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SHEL 06.07.84
                       E18 H04 J04
86-009178/02
                                                    *EP -167-215-A
SHELL INT RES MIJ BV
   06.07.84-NL-002149 (08.01.86) B01j-23/74 C07c-1/4 C10g-47/14
                                                                          The catalysts are prepd. as described in NL8301922 and
Hydrocarbon prodn. from synthesis gas - using cabalt catalyst with
                                                                      satisfy the relationship:
specified ratio of external to internal surface area
    C86-003885 E(AT BE DE FR IT NL SE)
                                                                                  (3 \times 4R) > L/S_i > Z (0.3 + 0.4R)
                                                                      where L = the total amt. of Co on the catalyst (mg/ml) and R
Prodn. of hydrocarbons is effected by contacting synthesis
                                                                      = the wt. ratio between the amt. of Co applied to the catalyst
gas at elevated temp. and pressure with a catalyst comprising
                                                                      by kneading and the total amt. of Co on the catalyst.
3-60 pts. wt. Co, 0.1-100 pts. wt. Zr, Ti and/or Cr and 100
                                                                      PREFERRED CONDITIONS
pts. wt. SiO2, Al2O3 or SiO2-Al2O3.
                                                                          The reaction is effected at 125-350°C and 5-100 bar,
    The catalyst (prepd. by kneading and/or impregnation)
                                                                      with an H,/CO molar ratio of 1.75-2.25, using a catalyst com-
is in the form of a fixed bed with an external surface area
                                                                      prising 15-50 pts. wt. Co, 100 pts. wt. SiO, and either (i)
(Se) of 5-70 cm<sup>2</sup>/ml and an internal surface area (S<sub>i</sub>) of 10-
                                                                      0.1-5 pts. wt. Zr if the Co was applied to the catalyst first
400 m<sup>2</sup>/ml, such that Se<sup>2</sup> x S<sub>i</sub> is less than 1,000,000 and
                                                                     or (ii) 5-40 pts. wt. 2r if the Zr was applied first.
greater than 25,000.
                                                                          Prods. boiling above the middle distillate range are
                                                                      hydrocracked using a catalyst comprising 0.1-2 wt. % Pt or
IADVANTAGE
    The process gives high C5+ selectivities, e.g. 76-79% at
                                                                      Pd on SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> to produce middle distillates. (12pp 367RKMH
                                                                      DwgNo0/0).
58-63% conversion.
                                                                      (E)ISR: No Search Report.
MORE SPECIFICALLY
    The catalyst bed has Se = 10-50 cm<sup>2</sup>/ml and S<sub>i</sub> = 15-200
m<sup>2</sup>/ml, with Se, x Si being less than 250,000 and greater than
                                                                                                                         EP-167215-A
30,000.
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E(10- AU-A-44575/85 1-C, 1-D, 2-B, 2-F, 3-B, 3-