

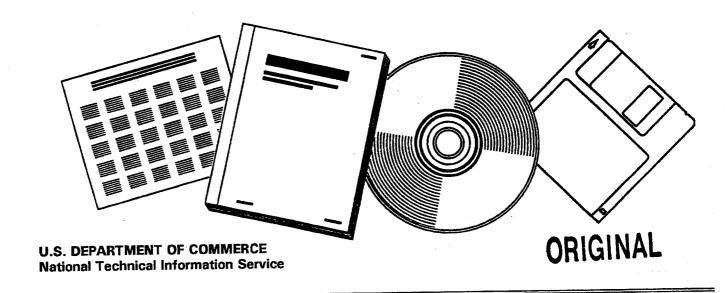
DE90002792



SLURRY REACTOR HYDRODYNAMICS STUDIES: FINAL REPORT

AIR PRODUCTS AND CHEMICALS, INC. ALLENTOWN, PA

1985



DOE/PC/30021--T20 DE90 002792

SLURRY REACTOR HYDRODYNAMICS STUDIES

FINAL REPORT

Work Performed Under
DOE Contract No. DE-AC22-80PC30021

Air Products and Chemicals, Inc.
Allentown, PA 18195

DISCLAIMER

This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.

1285G

Abstract

Air Products has completed a three-year BOE contract in which new slurry phase catalysts (Task 2) and slurry phase bubble column reactor correlations (Task 3) for the Fischer-Tropsch synthesis were developed. This report presents results from the reactor studies.

Using both a 12.7 and a 30.5 cm diameter cold flow simulator, phase holdups, phase dispersion coefficients, and interphase heat and mass transfer coefficients were measured and correlated. This information was incorporated into a computer model of a three-phase bubble column. The heat and mass transfer and phase dispersion correlations were found to conform to the literature, while the phase holdup correlations were different. Combining product distributions from the Task 2 catalyst tests with the results of the Task 3 hydrodynamic studies allowed prediction of space-time yields of product fuel fractions in larger-scale slurry bubble columns.

Slurry Reactor Hydrodynamic Studies Final Report

Table	of Conte	nts	Page #
	Execut	ive Summary	1
1.0	Introd	uction	4
	1.1	Background	5
	1.2	Slurry Reactors	6
	1.3	Flow Regimes	7
2.0	Task 3	Objective	8
	2.1	Dependent Variables	9
	2.2	Independent Variables	10
3.0	Experi	mental Procedure	11
4.0	Physic	al Property Determination	12
5.0	Gas Ho	ldup	14
	5.1	Literature Review	14
	5.2	Experimental	27
	5.3	Results	29
	5.4	Discussion	30
6.0	Bubble	Size	31
	6.1	Theory	32
	6.2	Experimental	· 32
	6.3	Results	35
	6.4	Discussion	35
7.0	Mass T	ransfer	37
	7.1	Theory	38
	7.2	Experimental	38
	7.3	Results	39
	7.4	Discussion	39
8.0	Liquid	Dispersion	41
	8.1	Theory	42
	8.2	Experimental	44
	8.3	Results and Discussion	45

Table	of Conte	ents	Page #
9.0	Solid	Loading and Concentration Profiles	46
	9.1	Theory	47
	9.2	Experimental	50
	9.3	Results	51
	9.4	Discussion	52
	9.5	Conclusions	54
10.0	Heat	Transfer	55 , *
	10.1	Theory	56
	10.2	Experimental	57
	10.3	Results and Discussion	59
11.0	Engineering Evaluation		61
	11.1	Staged Reaction Systems	64
12.0	Acknowledgements		65
13.0	Nomenclature		65
14.0	References		70
15.0	Table	s	80
16.0	Figures		109
A.0	Appendices		144
	A.5	Appendix to Section 5	144
	A.9	Appendix to Section 9	148
	A.11	Appendix to Section 11	151

