper Freeport (E)	URB	MI	1011.83	18
Indiana County	URB	MI	1716.93	18
Upper Freeport (E)	URB	MI	568.30	18
Lower Freeport (D)	URB	MI	423.95	18
Lower Kittanning (B)	URB	MI	694.12	18
Jefferson County	URB	MI	407.37	18
Upper Freeport (E)	URB	MI	91.25	18
Lower Freeport (D)	URB	MI	67.29	18
Lower Kittanning (B)	URB	MI	149.39	18
Brookville (A)	URB	MI	72.33	18
Somerset County	URB	MI	1240.55	18
Upper Freeport (E)	URB	MI	209.34	18
Lower Freeport (D)	URB	MI	121.07	18
Upper Kittanning (C)	URB	MI	444.87	18
Lower Kittanning (B)	URB	MI	294.43	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187s

Table 4, Part 20. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Washington County	URB	MI	3604.21	18
Waynesburg	URB	MI	316.19	18
Pittsburgh	URB	MI	2995.61	18
Upper Freeport (E)	URB	MI	187.23	18
Westmoreland County	URB	MI	747.54	18
Pittsburgh	URB	MI	95.13	18
Upper Freeport (E)	URB	MI	528.58	18
SOUTH DAKOTA				
Unnamed County <sup>c</sup>	SR	MI	160	17
Unnamed Seam	SR	MI	160	17
TEXAS				
Milam County <sup>c</sup>	SR	MI	167	17
Wilcox Formation	RSR	MI	813	3
VIRGINIA				
Buchanan County	URB	MI	819.98	18
Hagy	URB	MI	109.40	18
Splashdam	URB	MI	250.54	18
Kennedy	URB	MI	197.01	18
No. 5	URB	MI	134.77	18
Dickenson County	URB	MI	515.54	18
Splashdam	URB	MI	50.25	18
Upper Banner	URB	MI	122.14	18
Kennedy	URB	MI	78.60	18
Jewell	URB	MI	92.14	18
No. 5	URB	MI	82.66	18
Russell County	URB	MI	403.02	18
Kennedy	URB	MI	85.54	18
No. 5	URB	MI	185.31	18
Tiller	URB	MI	84.66	18
Wise County	URB	MI	716.60	18
Norton (No. 2)	URB	MI	62.10	18
Upper Banner	URB	MI	57.11	18
No. 5	URB	MI	62.83	18

<sup>a</sup> All undesignated coal is bituminous.<sup>c</sup> Lignite.

A75051187t

Table 4, Part 21. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
WEST VIRGINIA				
Barbour County	URB	MI	948.76	18
Upper Freeport	URB	MI	104.64	18
Upper Kittanning	URB	MI	165.17	18
Upper Mercer	URB	MI	159.70	18
Bed No. 928	URB	MI	347.34	18
Boone County	URB	MI	1868.85	18
Winifrede	URB	MI	347.79	18
SR		MI		
Chilton	URB	MI	187.40	19
SR		MI		
Hernshaw	URB	MI	289.70	18
Cedar Grove	URB	MI	241.89	18
SR		MI		
Alma	URB	MI	317.181	18
SR		MI		
Campbell Creek	URB	MI	332.97	18
Braxton County	URB	MI	467.73	18
Lower Kittanning	URB	MI	203.68	18
Sockton	URB	MI	61.82	18
Clay County	URB	MI	695.02	18
Upper Kittanning	URB	MI	77.54	18
Middle Kittanning	URB	MI	73.72	18
Lower Kittanning	URB	MI	227.16	18
Sockton	URB	MI	101.75	18
Coal Burg	URB	MI	157.10	18
Fayette County	URB	MI	796.26	18
SR		MI	148.7	18
Campbell Creek	URB	MI	220.80	18
Eagle	URB	MI	94.92	18
Sewell	URB	MI	171.47	18
Grant County	URB	MI	313.23	18
Bakers Town	URB	MI	72.31	18
Upper Freeport	URB	MI	228.20	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187u

