

RESERVE COPY

PATENT SPECIFICATION

620,775



Application Date: Sept. 6, 1946. No: 26906/46.

Complete Specification Accepted: March 30, 1949.

3521

Index at acceptance:—Classes 1(i), F3(b1 : c2 : c5) ; 1(iii), N13a ; and 2(iii), B1g.

COMPLETE SPECIFICATION

Improvements Relating to the Manufacture of Iron Catalysts and to the Manufacture of Liquid Hydrocarbons and Oxygenated compounds by the Aid of such Catalysts

(A communication from STANDARD OIL DEVELOPMENT COMPANY, a corporation duly organised and existing under the laws of the State of Delaware, United States of America, having an office at Linden, New Jersey, United States of America).

I, CONRAD ARNOLD, a British subject, of 29, Southampton Buildings, Chancery Lane, London, W.C.2., do hereby declare the nature of this invention, and in what manner the same is to be performed, to be particularly described and ascertained in and by the following statement:—

This invention relates to catalytic conversions and improved catalysts therefor. More specifically the invention is concerned with improved iron catalysts for fluid catalyst operation, particularly for the catalytic synthesis of normally liquid hydrocarbons and/or oxygenated compounds from CO and H₂.

Iron type catalysts are normally employed in the hydrocarbon synthesis at relatively high temperatures of about 450°-800°F. and relatively high pressures of about 3-100 atm. abs. or higher, to obtain predominantly unsaturated and oxygenated products from which motor fuels with high octane ratings may be recovered.

The extreme temperature sensitivity and relatively rapid catalyst deactivation of the hydrocarbon synthesis have led in recent years to various attempts and proposals to employ the so-called fluid catalyst technique wherein the synthesis gas is contacted with a dense turbulent bed of finely divided catalyst fluidized by the gaseous reactants and products and which permits continuous catalyst replacement and greatly improved temperature control. However, the adaptation of the hydrocarbon synthesis to the fluid catalyst technique has encountered serious difficulties, particularly when iron catalysts are used.

Application of the fluid catalyst technique requires in addition to the conventional characteristics determining catalyst utility, such as total desired yield, and active cata-

lyst life, ease of fluidization and attrition resistance. None of the iron catalysts prepared according to the prior art complies satisfactorily with all of these requirements.

Iron catalysts are usually prepared by the reduction of various natural or synthetic iron oxides or by the decomposition of iron carbonyls, the catalytic activity being enhanced by the addition of such promoters as various compounds of alkali metals or the oxides of chromium, zinc, aluminum, magnesium, manganese, the rare earth metals, and others, in small amounts of about 1-10%. While some of these catalysts exhibit excellent activity characteristics they are without exception deficient with respect to ease of fluidization and attrition resistance for the following reasons:

Catalysts obtained by the reduction of natural iron oxides, such as various oxidic iron ores, may be ground to a fluidizable particle size, however, not without excessive losses in the form of fines having particle sizes below the minimum fluidizable size of about 30 microns. In addition, the particles of proper fluidizable size are extremely brittle and subject to excessive attrition in the course of fluid operation.

Iron catalysts prepared by the reduction of synthetic oxides, such as precipitated red or yellow iron oxides or by the decomposition of iron carbonyls, are obtained in the form of extremely fine powders having particle sizes far below the fluidizable range. Attempts to convert these powders into fluidizable materials by agglomerating treatments, such as pilling or sintering, have failed as a result of either the low attrition resistance or the irregularity of the agglomerates.

The present invention overcomes the aforementioned difficulties and affords various additional advantages as will be fully understood from the more detailed description given below.

It is therefore the main object of this

(PRICE 2/-)

Price 4s 6d

invention to provide an improved process for the catalytic conversion of CO and H₂.

Another object of this invention is to provide an improved catalyst for the hydrocarbon synthesis and a method of preparing the same.

A more specific object of this invention is to provide an iron catalyst for the hydrocarbon synthesis, which combines high activity and long catalyst life with highest utility for fluid catalyst operation.

A still further object of this invention is to provide an improved hydrocarbon synthesis process operated by the fluid catalyst technique.

