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(54) **Catalyst preparation**

(57) A catalyst for the production of  
methanol from syngas is prepared by  
dispersing in water a co-precipitate

comprising zinc as well as chromium  
and/or aluminium together with a co-  
precipitate of copper, zinc and  
optionally chromium and/or  
aluminium, spray drying the dispersion  
and calcining the spray dried material.

**GB 2 130 114 A**

# **SPECIFICATION** **Catalyst preparation**

The invention relates to a process for the preparation of a catalyst suitable for use in the conversion of a mixture of carbon monoxide and hydrogen into methanol.

5 Among the catalysts eligible for use in the preparation on a technical scale of methanol from carbon monoxide and hydrogen, those containing copper, zinc and in addition chromium and/or aluminium are of considerable importance. The preparation of these catalysts usually comprises drying and calcining a co-precipitate obtained by adding a basic reacting substance to an aqueous solution containing salts of all the relevant metals concerned. The catalysts thus prepared have a high 10 selectively towards methanol; however, both their activity and their stability are insufficient. 10

In order to solve this problem the Applicant investigated whether spray drying would lead to enhanced performance of catalysts as described above. Spray drying is a process which has been in use for many years for the preparation of small globular particles from a solid or a mixture of solids. The process is carried out by atomizing a dispersion in water of the material to be spray 15 dried through a nozzle or from a rotating disc into a hot gas. The application of spray drying in the preparation of the catalysts concerned comprised replacing conventional drying of the aforementioned co-precipitate (which had been prepared by precipitating all metal components together) by spray drying. This change in working up resulted in considerable improvement of the stability of the catalysts, but also in a severe drop in activity. However, in view of 20 the favourable effect spray drying had on the stability of the catalysts, further investigation was carried out to attempt to achieve improved catalysts by introducing changes in the method of preparing the co-precipitate, while maintaining the spray drying. In accordance with the present invention, the change which was made in the preparation of the co-precipitate consisted in the preparation not of a single co-precipitate containing all the metals involved, but of two separate co-precipitates having different 25 compositions. The preparation of the catalyst was carried out by dispersing the two co-precipitates together in water, spray drying the dispersion thus obtained and calcining the spray dried material. Also in accordance with the invention, it was found that this technique leads to catalysts having both a very high activity and a very high stability, provided that the composition of each individual co-precipitate as well as the mixing ratio of the co-precipitates in the dispersion meet all following requirements:

- 30 1) One co-precipitate (hereinafter referred to as co-precipitate A) should contain zinc as well as chromium and/or aluminium in such quantities that the  $Zn/(Cr+Al)$  atomic ratio is 0.25—4. 30
- 2) The other co-precipitate (hereinafter referred to as co-precipitate B) should contain copper as well as zinc and, if desired, chromium and/or aluminium in such quantities that the  $Cu/Zn$  atomic ratio is lower than 10 and the  $(Cr+Al)/(Cu+Zn)$  atomic ratio is lower than 2. 35
- 3) The two co-precipitates should be dispersed in water together and in such quantities that in the dispersion the atomic ratio of the sum of the metals coming from co-precipitate A to the sum of the metals coming from co-precipitate B is 0.25—3 and the  $Cu/(Cu+Zn+Cr+Al)$  atomic ratio is higher than 0.1. 35

Any deviation from one or more of these three requirements will result in catalysts having either 40 low activity or low stability, or a combination thereof. 40

The importance of including a spray drying step in the present catalyst preparation is made evident by the results of an experiment in which two separately prepared co-precipitates were mixed and the mixture was dried and calcined in the conventional manner. Although the co-precipitates used met the requirements mentioned under 1) and 2) and the mixing ratio used met the requirements 45 mentioned under 3), the catalyst obtained showed moderate activity and extremely low stability. 45

