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REPORT ON

NISSAN EKITAI NENRYO CO., LTD.

WAKAMATSU PLANT

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I. INTRODUCTION

The Wakamatsu low-temperature coal carbonization plant, of the NISSAN EKITAI NENRYO K. K., was inspected by the Petroleum Section of the U. S. Naval Technical Mission to Japan, during the period 24-25 October, 1945. This report records and summarizes the technical information obtained during this visit. Japanese personnel connected with the plant, who assisted in supplying this information, were as follows:

Mr. N. YAMADA
Mr. S. KUNII
Mr. T. FUJIO
Mr. T. MONDEN

Mr. T. MONDEN

Director of Plant.
Head of Carbonization and
Refining Departments.
Head of Mechanical Dept.
Office Manager.

II. HISTORY AND ORGANIZATION

The company was founded on 25 February 1939, with an initial capitalization of 10,000,000 Yen, and construction was started on a plant at WAKAMATSU, to produce oil from coal mined nearby in the Orio district of NOPTH KYUSHU. The design of the low-temperature carbonization plant was based on the patents of the Lurgi-Gesellschaft, Frankfurt-am-Main. Complete licensing rights for this process had been purchased by the Teikoku Nenryo Co., Ltd., who in turn, sublicensed to the Nissan Rkitai Nenryo Company. The first units of the Wakamatsu plant were completed in March 1941, and consisted of a Lurgi low-temperature retort of 300 tons/day coal charge capacity plus tar separating and light oil distilling equipment. Production of gasoline, fuel oil and semi-coke was started. Additional refining equipment, including far distillation, light oil treating, and de-waxing units, were completed by the middle of 1942, and from that time on, the plant produced motor gasoline, diesel oil, fuel oil, pitch, semi-coke (coalite) and raw wax.

Three German engineers from Lurgi-Gesellschaft assisted in the construction and acceptance tests of the first units. Mr. Finkbeiner arrived in September, 1940, Mr. Erb in December, 1940 and Mr. Bruggeman in March, 1941. All three departed in June, 1941.

In September, 1941, the Japanese Government ordered an extension of the plant, and work was started on the construction of three additional low-temperature retorts plus auxiliary equipment. For this extension, the capitalization of the company was increased to 15,000,000 Yen on 22 December 1941, and a special "accommodation" loan of 15,000,000 Yen additional was obtained from the Teikoku Menryo Company. The first additional unit was completed in May, 1943, the second in May, 1944, and the third in November, 1944. In connection with this extension, the company also undertook installation of additional tar distilling and dewaxing units, also gasoline and phenol distillation equipment. This equipment was still in the process of construction in October, 1945. To finance this construction, the capitalization was increased, on 15 November 1944, to 25,000,000 Yen.

The plant maintained steady production with two or three units continuously on stream until the fire-bonb raid of 8 August 1945. Although damage was relatively light, destruction of the central ter oil pumping room necessitated a shut down of the entire plant. It was anticipated that production would be started again in Movember, although the supply of coal was becoming critical due to labor difficulties at the mines.

In the initial establishment of the company, it was planned to install a pilot plant for the hydrogenation of tar oils, and reaction vessels had been ordered from the Krupp Corp. in Germany. These vessels were not delivered and other

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items required were never ordered, due to increasing difficulties in procuring construction materials.

The main offices of the company are located in TOKYO, and at present, of the total capitalization of 25,000,000 Yen (20,000,000 paid up), the Teikoku Nenryo Company owns 50 per cent and the balance is largely held by the Nippon Kogyo Co., Ltd. (Nippon Mining Co.) The top management of Nissan Ekitai Nenryo Co. is as follows:

President:	Mr. M. FURUKAWA			
Directors:	Mr. J. TANAKA Mr. N. YAMADA Mr. E. SUZUKI Mr. T. YAMADA Mr. S. UCHIDA			
Inspectors:	Mr. S. NATSUBORI Mr. R. KUMADA			
Counsellors:	Mr. M. FUJITA Mr. M. TAKASHIMA			

The management of the Wakamatsu plant is as follows:

Mr. N. YAMADA. Mr. S. KUNII Plant Director Head of Low-Temp. Carb. and Tar Oil Refining Depts. Head of Mechanical Dept. Mr. T. MONDEN

Office Manager

Before the end of the war, the plant had a total of about 700 employees.

The Missan Ekitai Nenryo Company has no other plants in or outside of Japan.

III. DESCRIPTION OF PROCESS

A layout map for the Wakamatsu Plant is given by Plate I(H), and an over-all flow diagram is given by Plate II(H).

