

Table 1
Results of Synthesis Experiments at High Space Velocities

| Catalyst | IRON (SYNTHETIC-AMMONIA) | | | | | | | | | | | | | | COBALT | | | | | | | |
|--|--------------------------|-------|-------|-------|-------|-------|-------|-------|-------|-------|-------|-------|-----------|-------|-----------|-------|--------|-------|-------|-------|-------|-------|
| Type of process | FIXED BED | | | | | | | | | | | | FLUID BED | | FIXED BED | | | | | | | |
| Experiment number | 12/26 | | | | | | | | | | 12/28 | | 16/2 | | 10A/30 | | 10A/34 | | | | | |
| Time in days from start of synthesis | 9 | 16 | 20 | 36 | 68 | 73 | 80 | 90 | 93 | 107 | 124 | 18 | 21 | 1-5 | 6-9 | 35 | 42 | 37 | 41 | 47 | 52 | 64 |
| Reaction pressure, atmos. gauge | 10 | 20 | 20 | 20 | 20 | 20 | 20 | 25 | 25 | 25 | 25 | 20 | 20 | 20 | 20 | 10 | 10 | 10 | 10 | 10 | 10 | 10 |
| Reaction temperature °C. | 285 | 280 | 288 | 281 | 292 | 308 | 318 | 295 | 308 | 312 | 330 | 300 | 300 | 300 | 300 | 208 | 220 | 215 | 220 | 230 | 240 | 260 |
| H ₂ : CO Ratio of synthesis gas | 2.03:1 | | | | | | | | | | | | 2.31 | 2.34 | 2.05:1 | | | | | | | |
| Synthesis gas space velocity, vol./vol. catalyst/hr | 418 | 416 | 644 | 398 | 530 | 530 | 1050 | 530 | 688 | 556 | 1040 | 533 | 680 | 793 | 1019 | 366 | 510 | 353 | 516 | 526 | 500 | 538 |
| Recycle ratio, vol. residual gas vol. syn. gas | -- | -- | -- | 2.23 | 2.18 | 2.26 | 1.33 | 2.24 | 2.13 | 2.16 | 1.32 | 2.18 | 2.03 | 7.1 | 6.1 | -- | -- | 2.39 | 2.16 | 2.21 | 3.30 | 1.44 |
| Gas Contraction, per cent | 48.2 | 55.4 | 51.6 | 74.0 | 71.0 | 79.6 | 72.6 | 76.3 | 75.6 | 76.2 | 65.5 | 76.6 | 79.0 | 83.0 | 82.7 | 74.5 | 74.0 | 75.5 | 76.1 | 74.8 | 76.1 | 68.0 |
| CO converted, percent | 95.8 | 96.2 | 93.4 | 95.5 | 91.5 | 96.0 | 94.4 | 93.0 | 91.7 | 93.1 | 90.2 | 98.2 | 97.5 | 99.1 | 99.5 | 78.1 | 83.0 | 80.0 | 79.3 | 79.7 | 82.3 | 83.6 |
| CO converted to CO ₂ per cent of total | 29.2 | 23.2 | 23.9 | 7.5 | 6.6 | 5.2 | 9.2 | 4.4 | 4.8 | 3.4 | 8.1 | 6.2 | 5.6 | nil | nil | nil | 4.2 | nil | nil | nil | nil | 9.2 |
| CO converted to CH ₄ per cent of total | 17.1 | 14.3 | 11.7 | 12.0 | 11.2 | 12.4 | 12.9 | 10.6 | 9.6 | 13.8 | 13.6 | 18.8 | 15.5 | 19.9 | 20.9 | 18.7 | 26.9 | 14.5 | 23.9 | 28.4 | 36.1 | 54.0 |
| CO converted to higher hydrocarbons percent of total | 53.7 | 62.5 | 64.4 | 80.5 | 82.2 | 82.4 | 77.9 | 85.0 | 85.6 | 82.8 | 78.3 | 75.0 | 78.9 | 80.1 | 79.1 | 83.3 | 68.9 | 85.5 | 76.1 | 71.6 | 63.9 | 36.8 |
| Utilisation ratio, vol. H ₂ vol. CO | 1.14 | 1.29 | 1.15 | 1.75 | 1.68 | 1.83 | 1.71 | 1.78 | 1.77 | 1.81 | 1.58 | 1.82 | 1.88 | 2.23 | 2.30 | 2.22 | 2.23 | 2.10 | 2.23 | 2.29 | 2.30 | 2.22 |
| Yield CH ₄ g., N.cu.m. synthesis gas | 36.7 | 30.9 | 24.8 | 25.2 | 23.2 | 27.4 | 28.0 | 22.6 | 20.2 | 29.0 | 27.6 | 41.5 | 33.7 | 40.2 | 42.4 | 32.8 | 50.0 | 26.9 | 42.6 | 50.0 | 65.6 | 101.6 |
| Yield of C2 to C4,g., N.cu.m. synthesis gas | 56.6 | 76.3 | 77.2 | 53.6 | 75.0 | 71.4 | 85.0 | 87.7 | 92.5 | 85.4 | 82.4 | 87.9 | 71.8 | 104.4 | 106.7 | 34.3 | 32.0 | 74.0 | 64.4 | 60.7 | 68.2 | 28.0 |
| Yield of liquid hydrocarbons, g., N.cu.m. synthesis gas | 47.3 | 44.9 | 45.7 | 97.9 | 77.4 | 91.5 | 67.1 | 77.8 | 72.2 | 70.5 | 60.0 | 62.6 | 81.7 | 33.3 | 31.7 | 96.8 | 83.0 | 67.7 | 54.9 | 52.0 | 35.3 | 34.0 |
| Yield of total higher hydrocarbons, g./N.cu.m. synthesis gas | 103.9 | 121.2 | 122.9 | 151.5 | 152.4 | 162.9 | 152.1 | 165.5 | 164.7 | 155.9 | 142.4 | 150.5 | 153.5 | 137.7 | 138.4 | 131.1 | 115.0 | 141.7 | 119.3 | 112.7 | 103.5 | 62.0 |