The present patent application therefore relates to a process for the preparation of a catalyst, in which a co-precipitate A containing zinc as well as chromium and/or aluminium in such quantities that the  $Zn/(Cr+Al)$  atomic ratio is 0.25—4 and a co-precipitate B containing copper as well as zinc and, if desired, chromium and/or aluminium in such quantities that the  $Cu/Zn$  atomic ratio is lower than 10 50 and the  $(Cr+Al)/(Cu+Zn)$  atomic ratio is lower than 2, are together dispersed in water in such quantities that in the dispersion the atomic ratio of the sum of the metals coming from co-precipitate A to the sum of the metals coming from co-precipitate B is 0.25—3 and the  $Cu/(Cu+Zn+Cr+Al)$  atomic ratio is higher than 0.1, in which the dispersion thus obtained is spray dried and in which the spray 50 dried material is calcined. 50

55 In the process according to the invention two metal-containing co-precipitates are used which have been prepared separately. The preparation of each of these co-precipitates may very suitably be carried out by adding a basic reacting substance to an aqueous solution containing salts of the relevant metals. The basic reacting substance is preferably used in the form of an aqueous solution. Suitable basic reacting substances which may be used in the preparation of the metal-containing co-precipitates are ammonia, soda and alkali metal hydroxides. Co-precipitation is preferably carried out in 60 a mixture with a continuous supply of an aqueous solution containing the relevant metal salts and an aqueous solution of the basic reacting substance in stoichiometric quantities, calculated on the metals 60

and with a continuous discharge of the co-precipitate formed. Before the co-precipitates are together dispersed in water, they should advisably be allowed to age in the mother liquor for some time and subsequently be washed thoroughly with water.

As mentioned above, in the process according to the invention a co-precipitate A should be used in which the  $Zn/(Cr+Al)$  atomic ratio is 0.25—4. Preferably a co-precipitate A is chosen in which this atomic ratio is 0.5—3. As regards co-precipitate B in which the  $Cu/Zn$  atomic ratio should be lower than 10 and the  $(Cr+Al)/(Cu+Zn)$  atomic ratio lower than 2, preference is given to the use of a co-precipitate B in which these atomic ratios are lower than 5 and lower than 1.5, respectively. As regards the mixing ratio of the two co-precipitates, which should be chosen such that in the dispersion the atomic ratio of the sum of the metals coming from co-precipitate A to the sum of the metals coming from co-precipitate B should be 0.25—3 and the  $Cu/(Cu+Zn+Cr+Al)$  atomic ratio higher than 0.1, this mixing ratio should preferably be chosen such that said atomic ratios are 0.5—2 and higher than 0.15, respectively.

The catalysts which can be produced according to the invention contain copper and zinc and in addition chromium and/or aluminium. Preference is given to  $Cu/Zn/Cr$  and  $Cu/Zn/Cr/Al$  catalysts. These catalysts are preferably prepared by using a co-precipitate A which, as the metals, contains exclusively zinc and chromium. For the preparation of  $Cu/Zn/Cr$  catalysts the two preparing combinations that the feasible  $(Zn/Cr+Cu/Zn)$  or  $Zn/Cr+Cu/Zn/Cr$  are in conformity with said preference. For the preparation of  $Cu/Zn/Cr/Al$  catalysts, where six preparing combinations are feasible, preference is therefore given to the combinations  $Zn/Cr+Cu/Zn/Al$  and  $Zn/Cr+Cu/Zn/Cr/Al$ .

The catalysts prepared according to the process of the invention are excellently suitable for use in the conversion of a mixture of carbon monoxide and hydrogen into methanol. The present patent application therefore also relates to a process for the conversion of a mixture of carbon monoxide and hydrogen into methanol using a catalyst obtained according to the invention, starting from two separate co-precipitates A and B and using spray drying. Before they are suitable for this use, the catalysts should be reduced. This reduction is preferably carried out at a temperature of 150—350°C. The  $H_2/CO$  mixture used preferably has a  $H_2/CO$  molar ratio higher than 1.0. Examples of suitable  $H_2/CO$  mixtures eligible as feeds to be used in the process are  $H_2/CO$  mixtures obtained by coal gasification and  $H_2/CO$  mixtures obtained in the catalytic steam reforming of light hydrocarbons, such as methane.