The coal charged to the low-temperature carbonization units is obtained from mines in the Orio district, and was stated to be a coal with low sulphur content (0.5%), poor coking qualities, and well suited for gasification. A flow about of the lurgi-design low temperature-carbonization plant is given by sheet of the Lurgi-design low temperature-carbonization plant is given by Plate III(H). Coal is conveyed to the coal bunkers at the top of the retort and passes downward through the drying zone at about 250°0 and the carbonization zone at 600°C. The coke (coalite) is cooled by cold circulated fuel gas, introduced at the bottom of the retort. Heat for carbonization and drying is supplied by circulating gas from each of these zones through external "verbrennungsofen's". Hot carbonization gas, withdrawn from the top of the carbonization zone, is passed successively through the pre-cooler, Cottrell precipitator, coolers, and gasoline absorber. A flow diagram for the latter unit is given by Plate IV(H).

Tar from the pre-cooler and Cottruit is sent to batch ter stills (total charge capacity 10 tons oil per 24 hours) and fractionated into pitch and heavy oil. The heavy oil is dewaxed by cooling to -5°C and filtering. The desaxed oil is used either in bunker or semi-diesel fuels, and the rem wax is sold for use in lubricating oil manufacture.

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Both the crude middle oil from the coolers and gasoline from the absorption plant are washed with 10% caustic, to remove phenols and cresols, which are recovered and sold. The neutral middle oil can be used in diesel oil or fractionated for production of solvent naphthas. The caustic washed gasoline is treated with 60° Be. sulphuric acid, then with 4% caustic, and finally washed with water.

IV. PRODUCTION

Capacity of each of the four Lurgi retorts is 300 tons of cost per 24 hours. Table I(H) summarizes actual quantities of coal charged during the period from the start of operations on 16 April 1941, to 8 August 1945, when production was stopped as the result-of a fire-bomb raid on that date. The consumption of NaOH and HoSO, is given by Table II(H). Actual output of products is given by Table III(H). The yield of oil obtained is about 90% of that shown by the Fischer-Hempel carbonization test. No major operating difficulties were encountered, although actual retort throughputs varied with the coking properties of the coal.

Typical inspections on the several products are given in Table IV(H). No significant difference existed between design and actual product yields and quality.

In general, the plant appeared to be well-managed, and the maintenance of equipment was good.

V. RESEARCH AND DE VELOPMENT

The research department was very small, consisting of only three chemists plus assistants, and it was primarily concerned with tests necessary in controlling plant operations. The following Japanese patents regarding low-temperature carbonization are held by the company:

Patent No.	Date of Patent	Inventor	Title of Patent
No. 67614	25 Feb., 1926	0. Hubman	Process of drying fuels and its equipment.
No. 73611	28 Sept.,1927	G. Munschel	Process of drying fuels and its equipment.
No. 82931	4 Nov., 1929	O. Hubman	Equipment for low-temperature carbonization of fuels by internal heating.

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Table I(H)
ACTUAL COAL CHARGED TO WAKAMATSU PLANT

		Metric Tons						
-	1941	1942	1943	1944	1945			
Jan.		7,162	10,230	15,245	20,794			
Feb.	*# 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	7,015	3,630	16,002	14,801			
Mar.		7,669	7,797	16,120	19,602			
Apr.	2,978	6,656	11,109	15,417	. 20,149			
Kay	7,781	108	8,017	19,063	13,427			
June	5,906	8,219	13,690	16,693	18,441			
July	7,662	10,602	18,612	17,956	11,308			
Aug.	6,815	8,957	17,817	18,388	2,136			
Sept.	7,457	9,539	15,390	17,536	0			
Oot.	6,849	8,145	10,831	18,454	0			
Nov.	6,740	5,404	10,468	19,102				
Dec.	7,221	9,073	18,019	22,010				
Total	59,409	88,579	139,610	211,976	120,444			

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Table II(E)

ACTUAL CONSUMPTION OF

SODIUM HYDROXIDE AND SULPHURIC ACID

(Metric tons)

1943			19	44	1945		
	NaOH	H2804	NaOH	H ₂ S04	NeOH	H ₂ S0	
Jan.	42.5 -	-54 - -55	3 .	. 4	15	38	
Feb.	-		56	83	9	19	
Mar.			76	100	24	29	
Apr.			41	52	29	29	
kay	-	-	27	44	28	44	
June	-	~	40	72	28	51	
July	_	-	33	57	44	54	
Aug.	-	-	39	71	6	13	
Sept.	-	-	41	75	0	0	
Oat.	37	64	43	72	0	0	
Nov.	40	66	20	38		-	
Deo.	30	44	21	35	-	-	
Total	107	174	440	697	183	277	

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Table III(H)
ACTUAL PRODUCTION AT WAKAMATSU PLANT

	٦.	Semi-cokes (tons)	Gasoline (kl)	Fuel oil (kl)
1941	Apr. May June July Aug. Sept. Oct. Nov. Dec.	1,856 4,740 3,721 4,814 4,496 4,792 4,318 4,246 4,549	0 0 31 139 145 151 115 107 168	286 717 638 700 758 769 607 566 734
1942	Jen. Feb. Mar. Apr. May June July Aug. Sept. Oot. Nov. Dec.	4,513 4,420 4,832 3,919 68 5,178 6,892 5,822 6,220 5,294 3,518 5,898	132 132 148 141 0 148 157 161 168 134 65 125	645 934 701 626 68 753 992 824 862 738 505 909
1	Total	56,574	1,531	8,557

Note: Semi-diesel, pitch, and orude wax were not produced.