List of Tables

Table		Page	#
2.1	Slurry Reactor Design Studies (Variables)	80	
4.0	Physical Properties of Liquids and Solids	81	
5.3.1	Gas and Solid Holdup: 5-Inch Cold Flow Simulator	82	
5.3.2	Gas and Solid Holdup: 12-Inch Cold Flow Simulator	96	
6.3.1	Bubble Diameter Results12-Inch Cold Flow Simulator (Uncorrected)	99	
6.4.1	Bubble Diameter Results—12-Inch Cold Flow Simulator (Corrected)	100	
7.3.1	Gas/Liquid Mass Transfer Coefficients5-Inch Cold Flow Simulator	101	
10.3.1	Shellside Heat Transfer Coefficients: 12-Inch Cold Flow Simulator	103	
11.0.1	Rheinpreussen Simulation Using Deckwer Correlations	105	
11.0.2	Rheinpreussen Simulation Using APCI Correlations	106	
11.0.3	Optimum Gas Holdup, Gas Velocity, and Space-Time Yield	107	
11.1.1	Rheinpreussen SimulationStaged Reaction Systems	108	

List of Figures

Figure		Page	#
1.2	Three-Phase Slurry Reactor Types	109	
3.1	Bubble Column Schematic	110	
5.2.1	Gas Holdup AnalysisMethod 2	111	
5.2.2	Gas Holdup AnalysisMethod 3	112	
5.4	Gas Holdup vs. Gas Velocity for Different		
	Solids/Liquids	113	
6.2.1	Bubble Size Analysis System	114	
6.2.2	Bubble Diameter Double Cone Probe	115	
6.2.3	Bubble Trace from Double Cone Probe	116	
6.2.4	Calibration Chamber	117	
7.3.1	Gas/Liquid Mass Transfer Coefficients5-Inch Cold Flow		
	Simulator	118	
8.0.1	Dispersion Coefficient vs. Gas Velocity (Previous		
	Workers)	119	
8.2.1	Automated Liquid Dispersion System	120	
8.2.2	Normalized Concentration vs. Time Curves at		
	3.5 Inches for 48-Inch Bed	121	
8.2.3	Normalized Concentration vs. Time Curves at		
	14.75 Inches for 48-Inch Bed	122	
8.2.4	Normalized Concentration vs. Time Curves at		
	29.75 Inches for 48-Inch Bed	123	
8.2.5	Normalized Concentration vs. Time Curves at		
	44.58 Inches for 48-Inch Bed	124	,
8.2.6	Conductivity Probes	125	J
8.2.7	Liquid Dispersion Coefficient Experiments - Raw Output	126	j
0 2 0	liquid Disparsion Coefficient Experiments - Smoothed Data	a 127	į

List of Figures (continued)

Figure		Page	Ą
9.3.1a	Particle Size Effect on Solid Profiles. V _L =0, SiO ₂	128	
	Particle Size Effect on Solid Profiles, V,>0, SiO ₂	129	
	Particle Size Effect on Solid Profile:, V ₁ =0, Fe ₃ O ₄	130	
	Particle Size Effect on Solid Profiles, V _L >0, Fe ₃ O ₄	131	
9.3.3a	Particle Type and Liquid Effect, V _L =0	132	
9.3.3b	Particle Type and Liquid Effect, $V_{L}>0$.	133	
9.4.1	Solids Settling Velocity, Observed vs. Theoretical	134	
9.4.2	Solid Dispersion Coefficient, Literature Comparison	135	
9.4.3	Maximum Solid Loading, 12" Cold Flow Simulator	136	
	Placement of Heaters	137	
10.2.2	Cartridge Heater Arrangement	138	
10.3.1	Heat Transfer vs. Gas Velocity (Results)	139	
10.3.2	Heat Transfer vs. Gas Velocity (Air Products vs.		
	Deckwer)	140	
	Space-Time Yield at Rheinpreussen Conditions	141	
	Staged Reaction Systems	142	
11.1.2	Hydrogen Conversion vs. Column Height (Staged Reaction		
	Systems)	143	