The conversion of  $H_2/CO$  mixtures into methanol by using a catalyst prepared according to the invention is preferably carried out at a temperature of 175—350°C and in particular of 200—275°C, a pressure of 5—150 bar and in particular of 20—100 bar and a space velocity of 250—25000 NI synthesis gas per l catalyst per h and in particular of 500—10000 NI synthesis gas per l catalyst per h. In view of the activity and stability of the catalyst the feed used is preferably a  $CO_2$ -containing  $H_2/CO$  mixture and in particular a  $H_2/CO/CO_2$  mixture containing 0.5—25 %v  $CO_2$ , calculated on  $H_2/CO/CO_2$  mixture. Usually a synthesis gas prepared by coal gasification or by catalytic steam reforming of light hydrocarbons contains a quantity of  $CO_2$  which lies within the limits given hereinbefore. If the available synthesis gas contains too much  $CO_2$ , the  $CO_2$  concentration may be reduced by washing the gas. If the available synthesis gas contains too little  $CO_2$ ,  $CO_2$  may be added or the synthesis gas may be subjected to the CO shift reaction ( $CO+H_2O \rightleftharpoons CO_2+H_2$ ). Irrespective of the  $CO_2$  content of the synthesis gas the latter reaction may be carried out any way in order to raise the  $H_2/CO$  ratio of a synthesis gas with a low  $H_2/CO$  ratio.

The conversion of a  $H_2/CO$  mixture into methanol by using a catalyst prepared according to the invention may be carried out using a fixed catalyst bed or a moving catalyst bed, in particular a fluidized catalyst bed. Since the catalysts have very high activity, high degrees of conversion can be achieved at high space velocities. Preferably the present catalysts are used in the form of a fluidized bed.

The conversion of a  $H_2/CO$  mixture into methanol using a catalyst according to the invention may very suitably be carried out as an individual process in which the synthesis gas is converted in a single step. If desired, unconverted synthesis gas may be recirculated.

The conversion of a  $H_2/CO$  mixture into methanol using a catalyst prepared according to the invention may also very suitably be carried out as part of a multi-step process for the conversion of a  $H_2/CO$  mixture. A number of options may be distinguished in that case, viz.

A) The process is used as the first step of a two-step process in which in the first step methanol is formed and in which  $H_2$  and CO present in the reaction product of the first step, together with other components of this reaction product, if desired, is contacted in the second step with a catalyst comprising one or more metal components which have activity for the conversion of a  $H_2/CO$  mixture into paraffinic hydrocarbons and have been chosen from the group formed by cobalt, nickel and ruthenium.

B) The process is carried out as the first step of a three-step process in which the first two steps are carried out as stated under A) and in which in the second step a zirconium, titanium or chromium-promoted cobalt catalyst supported on silica as the carrier is used, which catalyst has been prepared by impregnation and/or kneading. In this process the fact is utilized that a catalyst hydrotreatment can be used to convert the high-boiling part of the product of the

second step into middle distillates in a high yield. In the present patent application the term "middle distillates" is used to designate hydrocarbon mixtures whose boiling range corresponds substantially with that of the kerosine and gas-oil fractions obtained in the conventional atmospheric distillation of crude mineral oil. Said distillation is used to separate from the crude mineral oil one or more gasoline fractions having a boiling range between 30 and 200°C, one or more kerosine fractions having a boiling range between 140 and 300°C and one or more gasoil fractions having a boiling range between 180 and 370°C.