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Table III(H) (cont'd)
ACTUAL PRODUCTION AT WAKAMATSU PLANT

		Semi-cokes (tons)	Gasoline (kl)	Semi-dies (kl)	el	Fuel (kl)		Pito			ons)
1943	Jan. Feb. Mar. Apr. May June July Aug. Sept. Oct. Nov. Dec.	6,419 2,285 4,859 7,030 6,936 9,326 11,997 11,458 10,556 7,268 6,721 7,711	126 42 86 137 154 161 150 157 341 191 143 209	507 172 76		968 327 736 1,173 1,076 1,74 1,700 1,52 1,01 65 56	7 3 3 5 5 9 9 0 7 0		28		- - - - - - 6 8
		Semi-cokes	Gasoline (kl)	Semi- Diesel (kl)		1 011 kl)	Pit (to			sol	Crude wax (tons
1944	Jan. Feb. Mar. Apr. May June July Aug. Sept. Oot.	9,486 10,307 10,378 9,923 12,290 10,753 11,517 11,567 11,301 10,985	73 81 160 0 89 152 553 272 372 272	63 0 187 182 170 170 259 200 69 281		,152 ,059 1,076 983 1,607 1,307 1,378 1,429 1,610	3 1	00000	-	75 25 14 18 17 25 37	70000000000
	Nov. Dec. Total	11,371 15,550 135,728	75 150 2,249	78 180 1,859		1,490 1,717 6,279	4	37 30 02	3	0 0 59	7
1945	Jen. Peb. Mar. Apr. May June June July Aug. Bept. Oct.	12,796 9,090 12,057 12,599 8,229 11,340 6,915 1,303	131 123 176 124 0 104 204 87 0	61 56 415 466 414 266 350 62 0	1	1,847 1,246 1,301 1,433 679 1,195 410 79 0	1	63 8 20 70 25 02 95 33 0		0 7 0 22 0 0 0 0 0	0 0 12 24 0 0 0
1	Total	74,129	949	2,088	-	8,190	7 3	96	$oldsymbol{ol}}}}}}}}}}}}}}}}}}$	20	36

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Table IV(H)
PROPERTIES OF PRODUCTS

			Liquid Fuels (°C)	
		Semi-diesel Oil	Fuel 011	Motor Gasoline
Distillation	Dew point 5% 10% 20% 30% 40% 50% 60% 70% 80% 90%	76 222 233 248 257 270 282 318 350	98 238 256 293 332 349 370 372	72 108 114 126 135 142 151 160 168 179 194 216
Composition	Acidic oil (%) Basic oil (%) Neutral oil (%)	19.0 2.0 79.0	36.5 0.5 63.0	
Red. Visc. (50	OC secs)	36	174	
Flash Point (°C) '	67	118	
Specific Gravi	lty	0.941 (15°C)	0.967 (50 ⁸ C)	795 (15° 0)
Solidifying Po	oint (°0)	. 13	31	
Spoot. Ign. Po	oint (°C)	285		

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Table IV(H) (Cont.) PROPERTIES OF PRODUCTS

Pitch

The second secon	and the second s
Solidifying point	above 150°C
Volatile matter	54.86%
Fixed carbon	44.88%
Ash	0.26%
Creso	<u>la</u>
Distillation	,
Dew point 54 106 206 303 406 506 706	76 ⁰ C 199 (H ₂ 0 3.8%) 205 207 209 211 215 225 268
Cok	<u>e</u>
Volatile matter	9.4%
Fixed carbon	67.5%
.asbdak.	22.5%
Bulfur	
Calorific value	6,000 Cals

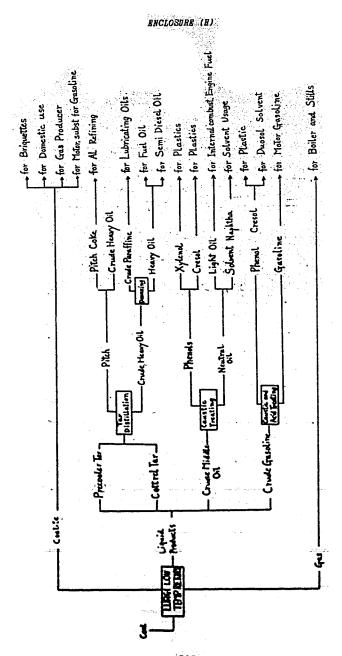


Figure 1(H)
OVER-ALL FLOW SHEET

