APPENDIX A. CATALYST TESTING: SUMMARY OF RUNS
REPORTED DURING THIS QUARTER

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This report is organized around the eight catalyst tests conducted from January through March 1986, the sixth quarter of this contract.

A list of the catalysts tested, a description of their preparation, and a brief statement of each test's objective, are shown in Table A1, except for the single blank run (Run 52). All of the catalysts tested involved cobalt oxide and additive X₁₁ intimately contacted with one of three supports: Molecular Sieve TC-121 (Run 50), Molecular Sieve TC-123 (Runs 51, 53, 54, 55 and 56), and γ-alumina (Run 49). The five TC-123 supported catalysts were used to study the effects of the additional promoter X₉ (Runs 51, 55 and 56), the additional promoter X₁₃ (Run 54), and the co-mixing with extrudates of a water gas shift catalyst.

An abbreviated table of results for these catalyst runs is shown in Table A2. The conversion, weight percent CE4, weight percent C5⁺, and specific activity, as well as a qualitative estimate of stability, are listed for each catalyst. A more complete report of results and analyses of these runs will be presented in the Seventh Quarterly Report.

Because of the large error inherent in its computation

(based on an alpha that is determined solely from the C_3 - C_6 compounds found in the off-gas), the methane factor will no longer be presented for the preliminary data given in monthly reports and in Appendix A (i.e., this Appendix) of the Quarterly Reports.

Table Al. Description of most of the catalysts tested during the sixth quarter.

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Run	Catalyst	Catalyst preparation	Objective of test				
49	Co/X ₁₁ /γ-A1 ₂ O ₃ (12561-O4)	The X_{11} promoted cobalt oxide catalyst was formulated similarly to Catalyst 45, except that the TC-123 was replaced by γ -alumina. Theoretical pct Co=8.2, pct X_{11} =1.6.	To help determine the effects of the TC-123 support on catalyst performance.				
50	Co/X ₁₁ /TC-121 (11617-08)	The X ₁₁ promoted cobalt oxide catalyst was formulated similarly to Catalyst 45, except that TC-123 was replaced with a new Molecular Sieve, TC-121. Theoretical pct Co=8.2, pct X ₁₁ =1.6.	To test the use of TC- 121 as the catalyst sup- port.				
51	Co/I ₉ /I ₁₁ /TC-123 (12570-03)	The I ₁₁ promoted cobalt oxide catalyst was formulated similarly to Catalyst 45, except that an additional promoter, I ₉ , was added. Theoretical pct Co=8.2, pct I ₉ =1.1, pct I ₁₁ =1.6.	To screen the effect of adding the X9 promoter to an X11 promoted system.				
52	Blank (12561-03)	Quartz chips.	To test the reactor for inherent catalytic activity.				
53	Co/X ₁₁ /TC-123 + K/Ni/Mo-γ-alu- mina (12561-05)	The X ₁₁ promoted cobalt oxide catalyst was formulated similarly to Catalyst 45. 1/8" extrudates of this were combined with 1/8" extrudates of K/Ni/Mo- γ -alumina, which occupied 30% of the total catalyst volume. Theoretical pct Co=5.7, pct X ₁₁ =1.1.	To test the addition of a water gas shift component to a Co/X ₁₁ /TC-123 catalyst.				
54	Co/X ₁₁ /X ₁₃ /TC-123 (11617-09)	The I ₁₁ promoted cobalt oxide catalyst was formulated similarly to Catalyst 45, except that an additional promoter, X ₁₃ , was added. Theoretical pct Co=8.1, pct X ₁₁ =1.6, pct X ₁₃ =0.7.	To screen the effect of adding the promoter X ₁₃ to an X ₁₁ promoted system.				

continued

Table Al, continued.

Run	Catalyst	Catalyst preparation	Objective of test
55	Co/Ig/I ₁₁ /TC-123 (12570-04)	The X9, X11 promoted cobalt oxide catalyst was formulated similarly to Catalyst 51, except that an extra calcination step was incorporated into the formulation procedure. Theoretical pct Co=8.0, pct X9=1.1, pct X11=1.6	To repeat the results of Run 51 as well as to screen the effects of the added calcination step.
56	Co/X9/X ₁₁ /TC-123 (12561-06)	The Xg, X ₁₁ promoted cobalt oxide catalyst was formulated similarly to Catalyst 55 except that the concentration of the X ₁₁ additive was reduced. Theoretical pct Co=8.0, pct X ₉ =1.1, pct X ₁₁ =1.0.	To further screen the x_{11} promoter effects.