The three-step process mentioned under B) comprises carrying out a catalytic hydrotreatment as the third step after the two-step treatment mentioned under A). The feed chosen for the catalytic hydrotreatment is at least that part of the reaction product of the second step whose boiling point lies above the final boiling point of the heaviest middle distillate desired as end product. The hydrotreatment which is characterized by a very low hydrogen consumption, yields middle distillates with a considerably lower pour point than that of those obtained in the direct Fischer-Tropsch conversion of a  $H_2/CO$  mixture. Very suitable catalysts for carrying out the catalytic hydrotreatment are those containing one or more noble metals from Group VIII supported on a carrier and in particular a catalyst containing platinum supported on a carrier 13—15 %w of which consists of alumina and the rest of silica.

C) The process is used as the first step of a two-step process in which methanol formed in the first step is catalytically converted in the second step into lower olefins and/or aromatic hydrocarbons. Catalysts very suitable for use in the second step of this process are crystalline metal silicates characterized in that, after calcination in air during 1 h at 500°C, they have the following properties:

a) an X-ray powder diffraction pattern in which the strongest lines are the lines mentioned in Table A.

20	<b>Table A</b>	25
	d(Å)	
	11.1±0.2	
	10.0±0.2	
25	3.84±0.07	30
	3.72±0.06	

b) in the formula which represents the composition of the silicate expressed in moles of the oxides and in which, in addition to  $SiO_2$ , one or more oxides of a trivalent metal M chosen from the group formed by aluminium, iron, gallium, rhodium, chromium and scandium occur, the  $SiO_2/M_2O_3$  molar ratio is higher than 10.

D) The process is carried out as the first step of a two- or three-step process as described under A) and B), respectively and the methanol formed in the first step is converted into lower olefins and/or aromatic hydrocarbons as described under C).

E) The process is carried out as the first step in a process for preparing methanol and generating power, in which from the reaction product of the first step are separated a fraction containing methanol and a fraction containing unconverted synthesis gas. The latter fraction is combusted and the combustion gas is used for generating power in a gas turbine. The hot exhaust gas of the gas turbine is used in the preparation of high-pressure steam, which is utilized for generating power in a steam turbine. In periods of peak loads the methanol prepared may very suitably be used as additional fuel for generating power in the gas turbine.

The invention is now illustrated by the following Example.

#### Example

Three zinc/chromium co-precipitates (co-precipitates A1—A3) and eight copper/zinc/chromium co-precipitates (co-precipitates B1—B8) were prepared.

The preparation of the zinc/chromium co-precipitates was carried out as follows. Zinc nitrate and chromium nitrate were together dissolved in water and the solution thus obtained, together with a stoichiometric quantity of an aqueous ammonia solution, was pumped with stirring through a mixing unit which was kept at a temperature of 20°C. The ratio of the feed rates was chosen such that the pH, measured at the outlet of the mixing unit, had a value between 7 and 8. The Zn/Cr co-precipitate obtained was collected and allowed to age for one hour with stirring at 20°C. The solid matter was filtered off and washed with water until the wash water was free from nitrate ions.

The preparation of the copper/zinc/chromium co-precipitates was carried out as follows. Copper nitrate, zinc nitrate and chromium nitrate were together dissolved in water and the solution thus obtained, together with a stoichiometric quantity of an aqueous soda solution, was pumped with stirring through a mixing unit which was kept at a temperature of 60°C. The ratio of the feed rates was

chosen such that the pH measured at the outlet of the mixing unit has a value between 6 and 7. The Cu/Zn/Cr co-precipitate obtained was collected and allowed to age for one hour with stirring at 20°C. The solid matter was filtered off and washed with water until the wash water was free from nitrate ions.

- 5 Co-precipitates A1—A3 and B1—B8 were used to prepare twelve catalysts (catalysts 1—12). 5  
The preparation was carried out as follows.

#### Catalyst 1

Cu/Zn/Cr co-precipitate B1 was dried at 120°C, the dried material was ground to an average particle size of 0.4 mm and the ground material was calcined for one hour at 300°C.

