AU-A-80280/91

92-017891/03 E17 H04 J04

*EP -466-268-A

SHELL INT RES MIJ BV 10.07.90-GB-015193 (15.01.92) B01j-27/22 C07c-01/04 Fischer-tropsch catalysts for hydrocarbon synthesis - comprising alloys of $G_D = Vib$. $G_D = Vilb and/or <math>G_D = Vili metals$ C92-007730 RIAT BE CHIDE DK ES FR GB GR IT LI LU NL SE)

Fischer-Tropsch catalysts comprise an alloy of at least two Group Vib, VIIb and/or VIII metals, provided that (a) the alloy has a negative heat of formation w.r.t. the

(b) 1-20 mole % of total metal and at least 50 mole % of surface metal in the alloy is converted to carbide after contact with synthesis gas (II,/CO=2) at 250°C and 1 bar for 3 hr.

ADVANTAGES

support.

individual metals, and

The catalysts have high initial activity and good activity stability for hydrocarbon synthesis.

SPECIFICALLY CLAIMED

The metals are Ni and Fe, with a Ni: Fe molar ratio of 45:55 to 70:30. The catalysts also include an alumina

SHEL 10.07.90 H(4-E5, 4-F2E) J(4-E4) N(2-A1, 2-C1)

EC10-J2DY

The negative heat of formation is 0.1-10 (0.4-5) KJ/mole. The allow upon contacting with synthesis gas forms a total amt, of carbide of 5-15 mole 2 and 60-90 mole 2 surface carbide.

EXAMPLE

2.29g of K.Fe(CN), was dissolved in 100 ml water and slowly injected into a soln. of 3.36g of Ni(NO₁)2.6H2O in 1 1. water in which 4.00g of Al.O. (Degussa Al oxide C) had been suspended. The resulting ppte was filtered, washed and vacuum dried. The product was pelletised, crushed to obtn. Nis/Fe complex evanide. Oxidation was then carried out at 305°C. The obtd. catalyst was reduced with hydrogen under

0.1 MPa pressure while heating from 100 to 450°C over 64 hr. and ratio of reduction gas:argon/hydrogen of 9:1. Synthesis gas was converted to hydrecarbons using the catalyst at 0.1 MPa, 250°C, H./CO ratio of 2 and GHSV of 60 NL/1/min. The entalyst showed high initial activity and good stendy state activity. (9pp367RBHDwgNo9/0). (E) ISR: US4687753 US4186112 US2601121.

EP-466268-A