88-037705/06 E36 H08 SHEL 05.08.86 E(31-A1) H(4-E4) SHELL INT RES MIJ BV *EP -255-748-A 05.08.86-GB-019076 (10.02.88) C01b-03/36 Partial oxidn, of hydrocarbon fuel using concentric burner arrangement having 3 oxygen channels and 1 fuel channel, giving in situ fine atomisation and long burner lifetime on residue fuels C88-016725 R(BE DE ES FR GB IT NL SE)

Process for partial oxidn. of a hydrocarbon-contg. fuel comprises supplying it and an O2-contg. gas through a concentric burner arrangement to a gasification zone, with autothermic prodn. of synthesis gas, and specifically supplying the central channel of the concentric burner arrangement with the O2-contg. gas at 21-42 m/sec., the 1st concentric channel (surrounding the central channel) with O2-contg. gas at 60-120 m/sec., the 2nd concentric channel with fuel at 3.0-3.8 m/sec., and the 3rd (outer) concentric channel with O,-contg. gas at 60-120 m/sec.

USE/ADVANTAGE

The process is useful for liq. fuels, for which in situ fine atomization is obtd. There is good and rapid mixing of O, and fuel, and preignition or flame-flash-back is prevented. (Heavy) residue may be gasified, with economic process

conditions (e.g. reduced moderator gas supply and reduced soot prodn.) for a sufficiently long burner lifetime (longer than 8000 h.).

STREAM VELOCITIES

The above velocities are pref. measured at the outlet of the respective channels.

OPERATING PRESSURE

The pressure is pref. 0.1-12 MPa.

OXIDANT GAS

The O₂-contg. gas may contain a moderator, pref. steam or CO₂. Pref. 5-40 wt.% of the O₂-contg. gas is supplied through the central channel.

INERT GAS

The burner lifetime can be increased by supplying a gaswhich does not react exothermically (e.g. H₂O, CO, or CH₄) through a 4th concentric channel, surrounding the 3rd. This can cause the flame to lift and the heat flux to decrease.

EXAMPLE

Tests have been carried out with fuel of s.g. 980-1018 EP-255748-A+

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