#### 10 Catalyst 2

- With the aid of a turbo stirrer Cu/Zn/Cr co-precipitate B1 was dispersed in water until the content of dry matter in the dispersion was 15 %w. The dispersion thus obtained was spray dried in a counter-current operation in air with the aid of compressed air. The inlet temperature of the air was 250°C and the outlet temperature of the air was 120°C. The pressure used was 0.4 bar. The powder obtained, 15  
which consisted substantially of globular particles of an average particle size of 50 micron, was pressed, ground to an average particle size of 0.4 mm and calcined for one hour at 300°C. 15

#### Catalyst 3

- Co-precipitates A1 and B2 were together dispersed in water with the aid of a turbo stirrer. The solid matter was filtered off, washed with water and dried at 120°C. The dried material was ground to an average particle size of 0.4 mm and the ground material was calcined for one hour at 300°C. 20

#### Catalysts 4 and 5

- Up to and including the spray drying preparation of these catalysts was carried out in substantially the same manner as that of catalyst 2, with the distinction that in the present case the starting mater was a dispersion containing both co-precipitate A1 and co-precipitate B2. The spray 25  
dried material was divided into two portions. The one portion was used to prepare catalyst 4 by pressing, grinding to an average particle size of 0.4 mm and calcined for one hour at 300°C. The other portion was calcined for one hour at 300°C to prepare catalyst 5. 25

#### Catalysts 6—12

- The preparation of these catalysts was carried out in substantially the same manner as that of catalyst 4. In all the cases the starting material was a dispersion which had been obtained by 30  
dispersing two separately prepared co-precipitates together in water and subsequently spray drying the dispersion. The spray dried material was used to prepare catalysts 6—12 by pressing, grinding and calcination. The co-precipitates used in the preparation of catalysts 6—12 were partly chosen from the group formed by A1—A3 and partly from the group formed by B2 and B4—B8.

- 35 The atomic ratio of the metals present in the co-precipitates used in the preparation of catalysts 1—12 are given in Table B. 35

- The atomic ratio of the two co-precipitates in each dispersion produced, calculated on the sum of the metals present in each co-precipitate is given in Table C. This table also lists the atomic ratios of the metals present in the ready catalysts (for the catalysts prepared by spray drying this ratio is also the 40  
atomic ratio of the metals present in the dispersions to be spray dried). 40

- In order to give some more understanding of the data listed in Table C, the preparation of catalyst 4 will hereinafter be pursued somewhat further. This catalyst was prepared starting from co-precipitate A1 having a Zn/Cr atomic ratio of 2:1 and a co-precipitate B2 having a Cu/Zn/Cr atomic ratio of 5:3:2. The two co-precipitates were together dispersed in water in an atomic ratio of 1:1, calculated on the 45  
sum of the metals present in each co-precipitate, viz. in addition to a quantity of co-precipitate containing 45

$$\frac{2}{3} \text{ gram atom Zn} + \frac{1}{3} \text{ gram atom Cr a quantity of co-precipitate B containing}$$

$$\frac{5}{10} \text{ gram atom Cu} + \frac{3}{10} \text{ gram atom Zn} + \frac{2}{10} \text{ gram atom Cr was dispersed in water.}$$

The dispersion thus prepared therefore contained the metals Cu, Zn and Cr in the atomic ratio

$$50 \quad \frac{5}{10} : \left( \frac{2}{3} + \frac{3}{10} \right) : \left( \frac{1}{3} + \frac{2}{10} \right) = 15:29:16 = 25:48:27 \quad 50$$

Table B

5	Co-precipitate no.	Atomic ratio of the metals present in the co-precipitate			5
		Cu	Zn	Cr	
	A1	—	2	1	
	A2	—	6	1	
	A3	—	1	5	
10	B1	25	48	27	
	B2	5	3	2	10
	B3	2	9	6	
	B4	2	3	2	
	B5	15	3	2	
	B6	5	1	4	
15	B7	25	1	24	
	B8	3	1	11	15

