MOBI 22.10.82 H(1-F) H04 (H06 H07) 83-820502/46 *US 4413-153-A MOBIL OIL CORP 140 22.10.82-US-436158 (01.11.83) C07c-01/04 Step (b) is pref. effected by steam reforming using a Fuel and petrochemical prodn. from wet natural gas - by zealite Ni-contg. catalyst. Step (c) may be effected converting the conversion of dehydrogenated heavier components synthesis gas to methanol and converting this to gasoline using a ZSM-5 catalyst. Step (d) may be effected by thermal cracking or catalytic dehydrogenation. Methane alone may be recycled from (e) to (b). C83-112690 | Prodn. of synthetic fuels and petrochemicals Step (f) may be effected at 350-600°F and 100-3000 paig from wet natural gas is effected by with a WHSV of 0.1-5 to produce olefinic gasoline and a (a) separating the wet gas into a C₃+ paraffin fraction (I) 330 °F+ distillate. The distillate may be catalytically and a dry gas fraction (II) comprising methane and athane; hydrogenated at 550-700°F and 100-500psig, with an LHSV (b) converting (II) to synthesis gas; of 0.5-5 and an H2 rate of 1000-5000 scf /bbl, to obtain a (c) converting the synthesis gas to gasoline; 330-500°F, jet fuel fraction, a 500-650°F diesel fuel frac-(d) converting (I) to a C3+ olefin fraction (III) and a 1-2C tion and a 650°F+ lubricating oil fraction. (8pp367APSDwgNd hydrocarbon fraction (IV); 0/0).(e) recycling (IV) to step (b); and (f) converting (III) to a wide range of transportation fuels and lubricating oils by contact with a zeolite having a SiO2/ Al2O3 molar ratio of at least 12 and a constraint index of 1-12 (esp. ZSM-5).

ADVANTAGES

DETAILS

The process increases the range of prods. obtainable from wet natural gas.

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