Table 4, Part 22. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Harrison County	URB	MI	380.89	18
Pittsburgh	URB	MI	335.06	18
Upper Kittanning	URB	MI	40.33	18
Kanawha County	URB	MI	1120.62	18
	SR	MI	284.1	17
Sockton	URB	MI	321.77	18
Campbell Creek	URB	MI	298.76	18
Bed Code 928	URB	MI	193.45	18
Lewis County	URB	MI	730.30	18
Redstone	URB	MI	221.55	18
Pittsburgh	URB	MI	254.05	18
Elklick	URB	MI	94.46	18
Lincoln County	URB	MI	360.43	18
Lower Kittanning	URB	MI	105.97	18
Sockton	URB	MI	129.03	18
Campbell Creek	URB	MI	113.44	18
Logan County	URB	MI	3076.26	18
	SR	MI	142.4	18
Cedar Grove	URB	MI	503.27	18
Alma	URB	MI	732.29	18
Campbell Creek	URB	MI	800.85	18
McDowell County	URB	MI	912.35	18
Beckley	URB	MI	123.72	18
Pocahontas No. 2	URB	MI	236.54	18
Pocahontas No. 3	URB	MI	241.10	18
Marion County	URB	MI	2599.46	18
Waynesburg	URB	MI	313.25	18
Swickley	URB	MI	989.71	18
Pittsburgh	URB	MI	1022.93	18
Marshall County	URB	MI	3043.77	18
Sewickley	URB	MI	916.06	18
Pittsburgh	URB	MI	1924.67	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187v



Table 4, Part 23. LARGE-SIZE U. S. STRIPPABLE AND  
EASTERN U. S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal. 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Mingo County	URB	MI	1887.45	18
	SR	MI	165.800	17
Coalburg	URB	MI	199.05	18
Cedar Grove	URB	MI	592.92	18
Alma	URB	MI	332.50	18
Monongalia County	URB	MI	3008.81	18
Waynesburgh	URB	MI	544.90	18
Sewickley	URB	MI	848.90	18
Pittsburgh	URB	MI	1342.14	18
Nicholas County	URB	MI	1433.69	18
Coalburg	URB	MI	155.95	18
Eagle	URB	MI	194.99	18
Sewell	URB	MI	236.86	18
Ohio County	URB	MI	379.05	18
Sewickley	URB	MI	54.27	18
Pittsburgh	URB	MI	273.29	18
Preston County	URB	MI	837.48	18
Upper Freeport	URB	MI	221.05	18
Upper Kittanning	URB	MI	141.79	18
Raleigh County	URB	MI	1656.34	18
Eagle	URB	MI	196.13	18
Beckley	URB	MI	334.13	18
Pocahontas No. 3	URB	MI	261.40	18
Randolph County	URB	MI	757.19	18
Sewell	URB	MI	308.12	18
Taylor County	URB	MI	388.24	18
Upper Kittanning	URB	MI	130.95	18
Lower Kittanning	URB	MI	201.10	18
Upshur County	URB	MI	876.87	18
Upper Kittanning	URB	MI	83.24	18
Upper Mercer	URB	MI	143.92	18
Bed Code 928	URB	MI	300.38	18

<sup>a</sup> All undesignated coal is bituminous.

A75051187w

Table 4, Part 24. LARGE-SIZE U.S. STRIPPABLE AND  
EASTERN U.S. UNDERGROUND COAL DEPOSITS<sup>a</sup>

<u>Location and Seam</u>	<u>Basis</u>	<u>Estimate Class</u>	<u>Amount of Coal, 10<sup>6</sup> tons</u>	<u>Reference No.</u>
Wayne County	URB	MI	403.55	18
Lower Kittanning	URB	MI	141.96	18
Campbell Creek	URB	MI	224.29	18
Webster County	URB	MI	1098.91	18
Eagle	URB	MI	160.78	18
Sewell	URB	MI	119.74	18
Pocahontas No. 13	URB	MI	130.18	18
Wetzel County	URB	MI	846.09	18
Sewickley	URB	MI	158.15	18
Pittsburgh	URB	MI	585.65	18
Wyoming County	URB	MI	1642.10	18
Beckley	URB	MI	168.03	18
Pocahontas No. 3	URB	MI	647.08	18
Pocahontas No. 2	URB	MI	150.30	18
WYOMING				
Campbell County	SR	MI	12160	17
Wyodak Deposit	RSR	MI	19000	11
Felix Deposit	RSR	MI	480	11
Smith Local Deposit	RSR	MI	236	11
Canyon Deposit <sup>d</sup>	RSR	MI	185	18
Converse County	SR	MI	253	17
Dry Cheyenne Deposit	RSR	MI	179	11
Johnson County	SR	MI	800	17
Healy Deposit	RSR	MI	1000	11
Lincoln County	SR	MI	140	17
Adaville Deposit	RSR		1000	11
Sweetwater County	SR	MI	403	17
Red Desert Deposit	RSR	MI	733	11
Jim Bridger Deposit	RSR	MI	200	11
Cherokee Deposit <sup>e</sup>	RSR	MI	200	11