Table C

20	Catalyst no.	Atomic ratio of the metals present in the catalysts			Atomic ratio of the co-precipitates in the dispersions produced, calculated on the sum of the metals present in each co-precipitate		20
		Cu	Zn	Cr			
	1	25	48	27	—	—	
	2	25	48	27	—	—	
25	3	25	48	27	1A1	1B2	
	4	25	48	27	1A1	1B2	25
	5	25	48	27	1A1	1B2	
	6	6	60	34	1A1	1B3	
	7	24	47	29	1A1	5B4	
30	8	17	55	28	3,5A1	1B5	
	9	25	48	27	1A2	1B6	30
	10	25	23	52	1A3	1B2	
	11	25	34	41	1A1	1B7	
	12	15	22	63	1A1	3B8	

35 After reduction in hydrogen at 220°C catalysts 1—12 were tested for the preparation of 35  
methanol from synthesis gas. The testing of catalysts 1—4 and 6—12 was carried out in a 50-ml  
reactor containing a fixed catalyst bed of 5 ml volume. In eleven experiments (Experiments 1—11) a  
H<sub>2</sub>/CO/CO<sub>2</sub> mixture of a volume ratio of 67:31.5:1.5 was passed over each one of catalysts 1—4 and  
6—12 at a temperature of 250°C, a pressure of 60 bar and a space velocity of 5000 NI . 1<sup>-1</sup> . h<sup>-1</sup>. The  
40 results of these experiments are given in Table D. 40

Table D

5	Exp. no.	Catalyst no.	Yield, kg methanol . (1 catalyst) <sup>-1</sup> . h <sup>-1</sup>	Deactivation, % decrease of yield over 100 h ( $\frac{\text{decrease of yield over 100 h}}{\text{average yield over same period}} \times 100$ )		5
	1	1	0.82		5	
	2	2	0.35		2	
	3	3	0.74		8	
	4	4	0.98		<1	
10	5	6	0.31		<1	
	6	7	0.45		2	10
	7	8	0.47		4	
	8	9	0.84		2	
	9	10	0.92		5	
15	10	11	0.56		7	
	11	12	0.40		3	15

Catalyst 5 was tested in a vertically disposed fluidized bed reactor of 175 cm in height and of 500 ml volume containing 150 ml catalyst. In five experiments (Experiments 12—16) H<sub>2</sub>/CO/CO<sub>2</sub> mixtures were contacted with catalyst 5 at various temperatures, pressures and space velocities. The conditions under which these experiments were carried out are given in Table E. In all the experiments deactivation was less than 1 %. The synthesis gas conversions and methanol yields obtained in each of the experiments are also given in Table E.

Table E

Exp. no.	Composition of $H_2/CO/CO_2$ feed	Space velocity $NI \cdot l^{-1} \cdot h^{-1}$	Pressure bar	Temperature $^{\circ}C$	Runhour	Conversion of synthesis gas %v	Yield, $kg \text{ methanol} \cdot (l \text{ catalyst})^{-1} \cdot h^{-1}$
12	80:19:1.0	4150	60	250	100	37	0.76
13	67:32:1.2	3360	60	250	130	48	0.73
14	67:32:1.2	3360	80	250	150	60	0.90
15	67:32:1.3	1200	30	230	190	36	0.19
16	67:32:1.2	3360	60	250	786	35	0.19
					800	46	0.69
					1000	46	0.69



On the data given in Tables B—E the following may be remarked. Of catalysts 1—12 mentioned in Table C only catalysts 4 and 5 have been prepared according to the invention. They were obtained starting from two separately prepared co-precipitates and using the method of spray drying. The other catalysts fall outside the scope of the invention. They have been included in the patent application for comparison. Catalyst 1 was prepared starting from a single co-precipitate and without the use of spray drying. Catalyst 2 was prepared starting from a single co-precipitate. Catalyst 3 was prepared without spray drying. Although catalysts 6—12 were obtained starting from two separately prepared co-precipitates A and B and with spray drying being used, they did not meet the criteria of the process according to the invention, since

