MOBI 18.12.78 46704C/27 H04 H(4-D, 4-E5, 4-F2E) N(2-A1). \*EP -- 12-571 MOBIL OIL CORP 29 18.12.78-US-970307 (25.06.80) B01i-29/30 C07c-01/04 Catalytic composite of iron component, zeolite and matrix - for high activity in converting synthesis gas to olefinic or conversion of synthesis gas, esp. to naphtha aromatic naphtha, producing < 30 wt % methane + ethane. Little aging is evident. **DETAILS** D/S: E(DT,GB,SW). (I) is pref. ferrous oxalate and may be formed in situ. (II) may be siliceous, Al<sub>2</sub>O<sub>3</sub> or SiO<sub>2</sub> /Al<sub>2</sub>O<sub>3</sub>. (III) is pref. A catalyst compsn., having been prepd. by (a) forming a ZSM-5. The composite is pref. spray-dried before the mixture of a water-insoluble Fe deriv, of an organic cpd. CO-treatment which is effected at 288-343°C for 0.5-24 (I), a matrix (I) and an acidic crystalline aluminosilicate hrs. zeolite (III) having an SiO2/Al2O3 ratio of > 12, a pore size The spray-drier is pref. operated with air at 500-1000 of  $\geq 5$  A and a constraint index of 1-12. (b) drying the °F, the particles at the completion of the drying pref. mixture, and (c) treating the dried composite with CO being at 200-350°F. Following this step, the catalyst is (or synthesis gas), is claimed. heated to decompose the organic Fe cpds., e.g. at 115-1200F Also claimed is the use of the catalyst in the conversfor 1-48 hrs. ion of synthesis gas at 500-600°F and 50-1000 psig. In a prefd. embodiment, (II) is made from mixtures of colloidal SiO2 and Al2O3, usually in a slurry contg. a weigh-USES ting agent (e.g. clay). Following this, (III) and (I) are In the product of hydrocarbons, esp. naphtha, from synthesis gas pref. 1:1  $H_2/CO$ ) at 550-580°F, 150-400 added and the mixt. homogenised and dried. (47pp920). (E) ISR: US4086262, FR2268771. psig and with a GHSV of 500-6000. ADVANTAGES The catalysts, which require no promotors, exhibit EP--12571