US4900707-A

ESSO 18.12.87 H04 *US 4900-707-A EXXON RES & ENG CO 13.12.88-US-283658 (+US-134698) (13.02.90) B01j-27/12 Wax isomerisation catalyst mfr. - by depositing metal on support,

fluorinating, crushing, sizing and activating C90-043471 Catalyst for use in a wax isomerisation process is produced by

(a) depositing a hydrogenation metal component (I) on a

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followed by calcination; (b) fluorinating the metal-loaded support to a level of 2-10 (2-8) wt. % F, using an acidic fluorine source (III); (c) crushing to expose the inner surfaces of the prod. and sizing to a particle size 1/32 in. or less across the largest continuous cross sectional dimension; and (d) activating by heating in a hydrogen atmos. In a process variant, step (c) precedes step (b).

refractory metal oxide particle or extrudate support (II),

USE/ADVANTAGE The catalyst gives an improved yield of isomerised prods., and lube oil fractions taken from the isomerate have exceptionally high viscosity. The wax feed pref. contains 5-15%, esp. 7-10%, oil.

AU-A-26946/88_ H(4-A7, 4-E, 4-F2A, 4-F2E) N(1-C2, 2, 4-D, 6-E) ESSO 18.12.07 89-180132/25 H04 *EP -321-299-A EXXON RES & ENG CO 18.12.87-US-134698 (21.06.89) B01j-23/40 B01j-37/26 C10g-45/62 PREFERRED CATALYST Prodn. of catalyst for isomerising wax - comprising catalyst on The metal is 0.1-5 (0.2-0.6) wt. % of a Gp. VIII metal, metal oxide support and hydrogenation metal, by calcining e.g. Pt. The support is, or contains, Al₂O₃. Fluoridising fluoriding, crushing and activating is with a soin. of HF, to give 2-10% of F. The support is C89-079540 R(BE DE ES FR GB IT NL) sleved to remove particles above 0.79375 mm; the particle size is pref. 0.3969-0.79375 mm. Activation is at 350-500 deg. A catalyst for use in wax isomerisation is prepd. by

(1) depositing a hydrogenation metal component on a refractory metal oxide particle or extrudate support, followed by calcination; (2) fluoriding the loaded support, using an acidic F source: (3) sizing the halogenated, loaded support to expose inner surfaces and give sized particles not more than 0.79375 mm across the longest continuous cross-sectional dimension; and

(4) activating by heating in H2.

ADVANTAGE

Opt. stage (3) may precede stage (2).

than do prods. from wax with 0% oil or 20% oil.

High selective conversion of wax to liq. isomerised prod. is achieved, and the isomerised dewaxed oil prod. has high VI. Prods. obtd. from wax contg. 7% of oil have higher VI

was fluorided in 11.6% aq. HF soln., washed, dried at 150 deg. C in a vacuum, crushed to particles of 1/30 inch, and activated in 50 psi flowing H, by heating from room temp. to 100 deg. C in 2 h, to 450 deg. C in 3 h, and at 450 deg. C for 1 h. (B) The catalyst used was to isomerise 600N slack waxes cong. (i) less than 1%, (ii) 7%, or (iii) 23% of oil. Conversion to 370+ deg. C prods. was: (i) 13, (ii) 24, (iii) 12.8; 25.8. The viscosity at 100 deg. C was: (i), (ii), (iii) 4.8; and viscosity index was: (i) 148, (ii) 150, (iii) 135, 137. (9pp510CGDwgNo0/0). (E) ISR: No Search Report. EP-321299-A

(A) A 1/16 inch γ-Al₂O₃ extrudete carrying 0.6 wt. % Pt

C in H, for at least 1-48 h.

EXAMPLE