- 10 — in the case of catalyst 6 the  $\text{Cu}/(\text{Cu}+\text{Zn}+\text{Cr})$  atomic ratio in the dispersion was 0.06,
- in the case of catalysts 7 and 8 the atomic ratio in the dispersion of the sum of the metals coming from co-precipitate A to the sum of the metals coming from co-precipitate B was 0.2 and 3.5, respectively,
- 15 — in the case of catalysts 9 and 10 the  $\text{Zn}/\text{Cr}$  atomic ratio in co-precipitate A was 6 and 0.2, respectively,
- in the case of catalyst 11 the  $\text{Cu}/\text{Zn}$  atomic ratio in co-precipitate B was 25 and
- in the case of catalyst 12 the  $\text{Cr}/(\text{Cu}+\text{Zn})$  atomic ratio in co-precipitate B was 2.75.

Of Experiments 1—11 listed in Table D only Experiment 14 was carried out using a catalyst prepared according to the invention. The other experiments have been included in the patent application for comparison. As seen from the results given in Table D, only the catalyst prepared according to the invention displays a combination of very high activity (high yield) and very good stability (very little deactivation).

Experiments 12—16 given in Table E were all carried out using a catalyst which had been prepared according to the invention. As seen from the results given in Table E, the catalysts prepared according to the invention are also very suitable for use in a fluidized bed operation.

#### Claims

1. A process for the preparation of a catalyst, characterized in that a co-precipitate A comprising zinc as well as chromium and/or aluminium in such quantities that the  $\text{Zn}/(\text{Cr}+\text{Al})$  atomic ratio is 0.25—4 and a co-precipitate B comprising copper as well as zinc and, if desired, chromium and/or aluminium in such quantities that the  $\text{Cu}/\text{Zn}$  atomic ratio is lower than 10 and the  $(\text{Cr}+\text{Al})/(\text{Cu}+\text{Zn})$  atomic ratio is lower than 2, are together dispersed in water in such quantities that in the dispersion the atomic ratio of the sum of the metals coming from co-precipitate A to the sum of the metals coming from co-precipitate B is 0.25—3 and the  $\text{Cu}/(\text{Cu}+\text{Zn}+\text{Cr}+\text{Al})$  atomic ratio is more than 0.1, that the dispersion thus obtained is spray dried, and that the spray dried material is calcined.
2. A process as claimed in claim 1, characterized in that a co-precipitate A is used in which the  $\text{Zn}/(\text{Cr}+\text{Al})$  atomic ratio is 0.5—3.
3. A process as claimed in claim 1 or 2, characterized in that a co-precipitate B is used in which the  $\text{Cu}/\text{Zn}$  atomic ratio is lower than 5.
4. A process as claimed in any one of claims 1—3, characterized in that a co-precipitate B is used in which the  $(\text{Cr}+\text{Al})/(\text{Cu}+\text{Zn})$  atomic ratio is lower than 1.5.
5. A process as claimed in any one of claims 1—4, characterized in that the mixing ratio of the two co-precipitates is chosen such that in the dispersion the atomic ratio of the sum of the metals coming from co-precipitate A to the sum of the metals coming from co-precipitate B is 0.5—2.
6. A process as claimed in any one of claims 1—5, characterized in that the mixing ratio of the two co-precipitates is chosen such that in the dispersion the  $\text{Cu}/(\text{Cu}+\text{Zn}+\text{Cr}+\text{Al})$  atomic ratio is higher than 0.15.
7. A process as claimed in any one of claims 1—6, characterized in that the catalyst comprises the metal combination  $\text{Cu}/\text{Zn}/\text{Cr}$  or  $\text{Cu}/\text{Zn}/\text{Cr}/\text{Al}$ .
8. A process as claimed in any one of claims 1—7, characterized in that a co-precipitate A is used which, as metals, contains exclusively zinc and chromium.
9. A process for the preparation of a catalyst as claimed in claim 1, substantially as described hereinbefore and in particular with reference to the Example.
10. Catalysts whenever prepared according to a process as described in claim 9.
11. A process for the conversion of a mixture of carbon monoxide and hydrogen into methanol, characterized in that it is carried out using a catalyst as described in claim 10, which catalyst has first been reduced.
12. A process as claimed in claim 11, characterized in that the  $\text{H}_2/\text{CO}$  mixture has a  $\text{H}_2/\text{CO}$  molar ratio higher than 1.0.
13. A process as claimed in claim 11 or 12, characterized in that the  $\text{H}_2/\text{CO}$  mixture has been obtained by coal gasification or by catalytic steam reforming of light hydrocarbons.
14. A process as claimed in any one of claims 11—13, characterized in that a  $\text{CO}_2$ -containing  $\text{H}_2/\text{CO}$  mixture is used which contains 0.5—25 %v  $\text{CO}_2$ , calculated on the  $\text{H}_2/\text{CO}/\text{CO}_2$  mixture.