<sup>a</sup> All undesignated coal is bituminous.<sup>d</sup> Partly in Sheridan County.<sup>e</sup> Partly in Carbon County.

A75051187x

### 3. Specific Heat of Coal, Char, and Ash

Work on the specific heat of coal, chars, and related materials was continued. The literature on the specific heat of clay (a major constituent of the mineral matter of most coals) was reviewed. Its specific heat ranges from about 0.4 to 0.5 cal/g-°C, or about twice that of typical ash from coal.<sup>6,7</sup> The difference is attributed to the presence of water of constitution in clay. Consideration of methods of correction is being deferred until recent Australian and Russian papers on the subject can be obtained.

Kirov's correlation<sup>4</sup> for the specific heat of coal, char, and coke was presented last month with data showing its good agreement with experimental data for temperatures up to 100°C. The literature has been searched for data published since Kirov's 1965 survey. It appears that measurements have been made, all told, on less than a dozen North American bituminous and lower rank coals, and on only about four of these have measurements been made at temperatures higher than 200°C. Work in this field is being pursued more actively in the Soviet Union and Japan.<sup>1,19</sup> Investigators in both countries use differential scanning calorimeters in which a sample is heated at a constant rate (2° to 10°C per minute) in a stream of inert gas. Results such as those shown in Figure 17 are obtained; an endothermic heat of reaction is found at temperatures from about 300° to 700°C, and

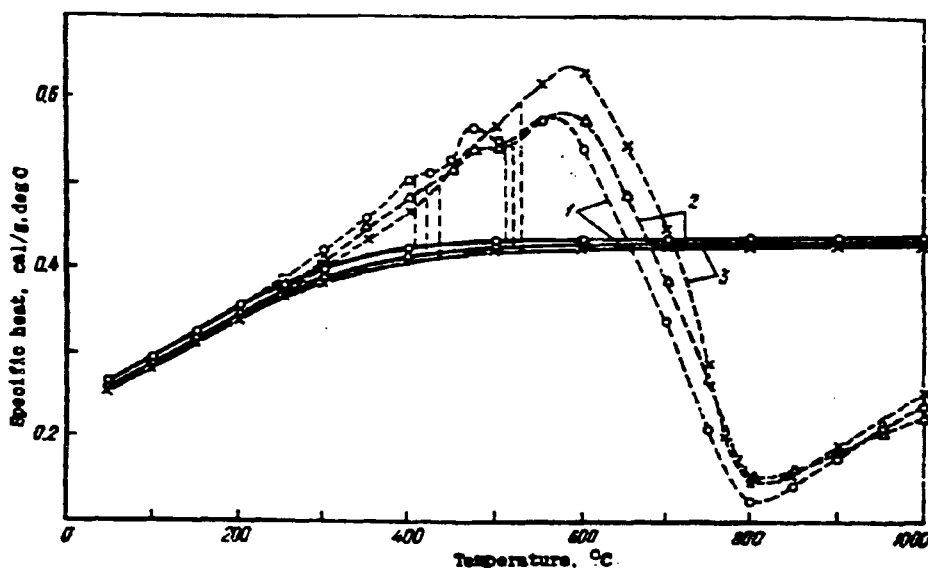


Figure 17. SPECIFIC HEAT OF COALS<sup>1</sup> (1) KZh14, (2) K13, AND (3) K<sub>2</sub> (Dashed Line Is the Apparent Value; Solid Line Is the True Value After Heat Soaking for 4 Hours)

an exothermic heat of reaction at higher temperatures. Measurements of this kind have begun at the Pennsylvania State University under a project funded by RANN.