Another object of this invention is to provide an iron catalyst having improved utility for fluid catalyst operation.

Other and further objects and advantages will appear hereinafter.

In accordance with the present invention easily fluidizable iron catalysts are obtained by subjecting iron oxides to a sintering treatment and grinding the sintered material to a fluidizable particle size. A reducing treatment may be applied, preferably prior to grinding. It has been found that the sintering treatment increases the mechanical strength of the catalyst mass so considerably that it may be ground in conventional grinders to a desired particle size, e.g., at least 50% of the particles falling within the range of 30 to 250 microns or about 60-400 mesh with a negligible loss in the form of non-fluidizable fines of less than 30 microns or about 400 mesh particle size represents a preferred size range. In addition, the fluidizable catalyst particles, hardened by sintering, are far superior to fluidizable iron catalysts prepared by conventional methods with respect to attrition resistance and exhibit highest catalytic activity and satisfactory catalyst life.

It is important for the catalytic, mechanical and pseudo-hydrodynamic properties of the catalysts of this invention that the sintering treatment be subsequent to any treatment with liquids or solids, which affects the chemical composition and/or physical structure of the catalyst. This statement does not apply to treatment in a reducing atmosphere which may be carried out before or after the sintering treatment. When preparing these catalysts, it is preferred, therefore, to combine the iron oxide with the addition agents desired, such as promoters as hereinbefore defined, by impregnation or mechanical mixing and to subject the resulting composite to sintering followed by grinding to the desired particle size.

While sufficiently pure iron oxides of any origin and particle size may be used as the starting material for the improved iron catalysts, the best results are obtained when fine iron oxide powders, particularly the precipitated material known as red iron oxide, are employed which have substantially uniform particle sizes of less than, say, about 50 microns and preferably less than about 30 microns. These iron oxide powders may first be impregnated with suitable solutions of promoters to yield a powdered or lumpy mass which is subjected to sintering to form a hard friable mass which is ground to the desired particle size of say about 30 to 200 microns. A reducing treatment may precede or follow the sintering treatment, but in accordance with the preferred embodiment of this invention the sintering treatment is carried out in a reducing atmosphere, using hydrogen, carbon monoxide, gaseous hydrocarbons, or the like, or mixtures of such reducing gases.

Suitable sintering temperatures fall within the approximate range of 1200°-1600°F. in a reducing atmosphere, but may be considerably higher in a non-reducing atmosphere. For instance in an inert atmosphere of nitrogen or the like it may range anywhere from about 1600°F. to about 2700°F. The sintering treatment should be carried at least to a point at which surface deformation of the sintered particles becomes appreciable. Reduction temperatures ranging from about 800° to about 1500°F. are generally adequate to obtain the desired degree of reduction which may reach the metallic state or any oxygen concentration known to be beneficial for iron catalysts.

A typical method suitable for preparing iron catalysts useful in fluid catalyst operation is illustrated by the following example:

EXAMPLE

Red iron oxide powder having an average particle size of about 10-20 microns is impregnated with a solution of potassium carbonate in distilled water of about 1-1.5 wt. % strength until about 1.5% of potassium carbonate based on iron has been incorporated in the iron oxide. The resulting pasty mass is dried at a temperature of about 150°-300°F. and reduced in a stream of hydrogen at about 900°F. for about 2-6 hours. The lumpy, reduced material is sintered in a hydrogen atmosphere at about 1600°F. for about 4 hours, ground by subjecting it to 3 or 4 passes through a conventional laboratory planetary disc grinder. Products having the following typical sieve analyses are obtained:

	Sieve Sizes		Weight Percent	
	Through	On	Sample A	Sample B
	...	40	1.0	
	40	60	1.1	
5	60	100	7.3	13.8
	100	140	9.1	11.5
	140	200	9.8	12.6
	200	270	22.3	8.1
	270	325	23.9	9.1
10	325	...	25.5	44.5
	Loss		0.0	0.4

The above samples contain more than 50% of particles within the size range of 60-325 mesh and fluidize readily, both in nitrogen and synthesis gas mixtures of carbon monoxide and hydrogen. For example, at superficial gas velocities normal for dense phase fluid operation, such as 0.2-0.4 ft. per second, a turbulent fluidized solids bed is formed having a well defined upper level and exhibiting a steady pressure drop over the height of the fluidized mass similar to that of a liquid. Small amounts of entrained solids may be readily separated from the gas by conventional mechanical gas-solids separators. The catalyst retains essentially this condition in normal fluid operation for more than 750 hours.