15. A process as claimed in any one of claims 11—14, characterized in that it is carried out at a temperature of 175—350 °C, a pressure of 5—150 bar and a space velocity of 250—25000 NI H<sub>2</sub>/CO mixture per 1 catalyst per hour.
- 5 16. A process as claimed in claim 15, characterized in that it is carried out at a temperature of 200—275 °C, a pressure of 20—100 bar and a space velocity of 500—10000 NI H<sub>2</sub>/CO mixture per 1 catalyst per hour. 5
17. A process as claimed in any one of claims 11—16, characterized in that it is carried out by using the catalyst in the form of a fluidized bed.
- 10 18. A process as claimed in any one of claims 11—17, characterized in that it is carried out as part of a multi-step process for the conversion of a H<sub>2</sub>/CO mixture. 10
19. A process as claimed in claim 18, characterized in that it is carried out as the first step of a two-step process in which in the first step methanol is formed and in which H<sub>2</sub> and CO present in the reaction product of the first step, together with other components of that reaction product, if desired, is contacted in a second step with a catalyst comprising one or more metal components having catalytic activity for the conversion of a H<sub>2</sub>/CO mixture into paraffinic hydrocarbons, which metal components have been chosen from the group formed by cobalt, nickel and ruthenium. 15
20. A process as claimed in claim 18, characterized in that it is carried out as first step of a three-step process in which the first two steps are carried out as disclosed in claim 19 and in which in the second step the catalyst used is a zirconium, titanium or chromium-promoted cobalt catalyst supported on silica as the carrier, which catalyst has been prepared by impregnation and/or kneading, and that in order to prepare middle distillates at least the part of the reaction product of the second step whose initial boiling point lies above the final boiling point of the heaviest middle distillate desired as end product is subjected in the third step to a catalytic hydrotreatment. 20
21. A process as claimed in claim 18, characterized in that it is carried out as the first step of a two-step process in which methanol formed in the first step is catalytically converted in the second step to form lower olefins and/or aromatic hydrocarbons. 25
22. A process as claimed in claim 18, characterized in that it is carried out as first step of a two-step or three-step process as described in claims 19 and 20, respectively, and that the methanol formed in the first step is converted into lower olefins and/or aromatic hydrocarbons as described in claim 21. 30
23. A process as claimed in claim 18, characterized in that it is carried out as the first step of a process for producing methanol and generating power, that from the reaction product of the first step are separated a fraction containing methanol and a fraction containing unconverted synthesis gas, that the latter fraction is combusted, that the combustion gas is used for generating power in a combined gas turbine/steam turbine system and that, in periods of peak loads the methanol produced in the first step is used as additional fuel for generating power in the gas turbine, if desired. 35
24. A process for the conversion of a mixture of carbon monoxide and hydrogen into methanol as claimed in claim 11, optionally followed by the preparation of hydrocarbons and the generation of power, substantially as described hereinbefore and in particular with reference to the example.
- 40 25. Methanol and, optionally, hydrocarbons and generated power whenever produced according to a process as described in claim 24. 40