PATENT SPECIFICATION



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COMPLETE SPECIFICATION.

Improvements in Methods for Carrying Out Catalytic Chemical Processes.

I, Joseph Prautmann, of 33, Halskestrasse, Berlin-Südende, Germany, of German nationality, do hereby declare the nature of this invention and in what manner the same is to be performed, to be particularly described and ascertained in and by the following statement:—

In carrying out catalytic processes it is
of great importance to secure as fine a
division of the materials to be treated as
possible and then to mix the particles
intimately so as to secure their very close
contact. These preliminary conditions
are a necessary part of the chemical conversion processes involved in improving
the quality of fuel, that is to say, in producing valuable liquid fuels, such as, for
example, benzine, from less valuable
liquid or solid fuels, such as, for example,
residues that are difficult to evaporate, or
coal. According to the present invention
they are created by the use of threshing
or centrifugal apparatus.

It is known to accelerate the hydrogenetion of carbon or oil or the synthetic
production of oils, for instance, from carbonic oxide and hydrogen by catalysers.
As such may be considered metals such as
tim. To assist the action of the catalyser
it has before been proposed to introduce
the catalyser in a liquid condition into
the reaction chamber or to force the raw
material through a liquid metal bath.
This last-mentioned method has the particular disadvantage that the surface
action is comparatively small.

The fine division, intimate, admixture, and increased surface action secured by the centrifugal or threshing movement according to the invention are combined with an increase in the action of the catalyser, the threshing or centrifugal apparatus working in a bath of threshing or centrifugal apparatus may also be coated with the catalyser.

The process according to the present invention may, 'for example, be carried 50 out as follows:

The metallic catalysers and other reaction substances may be introduced into the reaction chamber in liquid condition,

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or they may be liquefied by heating the reaction chamber and are maintained in this condition. Botating members are disposed in the reaction chamber; these thresh the liquid bath and thus atomize the liquid, the reaction substances intimately mixing with the resulting 60 mist.

Furthermore, the rotating parts can be so arranged that they drag the reaction substances through the bath and produce intimate contact between the reaction substances and the bath. This method has the advantage that by the threshing action of the rotating parts—that is, by the dragging of the reaction substances through the metal bath, local compressions are produced which assist the reaction process.

The liquid metal may, for instance, be circulated through the reaction chamber and heating apparatus, or the whole reaction chamber may be heated, the operation being advantageously so carried out that the atomized metal impinges upon the hot walls and is there permanently maintained heated. In this way the transmission of heat from the walls to the reaction substances is appreciably

The reaction chamber or the metal therein may be advantageously heated electrically, resistance heating elements, properly insulated, being provided outside the reaction chamber or in the metal bath itself. If metal salts are used as catalysers instead of metals themselves, electrical heat can be applied by directing the current directly through the bath of salts. Furthermore, the reaction chamber may be immersed in an electrically heated bath of salts.

A large surface action may be secured, moreover, by providing the threshing members, and if necessary, also the walls of the reaction chamber, with a catalytically acting coating. This process applies 100 to a further action by catalysers having a high melting point.

The catalytic coating may be applied electrolytically (galvanically) or by spraying those faces of the reaction chamber 105 or threshing apparatus which come into

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contact with the reaction substances during the operation.

The reaction chambers may be provided similarly to the blowers of known form 5 used for other purposes, in which a plurality of blowers can be arranged in series. In thus arranging the blowers the pressure rises in stages in the several blowers.

Apparatus for carrying out the method of the invention are illustrated by way of example in the accompanying drawings, in which:

Bigures 1 and 2 show an apparatus 15 which operates chiefly by threshing action:

Figure 3 shows an apparatus with centrifugal action; and

Figure 4 shows a blower.