Catalysts obtained from red iron oxide powder or iron ores by sizing without sintering or by sintering without subsequent grinding on the other hand, when applied at similar conditions of gas flow form either immediately or after about 5-10 hours operation compact catalyst masses through which the gas bubbles without any fluidizing effect entraining usually large proportions of catalyst fines which cannot be separated by gas-solids separators of the type mentioned and require gas filters or similar complicated means of separation.

A catalyst prepared in accordance with the above Example was employed in the hydrocarbon synthesis using a synthesis gas containing about 2 moles of H_2 per mol of CO and a gas recycle ratio of about 2:1 at a fresh feed gas throughput of about 1,000 volumes of gas per volume of catalyst per hour, a superficial gas velocity of about 0.4 ft. per second, a pressure of about 250 lbs. per sq. in. gauge and a reaction temperature of about 600°F. At these conditions about 97% of the CO supplied was converted to form, per cubic meter of synthesis gas, about 214 c.c. of C_4 and higher hydrocarbons including oxygenated organic compounds recovered from the product water.

The experimental results reported above demonstrate that the catalysts prepared in accordance with the present invention combine perfect ease of fluidization with highest catalytic activity.

While this invention has been described with specific reference to the catalytic synthesis of hydrocarbons it will be readily understood that the invention affords similar advantages in connection with other fluid catalyst operations involving the use of iron type catalysts, for example the hydrogenation of unsaturated hydrocarbons, the synthesis of ammonia, the halogenation of certain hydrocarbons, etc.

The present invention is not to be limited to any examples given merely for illustration purposes.

Having now particularly described and ascertained the nature of the said invention, and in what manner the same is to be performed, as communicated to me by my foreign correspondents, I declare that what I claim is:—

1. An improved iron catalyst, comprising sintered iron oxide particles of fluidizable size.

2. A catalyst according to Claim 1, comprising iron oxide particles at least 50% of which has a size falling within the range of 60-400 mesh per linear inch.

3. A catalyst according to Claim 2, wherein said iron oxide is red iron oxide.

4. A process for preparing iron oxide catalyst which comprises subjecting an oxidic iron mass to a sintering treatment and grinding the sintered material to a fluidizable size.

5. A process according to Claim 4, wherein the oxidic iron mass is subjected to a reducing treatment.

6. Process according to Claims 4 or 5, wherein said oxidic iron mass is ground to contain at least 50% of particles having a size falling within the range of 60-400 mesh per linear inch.

7. Process according to Claims 4 or 5, wherein a promoter as hereinbefore defined is incorporated into the oxidic iron mass prior to the sintering treatment.

8. Process according to Claim 7, wherein the composite is subjected to a reducing treatment prior to its use as a catalyst.

9. Process according to Claim 7, wherein the oxidic iron mass is impregnated with a solution of said promoter.

10. Process according to Claim 9, wherein the oxidic iron mass is red iron oxide powder.

11. An improved process for producing valuable conversion products from CO and H_2 in the presence of an iron catalyst which comprises contacting a gas containing CO and H_2 in synthesis proportions, under synthesis conditions with a fluidized mass of a catalyst prepared according to any one of Claims 4, 5, 7, 9 or 10.

12. A process according to Claim 11,

wherein the catalyst is prepared by subjecting an oxidic iron mass containing an incorporated promoter, to a sintering treatment, and grinding the sintered material to a fluidizable size.

5 13. A process according to Claim 12, wherein the sintering treatment for the

preparation of the catalyst is carried out in an inert atmosphere.

Dated this 6th day of September, 1946.

D. YOUNG & CO.,

29, Southampton Buildings Chancery Lane,
London, W.C.2.

Agents for the Applicant.