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26668 E/14 A41 E17 H09 J04 RUHRCHEMIE AG

19.09.80-DE-035404 (31.03.82) B01i-23/84

catalysts, yield is increased by addn. of lower alcohol(s)

RUHR 19.09.80 A(1-D13) E(10-J2C3) H(4-E5) J(4-E1) N(2, 3)

\*EP --48-378

C07c-01/04 C07c-

normally 1:1. The synthesis gas: alcohol (vapour) volume lower olefin(s) prepn. by reaction of synthesis gas - over iron ratio is pref. 1-4:1.

EXAMPLE

D/S: E(FR GB NL)

11/02

In the production of lower (esp. 2-4C) olefins by the reaction of carbon oxides with H2 at 220-500°C and up to 30 bars in the presence of known (esp. Fe- and/or Co-based) catalysts,

presence of low-molecular (esp. 1-3C) alcohols. ADVANTAGES

the improvement comprises effecting the reaction in the

The yield of lower olefins is increased synergistically. E.g., with added methanol, the yield of 2-4C olefins can be increased from 40.7 to 76.8 g/N cu.m.

## **DETAILS**

The catalyst, usually as a solid bed, comprises (a) Fe and/or Co; (b) activators, e.g. oxides of Gp. Ha and/or Hb metals in amts. of 2-20 wt. % or Na<sub>2</sub>CO<sub>3</sub> or K<sub>2</sub>CO<sub>3</sub>; and (c) selectivity-improvers for olefin prodn., e.g. difficultlyreducible oxides of V and/or Mn, or Ti or Th, in amts, of 5-50 wt. %. The CO:H2 volumeratio in the synthesis gas is

mixt. of 50 ml. catalyst and 250 ml. silicon carbide. The catalyst comprised (pts. wt.): Fe in the form of Fe O., 100: V in the form of V<sub>2</sub>O<sub>5</sub>, 80; ZnO, 30; and K<sub>2</sub>O, 4. The temp. was 335°C, and the pressure was 10 bar. In three experiments, the flow rates (v/vh) were: (i)

A laboratory reactor, of 2 cm. i.d., was packed with a

CO+H<sub>2</sub>1005; (ii) CO+H<sub>2</sub> 944 and MeOH vapour 562; (iii) MeOH vapour 591 and N2 980. The 2-4C olefin yields (a/N cu.m.) were: (i) 40.7; (ii) 76.8; (iii) -.(15pp1492) (G) ISR: DE2438251 US2486633 DS-764165 DS-865893 DS-904891 DE2507647 DS2518982