Table A2. Preliminary catalyst test results for most of the runs made during the sixth quarter.

Run	Catalyst	Hours on stream	Total conver- sion (CO+H ₂)	CH4 wt %	C ₅ + wt %	Spe- cific acti- vity	Stability
49 ,	Co/I ₁₁ - Y-Al ₂ O ₃ (12561-04)	66.0 138.0	48.7 45.0	6.9 7.1	82.3 82.5	3.22 3.40	Excellent ¹
		162.0 258.0	62.3 58.2	8.1 10.0	81.0 76.5	3.35 2.86	Fair ²
		283.0 331.0	73.6 69.0	14.8 16.5	70.7 67.6	1.18 0.95	Fair ³
50	Co/X ₁₁ /TC-121 (11617-08)	48.5 166.0	34.3 31.8	10.2 9.9	77.3 78.3	1.28 1.10	Fairl
51	Co/Xg/X ₁₁ /TC-123 (12570-03)	45.5 166.5	46.0 44.5	4.0 3.5	89.6 89.2	3.09 2.99	Excellent ¹
Ý		214.5 331.0	56.6 55.5	6.8 6.8	83.2 83.2	1.86 1.91	Excellent ²
		358.0 478.5	77.8 75.9	11.9 9.2	77.5 81.9	1.44 1.16	*Good3
52	Blank (quartz chips) 24.0 no activity (12561-03)						
53	Co/X ₁₁ /TC-123 + K/Ni/Mo- γ-alumina	19.2 43.7	50.5 45.4	7.0 6.1	77.3 78.2	2.63 2.55	1
V	(12561–05)	68.2	62.4	4.5	85.2	1.52	4
		91.2 163.7	75.3 72.3	17.4 16.4	69.0 69.9	0.94 0.85	Fair ³

*Estimate of stability questionable due to mechanical problems. Reactor conditions:

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^{1:1} H₂:CO, 300 GHSV. 1. 240C, 300 psig,

^{2. 260}C, 3.

⁵⁰⁰ psig, 1.5:1 H₂:CO, 1:1 H₂:CO,

Table A2, continued.

Rum	Catalyst	Hours on stream	Total conver- sion (CO+H ₂)	CH4 wt Z	C5+ vt %	Spe- cific acti- vity	Stability
54	Co/X ₁₁ /X ₁₃ /TC-123 (11617-09)	27.8 122.8	55.2 51.3	4.4 4.5	84.0 82.8	5.23 4.05	Excellent ¹
	1.5	147.3 170.3	65.7 67.6	16.5 14.9	68.2 71.0	3.18 3.27	Excellent ⁵
	1,5/1 5 ec "	193.3	85.2	28.97	47.8	1.65	3
	(st	216.8 266.3	71.9 65.6	5.3 5.0	84.8 84.9	2.58 1.95	Fair ⁴
	12/1 1 160	289.3 506.8	72.8 65.4	8.9 4.8	79 . 9 86 . 5	1.71 1.76	Fair6
55	Co/X9/X11/TC-123 (12570-04)	24.5 48.5	35.8 40.7	6.8 3.5	79.9 88.8	1.70 2.70	1
	, , , , , , , , , , , , , , , , , , , ,	71.5 886.5	75.4 68.5	9.3 9.3	80.3 81.0	1.39 0.78	Good ³
56	· Co/Xg/X ₁₁ /TC-123 (12561 - 06)	48.0 192.5	48.7 47.7	5.5 4.6	85.3 86.2	3.03 3.13	Excellent ¹
		216.5 360.5	79.8 76.1	14.3 12.9	73.9 76.0	1.34 1.04	Fair ³

Reactor conditions:
1. 240C, 300 psig, 1:1 H2:CO, 300 GHSV.
3. " 500 psig, 1.5:1 H2:CO, "
4. " " 1:1 H2:CO, "
5. 240C, 300 psig, 1.5:1 H2:CO, "
6. 260C, 500 psig, 1.2:1 H2:CO, "