For future work on this topic we plan to a) consult the principal investigator(s) at Penn State, b) obtain all the Japanese and Russian papers of interest and obtain translations as required, and c) test Kirov's correlation at elevated temperature by plotting calculated and observed specific heats against volatile matter, at selected constant temperatures.

#### 4. References Cited

1. Agroskin, A. A. et al., "Thermal Properties of Coals in the Plastic State," Coke Chem., 1972 (9), 1-4 (English translation).
2. Hornbaker, A. L. and Holt, R. D., 1972 Summary of Coal Resources in Colorado. Denver: Colorado Geological Survey, Department of Natural Resources, 1973.
3. Kaiser, W. R., "Texas Lignite: Near-Surface and Deep Basin Resources," Rep. Invest. No. 79. Austin, Tex.: Bureau of Economic Geology, The University of Texas, 1974.
4. Kirov, N. Y., "Specific Heats and Total Heat Contents of Coals and Related Materials at Elevated Temperatures," Br. Coal Util. Res. Assoc. Mon. Bull. 29, 33-57 (1965) February-March.
5. Lawson, D. C., "Directory of Mining Enterprises for 1972," Montana Bur. Mines Geol. Bull. No. 88. Butte, Mont., 1973.
6. MacGee, A. E., "The Heat Required to Fire Ceramic Bodies," J. Amer. Ceram. Soc. 9, 206-47 (1926).
7. Navias, L., "Measurement of the Heat Absorbed and Evolved by Clays During Firing and Cooling," J. Am. Ceram. Soc. 6, 1268-98 (1923).
8. Nielson, G. F., 1973 Keystone Coal Industry Manual. New York: McGraw-Hill, 1973.
9. Pollard, B. C. et al., "Strippable Lignite Reserves of North Dakota," U.S. Bur. Mines IC 8537. Denver, 1972.
10. Reinertsen, D. L., "Strippable Coal Reserves of Illinois, Part 4," Ill. State Geol. Surv. Circ. 374. Urbana, Ill., 1964.
11. Smith, J. B. et al., "Strippable Coal Reserves of Wyoming," U.S. Bur. Mines IC8538. Denver, 1972.

12. Smith, W. H., "Strippable Coal Reserves of Illinois, Part 1," Ill. State Geol. Surv. Circ. 228. Urbana, Ill., 1957.
13. Smith, W. H., "Strippable Coal Reserves of Illinois, Part 2," Ill. State Geol. Surv. Circ. 260. Urbana, Ill., 1958.
14. Smith, W. H., "Strippable Coal Reserves of Illinois, Part 3," Ill. State Geol. Surv. Circ. 311. Urbana, Ill., 1961.
15. Smith, W. H., "Strippable Coal Reserves of Illinois, Part 6," Ill. State Geol. Surv. Circ. 419. Urbana, Ill., 1968.
16. Smith, W. H. and Berggren, D. J., "Strippable Coal Reserves of Illinois, Part 5A," Ill. State Geol. Surv. Circ. 348. Urbana, Ill., 1963.
17. U.S. Bureau of Mines, "Strippable Reserves of Bituminous Coal and Lignite in the United States," IC8531. Washington, 1971.
18. U.S. Bureau of Mines, "The Reserve Base of Bituminous Coal and Anthracite for Underground Mining in the Eastern United States," IC8655. Pittsburgh, 1974.
19. Yamashita, Y. and Ouchi, K., "Specific Heat of Coal and Heat-Treated Coal," Nenryo Kyokai-shi 49 (524), 890-97 (1970).

#### IV. Patent Status

The work performed during April is not considered patentable.

#### V. Future Work

The data collection and evaluation work will be continued in the selected areas of coal conversion technology.

Approved

W.W. Bodle

W. W. Bodle, Director  
Process Analysis

Signed

A. Talwalkar

A. Talwalkar, Coordinator  
Process Data

IGT-MPR--7

**INSTITUTE OF GAS TECHNOLOGY**



3424 SOUTH STATE STREET

IIT CENTER

CHICAGO, ILLINOIS 60616

AFFILIATED WITH ILLINOIS INSTITUTE OF TECHNOLOGY