AIRP 07.04.88 | E(10-E4E1) J(4-E1) N(1-C2, 2-D1, 3-F) E17 J04 89-294351/41 *EP -336-440-A AIR PRODUCTS & CHEM INC 07.04.88-US-178953 (11.10.89) C07c-29/15 C07c-31/04 EMBODIMENT Conversion of carbon mon:oxide-rich synthesis gas to methanol - in Carbon monoxide-rich synthesis gas and liquid water are lig, phase reactor with addn. of water to effect shift reaction in fed together or separately to liquid phase reactor (7) operating reactor in slurry or ebullated mode with a methanol synthesis catalyst R(BE DE ES FR GB IT NL SE) C89-130331 (e.g. CuO/ZnO/Al,O1) opt. mixed with a low temp. shift catalyst. Vapour effluent is cooled, separated at (11) and liquid In the conversion of a carbon-monoxide rich synthesis gas (I) to a crude methanol product (II), (I) is balanced by reaction recycled; vapour is further cooled and passed to CO, absorber (17) where it is contacted countercurrent with cold with water in the presence of a water/gas shift catalyst to decrease its carbon monoxide content and increase its hydromethanol solvent which removes CO,, methanol and water; gen and carbon dioxide contents. At least part of the carbon crude methanol is recovered in unit (23). Water-free dioxide is removed from the shifted gas to produce a balanced methanol-free synthesis gas (19) is passed to a second liquid synthesis gas, which is then reacted in presence of a methanol phase reactor (31) where further synthesis takes place. Further crude methanol is recovered by separator (43), and synthesis catalyst to produce (II). The improvement comprises combining the water/gas shift unconverted synthesis gas from this separator is compressed and methanol synthesis reactions into a single step, by and passed to third liquid phase reactor (51). Further crude reacting (I) with water in presence of a catalyst in a liquid methanol is recovered by separator (61) and unreacted gas phase reactor, to produce both (II) and a synthesis gas of (63) compressed after removal of a purge stream, and reduced carbon monoxide content and increased hydrogen and recycled to the reactor. carbon dioxide contents suitable after carbon dioxide removal Conventional gas-phase methanol synthesis reactors may be used instead of the liquid phase reactors (31) and (51). for further conversion to methanol. EP-336440-A+