In the construction according to Figures 1 and 2, threshers d are mounted on a shaft c in a vessel a, which is provided with a heating jacket and a removable cover b that is likewise heated; the shaft rotates in the bearing blocks k and l and is driven by means of the belt pulley At the ends of the threshers d beaters e are pivotally mounted. The substance to be treated is fed under pressure through the pipe g in such manner that it comes into position under the beaters, and is thence forced into the liquid in the vessel, which is molten metal m, and drawn right through it. As already indicated, this ensures particularly intimate contact between the liquid m and the reaction substance. Those of the products that are gaseous are carried off through the pipe i, and those which are 40 solid or liquid are drawn off through the

pipes h. Figure 3 shows a different construction. The upper part b of the heated vessel a has a number of recesses or cavities i, which has the effect of increasing the heating action. The shaft c, which runs in the bearings Is and I, is provided with a number of discs d which are connected together at their peripheries by bars e. The hars e pass through the metal in the vessel a taking up particles and carrying them along, so that a mist is formed from the molten metal or metal salts in the lower part. The reaction substances, which enter at g and leave at h, are chliged to pass through the mist so that very intimate contact is secured. The projections i prevent the reaction substance from passing directly from g to h, but cause it to be deflected towards the centre of the vessel. The device shown in Figure 4 comprises a wheel d with two inlet (suction) openings and common outlet openings on the periphery. It is dis-

65 posed within the outer heated jacket, the

upper part b of which can be lifted from the lower part a. The jacket is heated so strongly that the molten metal passing through the apparatus does not change its condition. Through the pipe s and the annular space to which it leads the molten metal is fed to the suction opening d^1 while through the pipe g and the annular space to which it leads reaction substances are fed to the suction opening d^2 of the wheel d, the openings d^1 and d^2 being oppositely disposed. The surfaces h^1 , h^2 form the blades of the blower wheel. On leaving the blade space the metal and the reaction substances are brought together. The centrifugal force produces centrifugal action which causes an intimate mixture of the metal acting es the catalyser and the reaction substances. The whole mixture is discharged through the outlet y, to a separating plant (not illustrated) by which the metal is separated from the products of the treatment, and the meral can be re-introduced into the circuit as a catalyser after it has been again heated up.

Having now particularly described and ascertained the nature of my said invention and in what manner the same is to be performed, I declare that what I

claim is:-

1. A method of carrying out catalytic reactions with molten metals or alloys or metal salts as catalysers, characterised in that the molten metal or the alloy or 100 metal salts is atomised in the reaction chamber by threshing or centrifugal apparatus, for the purposes and substantially as hereinbefore described.

2. A method as specified in Claim 1, 103 in which the threshing or centrifugal action is produced by rotating members, which pass through a bath of metal, for example, liquid tin, or of a metal alloy or a metal salt, and spray the liquid, sub- 110 stantially as hereinbefore described.

3. A method as specified in Claim I or in Claim 2, in which the rotating members drag the raw material through the bath and thus produce intimate contact, 115 substantially as hereinbefore described.

 Δ method as specified in any of the preceding claims, in which the bath of metal or metal salts, and in certain ciroumstances also the reaction chamber, are 120 heated electrically, substantially as hereinbefore described.

5. A method as specified in any of the preceding claims, in which the liquid, which acts as a catalyser, circulates 125 through the reaction chamber and a heating apparatus provided in series therewith, substantially hereinbefore สร described.

6. A method of carrying out catalytic 180

processes with molten metals or alloys as catalysts, according to Claims 1 to 5, characterised in that the threshing or centrifugal members provided for atomising the 5 molten metal or the metal alloy, and/or the walls of the reaction chamber are provided with a coating of a difficultly fusible catalytically acting metal for the purpose of securing an additional 10 catalytic action, substantially as herein-

before described.

7. A method of carrying out catalytic processes with molten metals or alloys as catalysers, as specified in any of the preceding claims, in which the reaction is carried out in a centrifugal blower into

which the material to be treated and the molten catalyser are fed or drawn in by suction and the inner surfaces of which can be completely or in part provided 20 with a catalytic coating, substantially as hereinbefore described.

8. A method as specified in any of the preceding claims, in which the material to be treated and the molten catalyser are treated in a number of blowers arranged in series in differing pressure stages.

Dated this 20th day of November, 1926. EDWARD EVANS & Co., 27, Chancery Lane, London, W.C. 2, Agents for the Applicant.

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