## AU-A-40005/89

E(31-A1) H(4-E4) N(2-C1)

ESSO 28.03.88 \*US 4877-550-A ADVANTAGES

0/2).

09.01.89-US-294854 (+US-1 '4173) (31.10.89) C01b-03/30 Mfg. hydrogen and carbon i iono:oxide as synthesis gas - by indirectly cooling prod. gas I miting formation of methane and

Process for the prodn. of H. and CO comprises:

(i) reacting in a fluidise i reaction zone a light hydrocar-

bon feed with steam and oxy en at elevated temps, in the presence of a catalyst contg Ni on a support;

(ii) recovering from the reaction zone a prod. gas comprising H2, CO and entrained catalyst: (iii) cooling by indirect neans with boiling water forming high pressure steam in a cocing zone, the prod. gas at a

rate of at least about 306°F/ , thereby minimising the reaction of CO with H2 to form CH4; (iv) recovering high pressure steam from the cooling zone: (v) preheating the hydr carbon feed with at least a portion of the steam recovered in step (iv); and

(vi) maintaining a net or aversion of feed to CO and H2 of

E36 H04

90-014906/02

EXXON RES & ENG CO

cooler carbon deposits

C90-006444

at least 80%.

The process preserves as H2 and CO, the hydrocarbon conversion to synthesis gas in the reaction zone, whilst preventing carbon deposition in equipment lines during the cooling step as well as making more efficient use of the heat

that heat to preheat the light hydrocarbon feed to the reaction zone. PREFERRED CONDITIONS

Cooling is effected at a rate of 400-900°F/s until the temp, of the prod. gas is less than about 1200°F. The temp. in the reaction zone is at least about 1750°F. At least 5% of the recovered steam is used for preheating the feed. The net conversion of feed to CO and H2 is at least about 90%.

The formation of carbon in the cooling zone is less than about

0.2 moles carbon per 100 moles CO and H2. (6pp1684CGDwgNo

recovered in the cooling zone and to save energy by using

US 4877550- A